



Gasoline Particulate Filter (GPF) Modeling and Multi-Objective Optimization Investigation

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Motivation



- The pursuit of higher fuel efficiency and power from IC engines has led to the rapid development of combustion strategies, such as gasoline direct injection (GDI).
- GDI has higher particulate matter (PM) and particle number (PN) emissions than port fuel injection (PFI). [1]
- Ceramic wall-flow exhaust filters are one way to control PM and PN in gasoline exhaust.
- Gasoline particulate filters (GPFs) are different from diesel particulate filters (DPFs).
 - PM from GDI engine is lower in concentration than diesel [1]
 - GDI vehicles are more sensitive to back pressure, cost, and weight
 - GPFs often need a three-way catalytic coating for four-way functionality



There is need for GDIspecific PFs with high filtration efficiency and low pressure drop, to meet the EURO 6 or similar PN regulations.[2]



[1] Maricq, M. How are emissions of nuclei mode particles affected by emission control. in HEI-conference May. 2009.

[2] Badshah, H., Kittelson, D., and Northrop, W., Particle Emissions from Light-Duty Vehicles during Cold-Cold Start, SAE Int. J. Engines 9(3):1775-1785, 2016, doi:10.4271/2016-01-0997.



Background



- The analytical solution for DPF flow fields and regeneration was derived by Bissett [3], which set up a solid foundation for later DPF and GPF modeling.
- Unit collector model by Konstandopolous and Johnson [4], incorporated with the packed bed theory proposed by Payatakes [5] are still widely used in DPF and GPF filtration modeling. Both models have been validated by numerous experiments.



 Both models are used in this study with modification for the porous wall microstructure study of GPF and 3D filtration study.

[3] Bissett, E., Mathematical model of the thermal regeneration of a wall-flow monolith diesel particulate filter. Chemical Engineering Science, 1984. 39(7-8): p. 1233-1244.
[4] Konstandopoulos, A.G. and J.H. Johnson, Wall-flow diesel particulate filters—their pressure drop and collection efficiency. 1989, SAE Technical Paper.
[5] Payatakes, A.C., C. Tien, and R.M. Turian, A new model for granular porous media: Part I. Model formulation. AIChE Journal, 1973. 19(1): p. 58-67.
[6] G. Muntean, George & L. Stewart, Mark & Devarakonda, Maruthi. Solid/Condensed Phase Aftertreatment Systems. 2014



Model Platform Selection



GPF Study	CFD (ANSYS FLUENT)	Analytical Study
0D/1D solution		
2D solution		
3D solution		\bigcirc
Detailed flow field		\bigcirc
Particle tracking		\bigcirc
Enable microstructure study		

 \checkmark

Good!



Approach



Two Objectives:

- 1. High Filtration Efficiency
- 2. Low Pressure Drop

Three areas of research interest:

- 1. Pore size and distribution effects
- 2. Effect of pore structure
- 3. Permeability uniformity effects



1. Pore Size and Distribution



FLUENT Setup

- Steady state study
- Incompressible flow
- Laminar flow
- Boundary conditions:
 - > Velocity inlet: 5 cm/s
 - Pressure outlet: 1 atm

30 um

Injected particle size

↔ 10 um

≻ 100 nm

20 um





Velocity Field





Wide Pore Distribution

Tight Pore Distribution

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Pressure Field





Wide Pore Distribution $\Delta P=54 Pa$

Tight Pore Distribution ΔP=43 Pa



Particle Tracking



100 nm particles injected





100 nm particles injected

Wide Pore Distribution Filtration Efficiency E = 24%

Tight Pore Distribution Filtration Efficiency E = 18%



2. Effects of Pore Structure





The cavity to throat ratio indicates that the throat is the key length scale.



Throat Unit Collector



FLUENT Setup

- Axis-symmetric simulation
- Virtual surface (one radius from wall) is introduced to account for the particle capture by interception
- Steady state study
- Incompressible flow
- Laminar flow
- Boundary conditions:
 - Velocity inlet 5 cm/s
 - Pressure outlet 1 atm
- Injected particle sizes:
 - ≻ 100 nm
 - ➢ 50 nm/300 nm

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Diameter Ratio	Throat Diameter	Cavity Diameter
5:1	20 um	100 um
3:1	20 um	60 um
2:1	20 um	40 um
1.5:1	20 um	30 um
1:1	20 um	20 um





Filtration Efficiency Increases with Decreasing Cavity Diameter

100 H 100	Diameter Ratio	Throat Diameter	Cavity Diameter
101-04 - 101-04 - 101-04	5:1	20 um	100 um
Contraction of the	3:1	20 um	60 um
	2:1	20 um	40 um
115-2722	1.5:1	20 um	30 um
10000	1:1	20 um	20 um



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3. Permeability Uniformity Effects



FLUENT Setup

- Steady state, incompressible, laminar flow
- Boundary conditions:
 - Velocity inlet: 2.226m/s (based on working condition of 60 kg/hr, 500 C)
 - Outlet P: 1 atm
 - Particle injection:
 - 100 nm, 648 kg/m³

Inlet Channel Outlet Channel Porous Wall Inlet Zone Outlet Zone		Y Y Y X
GPF Specifica	ations]
Cell density	300 CPSI	
Wall thickness	12 mil	
Plug length	5 mm	
Inlet/Outlet zone length	5 mm	

Wall Permeability Distribution

CRC





Permeability Changing Axially





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Pressure Drop Comparison

	Pressure Drop	From the Viscous Friction	From the Wall
Uniform	864 Pa	280 Pa	584 Pa
Three Zones	893 Pa	280 Pa	613 Pa
Linearly Increases	830 Pa	280 Pa	550 Pa
Linearly Decreases	830 Pa	280 Pa	550 Pa
1D Analytical from Ford	973 Pa	400 Pa	573 Pa

Three zones has a higher pressure drop due to _ higher wall velocity

Compared to the 3D prediction, 1D model has

a higher pressure drop because of the higher viscous friction





Wall Velocity Comparison



Determining Filtration Efficiency

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By using User Defined Function (UDF), filtration efficiency can be resolved to every single particle injected in the system, in accordance to their travel speed and local fluid velocity.



Particle Tracking





ANSYS R18.0

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Particle Tracking

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Summary



- 1. Pore size and distribution study
 - Under the same working condition (500 C, 60 kg/s), a tight pore distribution has a 20% lower pressure drop across the porous wall.
 - However tight pore distribution has a filtration efficiency 25% lower than wide.
- 2. Pore structure study
 - Using the throat unit collector model, filtration efficiency increases with decreasing diameter ratio.
 - The pressure drop for throat unit collector decreases with decreasing diameter ratio.
- 3. Permeability uniformity study
 - For most permeability distributions, particles tend to accumulate at the end of channel due to inertial effects.
 - linearly decreasing permeability along the flow path is more stable, with lower overall pressure drop and more even ash storage potential.



Work In Progress



- The effect of the vertical gap between unit collectors is also being investigated.
- Sensitivity study on the influence of average pore size change *i.e.* wider distribution with smaller average pore size vs. smaller distribution with larger average pore size.
- Develop a method to relate the single unit collector efficiency to total filter efficiency, and compare it with the spherical unit collector model and experiments. $\eta \xrightarrow{\mathcal{P}} E(\eta, \varepsilon, w, d_p)$
- Transient study to investigate the permeability uniformity effects on GPF pressure drop, filtration efficiency and ash storage in a longer term.





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Questions?