

# SCR DEACTIVATION KINETICS STUDY FOR CONTROL AND AGING APPLICATIONS

SwRI Internal Research Project



$NH_3$  STORAGE CAPACITY AND  $E_d$  DETERMINATION  
Final Report

# Presentation Outline

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- Project Objectives
- BASF Fe-Zeolite catalyst - recap
  - $\text{NH}_3$  storage capacity ( $\Omega$ ) test conditions, results and conclusions
  - Deactivation energy ( $E_d$ ) determination
- Johnson Matthey V/W/TiO<sub>2</sub> 'SINOx' Catalyst - recap
  - $\text{NH}_3$  storage capacity ( $\Omega$ ) test conditions, results and conclusions
  - Deactivation energy ( $E_d$ ) determination
- BASF Cu-Zeolite catalyst – new data
  - $\text{NH}_3$  storage capacity ( $\Omega$ ) test conditions, results and conclusions
  - Deactivation energy ( $E_d$ ) determination
- Overall Summary and Conclusions



# Project Objectives

- SwRI Completed an Internal Research and Development Project to Better Understand SCR Catalyst Deactivation in Fall 2010
  - The project had three primary objectives:
    - Evaluate  $\text{NH}_3$  storage capacity ( $\Omega$ ) as a function of aging time and temperature to provide data for on board SCR catalyst model-based control algorithms
    - Determine deactivation energies ( $E_d$ ) for each SCR formulation to assist in accelerated thermal aging calculations using Arrhenius equation
    - Evaluate  $\text{NO}_x$  transient response with  $\text{NH}_3$  transients for possible use as an On-Board Diagnostic (OBD) metric - presented in 2010. Not repeated here.



# Catalyst Aging

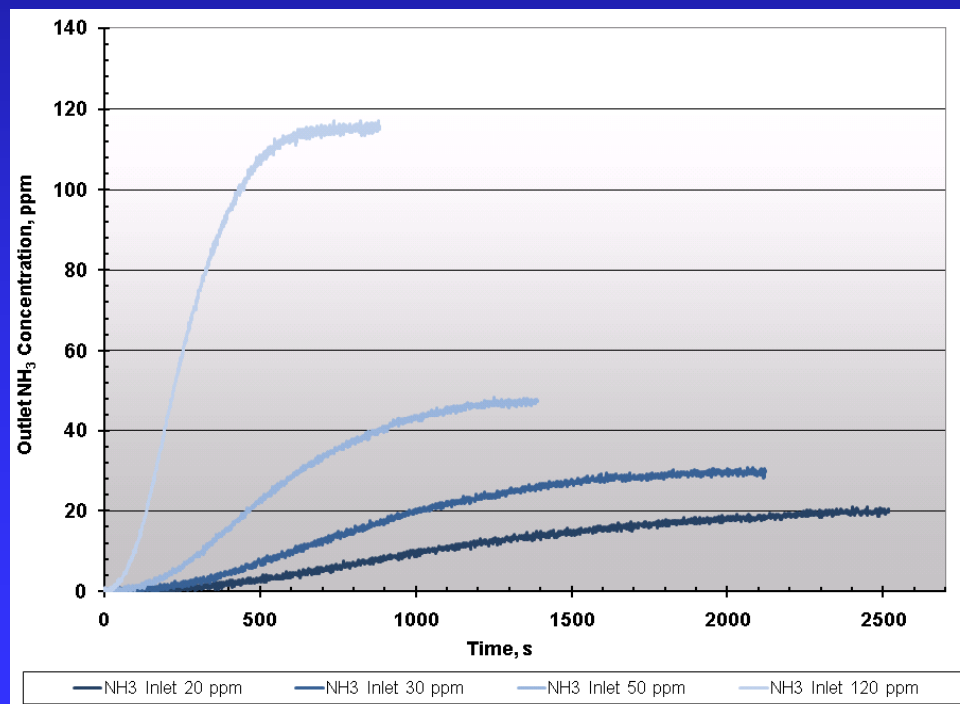
- 1 inch diameter x 1 inch long core
- Aged in situ in SwRI Universal Synthetic Gas Reactor® (USGR®)
- Gas Mixture: 14% O<sub>2</sub>, 5% CO<sub>2</sub>, 6% H<sub>2</sub>O, balance N<sub>2</sub>
- Space Velocity: 60,000 hr<sup>-1</sup>
- Fe-Zeolite
  - Preconditioned 2 hours, 350°C (Max. Ω)
  - Aged 2, 4, 8, 16 hours at 475, 550, 625, 700°C
- V/W/TiO<sub>2</sub>
  - Preconditioned 2 hours, 600°C (Max. Ω)
  - Aged 2, 4, 8, 16 hours at 550, 600, 650, 700°C
- Cu-Zeolite
  - Preconditioned 8 hours, 775°C (Max. Ω)
  - Aged 2, 4, 8, 16 hours at 700, 775, 800, 850°C



# Fe-Zeolite

## NH<sub>3</sub> Adsorption Test Conditions

- Gas Mixture: 14% O<sub>2</sub>, 5% CO<sub>2</sub>, 5% H<sub>2</sub>O, X ppm NH<sub>3</sub>, balance N<sub>2</sub>
- Test Temperature 200°C ± 0.5°C (tight control critical)
- Space Velocity 120,000 hr<sup>-1</sup>
- Catalyst 'cleaned' of NH<sub>3</sub> Between Test Points (NO + NO<sub>2</sub> + NH<sub>3</sub> fast reaction used)
- NH<sub>3</sub> Setpoints 20, 30, 50, 120 ppm
- Note Single Point Equilibration Times as Long as 54 Minutes at 20 ppm NH<sub>3</sub> Concentration



# Fe-Zeolite

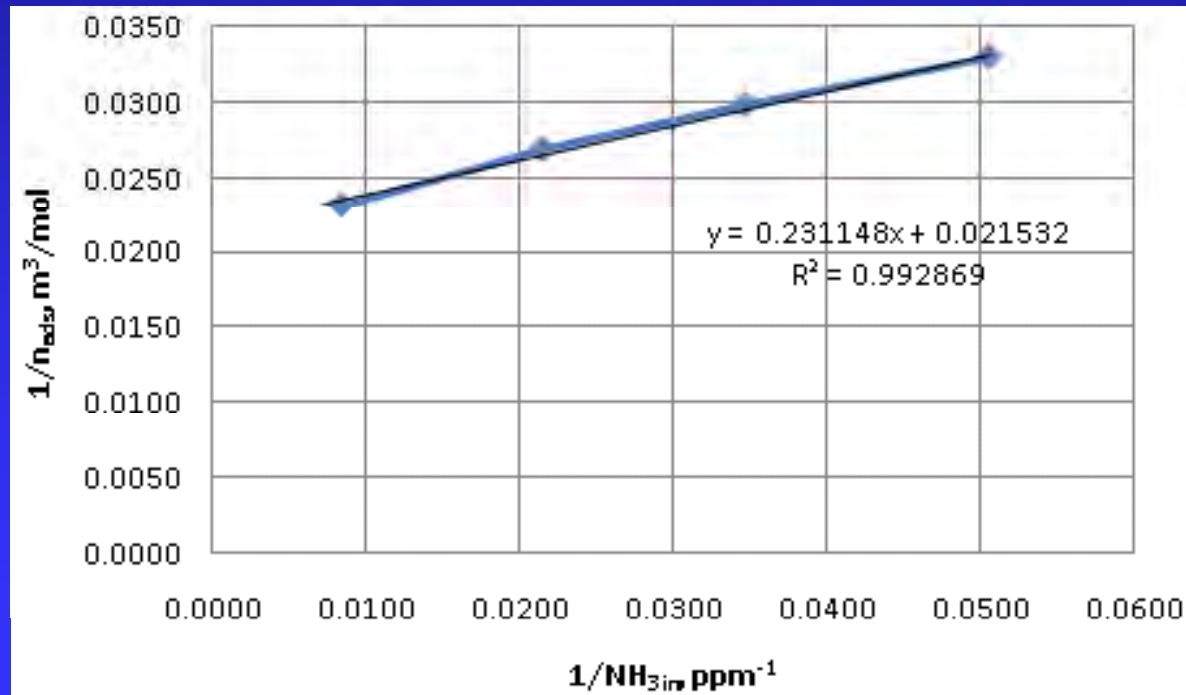
## NH<sub>3</sub> Adsorption Test Results (1)

- Data fitted to Langmuir adsorption isotherm model by plotting the data in Langmuir coordinates

$$1/n_{ads} = 1/\Omega + 1/(K_{eq} \times \Omega) \times 1/C_{NH_3}$$

Plotting  $1/n_{ads}$  as a function of  $1/C_{NH_3}$  yields a line with slope  $1/(K_{eq} \times \Omega)$  and intercept  $1/\Omega$

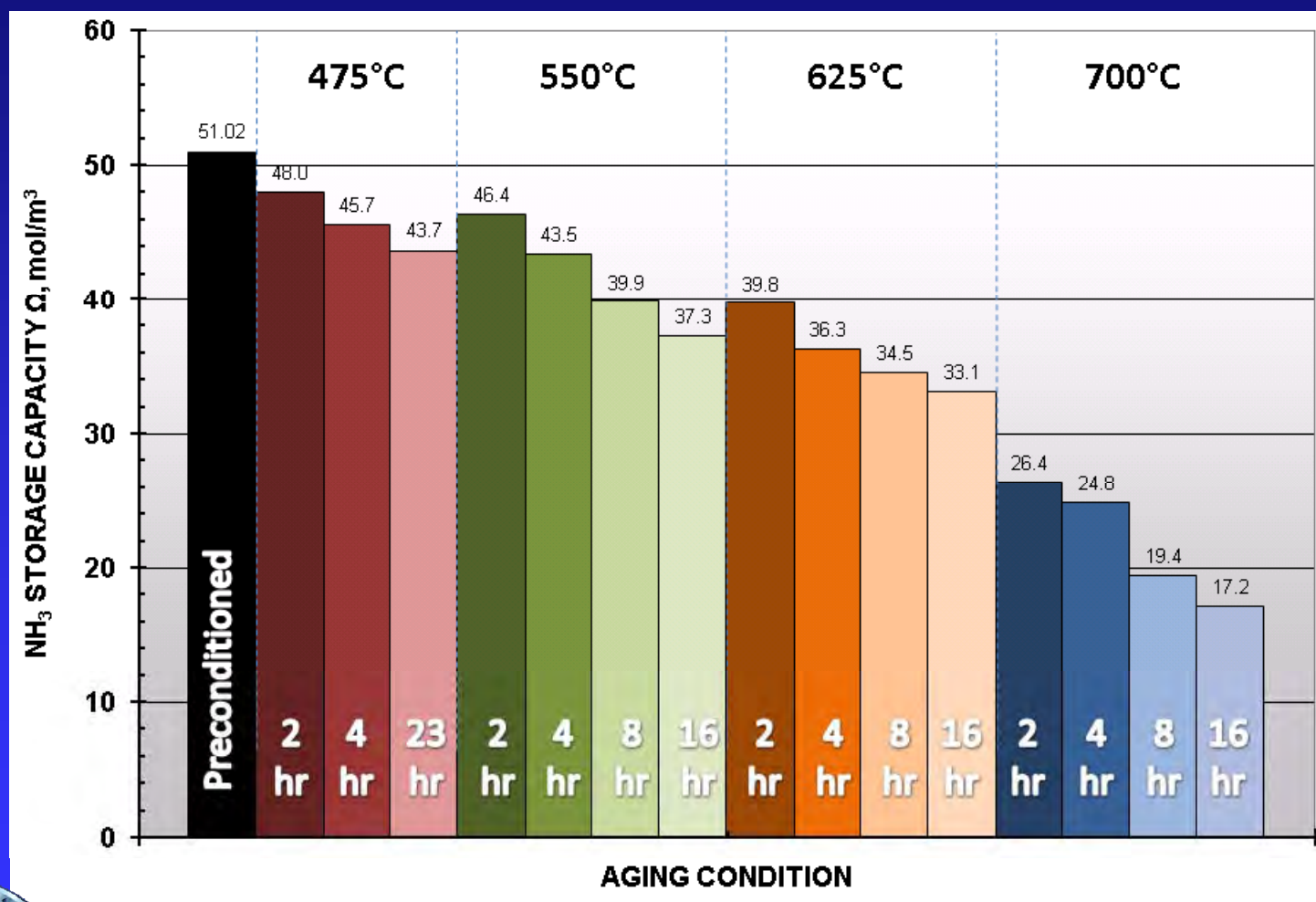
- $R^2 = 0.99$ , therefore NH<sub>3</sub> adsorption obeyed a Langmuir type isotherm well



# Fe-Zeolite

## NH<sub>3</sub> Adsorption Test Results (2)

- NH<sub>3</sub> Storage Capacity Decreased with Aging Time and Temperature



# Fe-Zeolite

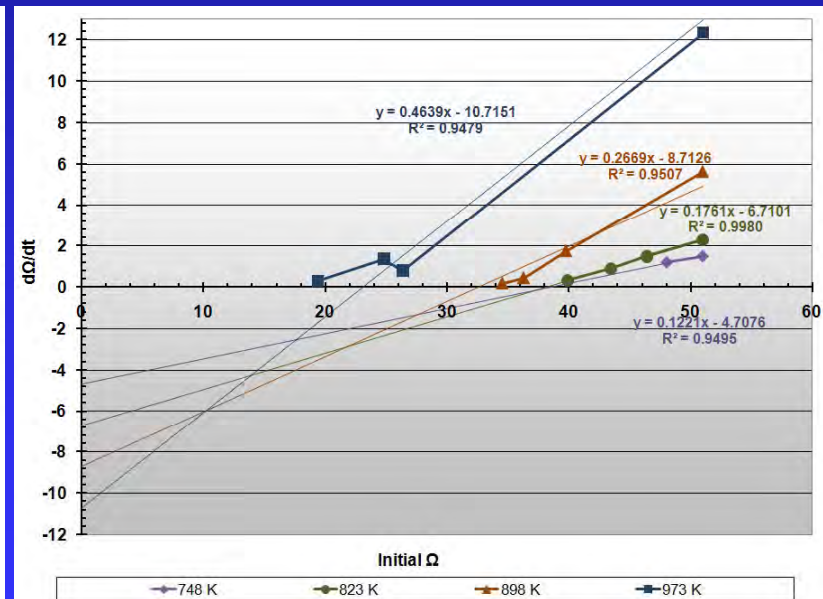
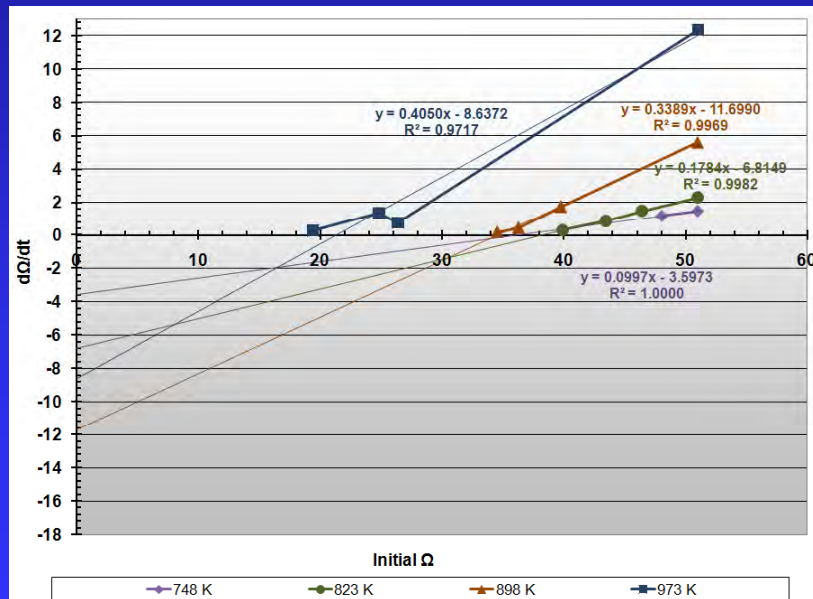
## Deactivation Energy Determination, $E_d$ (1)

- 1<sup>st</sup> Order Rate Equation Returned 'Straight' Lines with Variable Intercepts

Rate Equation  $-d\Omega/dt = k\Omega_1 + (x - yT)$

$\Omega$   $\text{NH}_3$  storage capacity,  $\text{mol/m}^3$      $t$  time, hours     $k$  rate constant     $T$  temperature, K  
 $x$  constant     $y$  constant

- Linear regression trendlines processed to obtain  $x$  and  $y$  constants

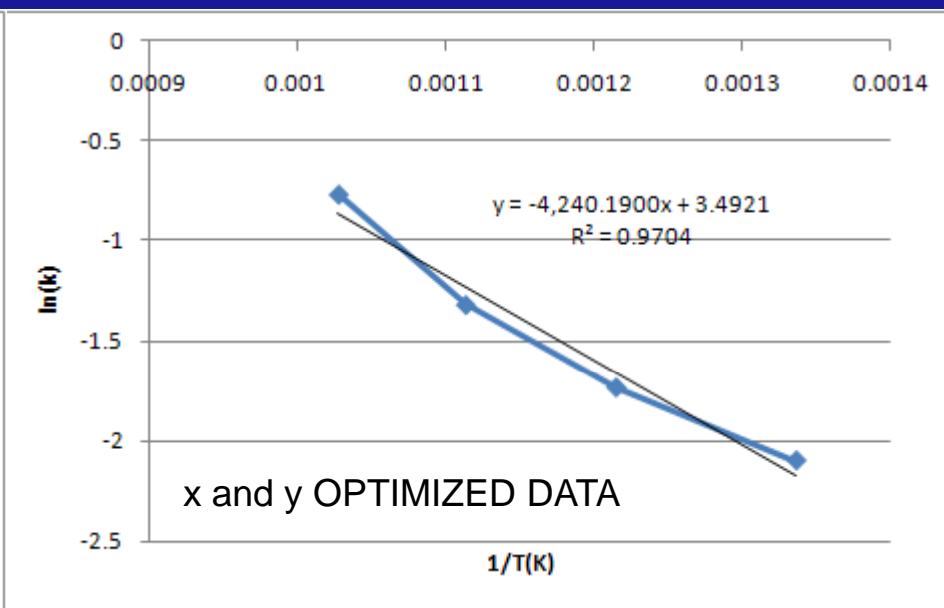
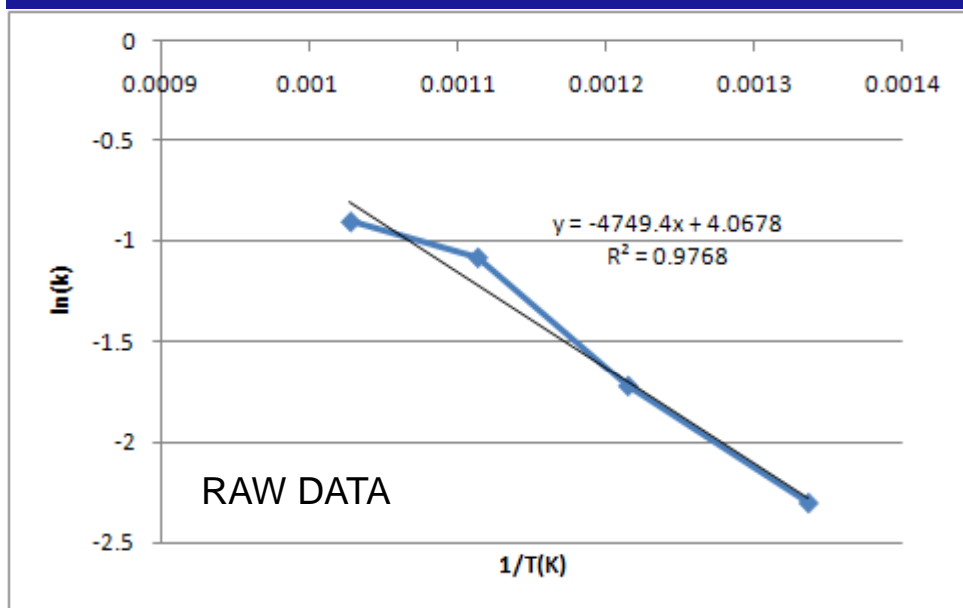


# Fe-Zeolite

## Deactivation Energy Determination, $E_d$ (2)

Arrhenius Equation Plots  $k = A e^{-(E_d/RT)}$

- Raw Data -  $E_d = 39.49$  kJ/mol  $A = 56.83$
- $x$  and  $y$  Optimized Data -  $E_d = 35.26$  kJ/mol  $A = 32.85$   $x = 15.268$   $y = 0.0267$



# Fe-Zeolite

## Deactivation Energy Determination, $E_d$ (3)

- MS Excel Solver Used to Obtain Best Fit Constants
- Best fit -  $E_d = 43.16$  kJ/mol  $A = 118$   $x = 45.05$   $y = 0.06454$

	MEASURED $\Omega$			
	TEMPERATURE, Kelvin			
Aging, Hrs	748.15	823.15	898.15	973.15
2	48.0	46.4	39.8	26.4
4	45.7	43.5	36.3	24.8
8	nd	39.9	34.5	19.4
16	nd	37.3	33.1	17.2

Test Data

	CALCULATED $\Omega$			
	TEMPERATURE, Kelvin			
Aging, Hrs	748.15	823.15	898.15	973.15
2	45.8	45.2	39.6	28.4
4	41.8	42.2	38.2	29.2
8	35.6	38.1	32.5	17.7
16	28.9	38.9	35.1	15.5

Calculated Values using  
Rate Equation

-  $d\Omega/dt = k\Omega_1 + (x - yT)$   
and Best Fit Constants

	PERCENTAGE ERRORS			
	TEMPERATURE, Kelvin			
Aging, Hrs	748.15	823.15	898.15	973.15
2	4.6	2.6	0.4	7.7
4	8.6	2.9	5.3	17.6
8		4.5	5.8	9.0
16		4.2	6.0	9.6
Average % error =		6.3		

Comparative Errors



# Fe-Zeolite

## Summary and Conclusions (1)

- Aging of Catalyst for 2, 4, 8 and 16 Hours at 475, 550, 625 and 700°C  
Decreased  $\text{NH}_3$  Storage Capacity ( $\Omega$ )

Using 1<sup>st</sup> Order Rate Equation

- Deactivation Energy  $E_d$  determined to be 43 kJ/mol
- Pre-Exponential Factor A determined to be 118



# Fe-Zeolite

## Summary and Conclusions (2)

- Possible to Predict NH<sub>3</sub> Storage Capacity In-Field using Two Equations:

$$t_c = t_{c-1} + e^{\left[-\frac{Ed}{R}\left(\frac{1}{T_2} - \frac{1}{T_1}\right)\right]}$$

Equation 1

where  $t_c$  is the cumulative effective aging time,  $t_{c-1}$  is the previous cumulative effective aging time,  $Ed$  is the deactivation energy value (43 kJ/mol),  $R$  is the molar gas constant (0.00831451 kJ/mol/K),  $T_1$  is the given effective aging temperature and  $T_2$  is the current actual measured temperature

$$\Omega = \Omega_0 - t_c * \left[ \left( A * e^{\left(\frac{Ed}{RT_1}\right)} \right) * \Omega_0 + (x - yT_1) \right]$$

Equation 2

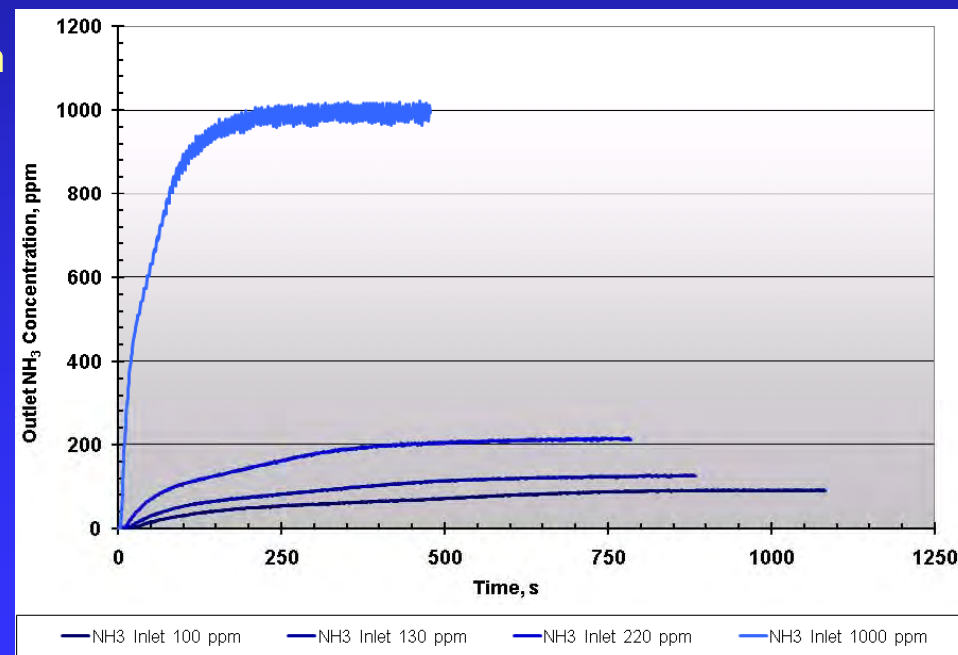
where  $\Omega$  is the current NH<sub>3</sub> storage capacity to be calculated,  $\Omega_0$  is the initial maximum NH<sub>3</sub> storage capacity (51.02 mol/m<sup>3</sup>),  $t_c$  is the effective aging time calculated using Equation 1,  $A$  is the pre-exponential factor (118),  $Ed$  is the deactivation energy value,  $R$  is the molar gas constant,  $T_1$  is the given effective aging temperature and  $x$  and  $y$  are constants (45.05 and 0.06454)



# V/W/TiO<sub>2</sub>

## NH<sub>3</sub> Adsorption Test Conditions

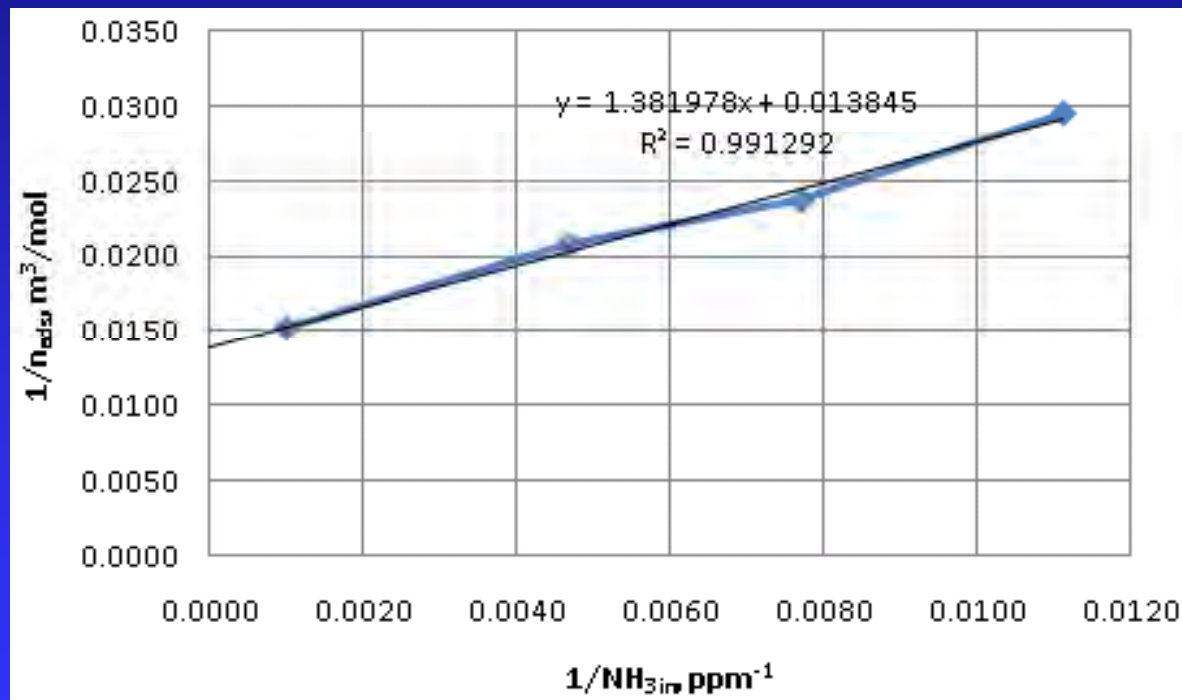
- Gas Mixture: 14% O<sub>2</sub>, 5% CO<sub>2</sub>, 5% H<sub>2</sub>O, X ppm NH<sub>3</sub>, balance N<sub>2</sub>
- Test Temperature 200°C
- Space Velocity 120,000 hr<sup>-1</sup>
- Catalyst 'cleaned' of NH<sub>3</sub> Between Test Points (NO + NO<sub>2</sub> + NH<sub>3</sub> fast reaction used)
- NH<sub>3</sub> setpoints 100, 130, 220, 1000 ppm
- Note Single Point Equilibration Times Still as Long as 37 Minutes Despite 100 ppm Lowest NH<sub>3</sub> Concentration



# V/W/TiO<sub>2</sub>

## NH<sub>3</sub> Adsorption Test Results (1)

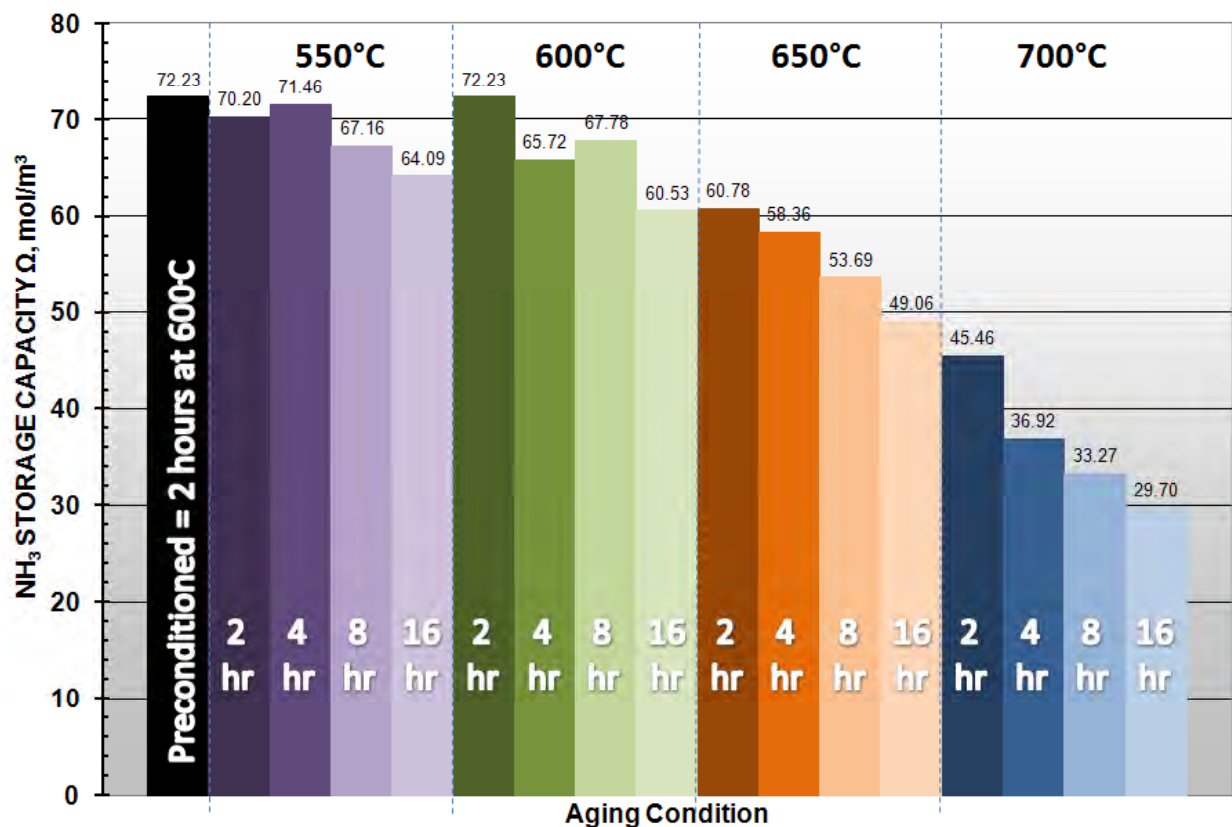
- Data fitted to Langmuir adsorption isotherm model by plotting the data in Langmuir coordinates
  - R<sup>2</sup> = 0.99, therefore NH<sub>3</sub> adsorption obeyed a Langmuir type isotherm well



# V/W/TiO<sub>2</sub>

## NH<sub>3</sub> Adsorption Test Results (2)

- NH<sub>3</sub> Storage Capacity Decreased with Aging Time and Temperature



- 550°C data includes some preconditioning, with deactivation at  $\geq 8$  hours
- 600°C data had inconsistent data points

550 and 600°C data could not readily be used for *Ed* calcs.



# V/W/TiO<sub>2</sub>

## Deactivation Energy Determination, $E_d$ (1)

### ● 1<sup>st</sup> Order Rate Equation with Variable Intercepts

Rate Equation

$$-d\Omega/dt = k\Omega + (x - yT)$$

$\Omega$  NH<sub>3</sub> storage capacity, mol/m<sup>3</sup>

$t$  time, hours

$k$  rate constant

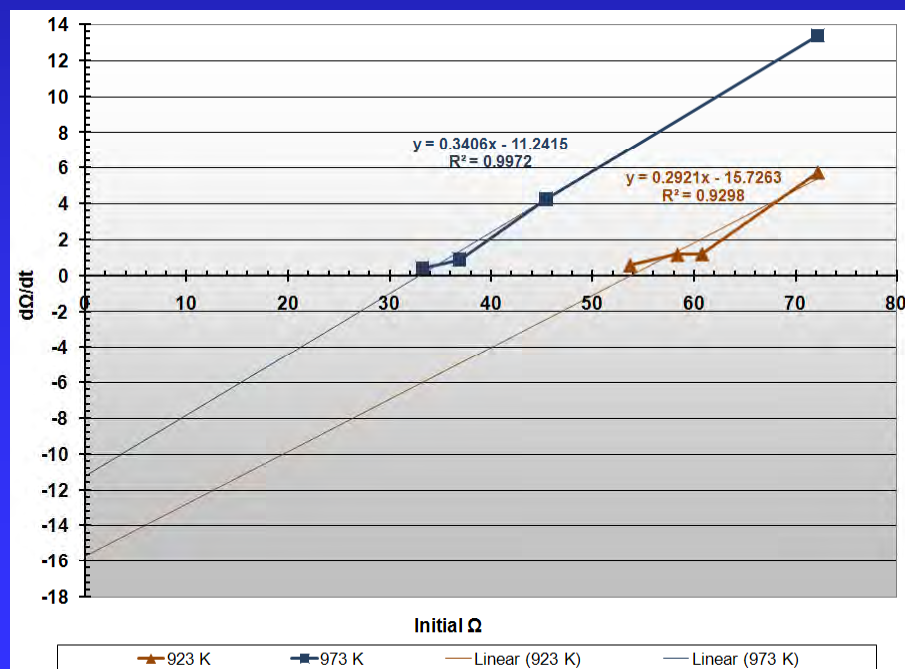
$T$  temperature, K

$x$  constant       $y$  constant

$$k = A e^{-(E_d/RT)}$$

Arrhenius Equation

- Only 650 and 700°C data used (550°C data includes conditioning, 600°C data inconsistent)

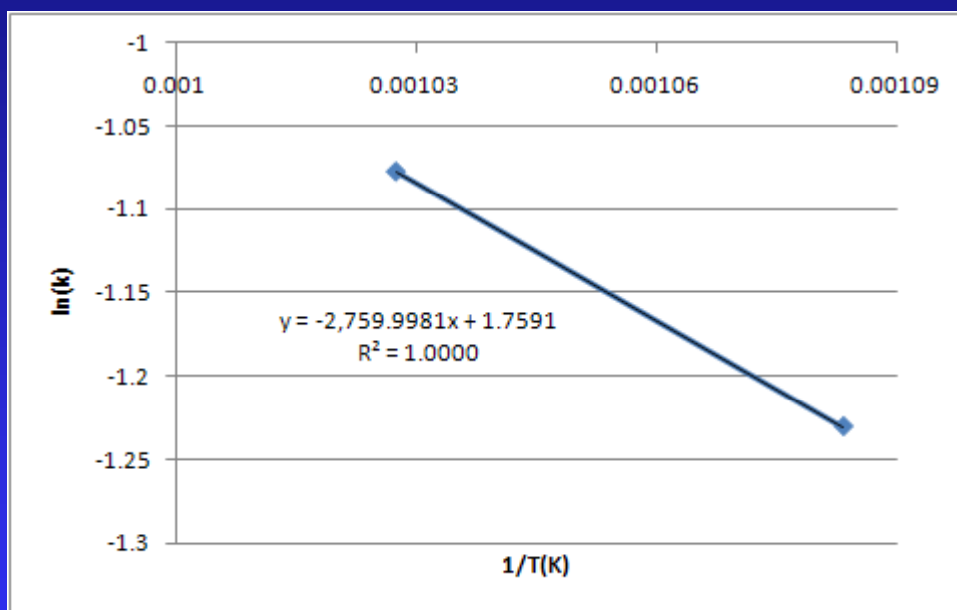


V/W/TiO<sub>2</sub>

## Deactivation Energy Determination, $E_d$ (2)

Arrhenius Equation Plots  $k = A e^{-(E_d / RT)}$

- Raw Data -  $E_d = 22.95$  kJ/mol  $A = 5.81$



Only two test points used. Therefore, repeat/verification testing highly recommended



# V/W/TiO<sub>2</sub>

## Deactivation Energy Determination, *Ed* (3)

- MS Excel Solver Used to Obtain Best Fit Constants
- Best fit - *Ed* = 98 kJ/mol *A* = 71971 *x* = 89.10 *y* = 0.10701

	MEASURED $\Omega$			
	TEMPERATURE, Kelvin			
Aging, Hrs	823.15	873.15	923.15	973.15
2	70.2	72.2	60.8	45.5
4	71.5	66.8	58.4	36.9
8	67.2	62.3	53.7	33.3
16	64.1	60.5	49.1	29.7

Test Data

	CALCULATED OMEGA 2			
	TEMPERATURE, Kelvin			
Aging, Hrs	823.15	873.15	923.15	973.15
2	64.0	66.9	62.5	46.1
4	56.6	60.3	57.6	44.3
8	42.9	52.0	49.7	28.7
16	20.2	44.3	51.2	29.7

Calculated Values using  
Rate Equation

-  $d\Omega/dt = k\Omega_1 + (x - yT)$   
and Best Fit Constants

	PERCENTAGE ERRORS			
	TEMPERATURE, Kelvin			
Aging, Hrs	823.15	873.15	923.15	973.15
2	--	--	2.78	1.40
4	--	--	1.32	19.94
8	--	--	7.47	13.78
16	--	--	4.38	0.15
Average % error =				6.40

Comparative Errors



# V/W/TiO<sub>2</sub>

## Summary and Conclusions (1)

- Aging of Catalyst for 2, 4, 8 and 16 Hours at 550, 600, 650 and 700°C  
Generally Decreased NH<sub>3</sub> Storage Capacity ( $\Omega$ )
- Deactivation Energy  $E_d$  determined to be 98 kJ/mol
- Pre-Exponential Factor A determined to be 71971
  - Only two aging temperatures used in calculations (650 and 700°C)
  - Repeat/verification testing highly recommended, but not performed in this work



# V/W/TiO<sub>2</sub>

## Summary and Conclusions (2)

- Possible to Predict NH<sub>3</sub> Storage Capacity In-Field using same two equations:

$$t_c = t_{c-1} + e \left[ -\frac{Ed}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right) \right]$$

Equation 1

$$\Omega = \Omega_0 - t_c * \left[ \left( A * e^{\left( \frac{Ed}{RT_1} \right)} * \Omega_0 + (x - yT_1) \right) \right]$$

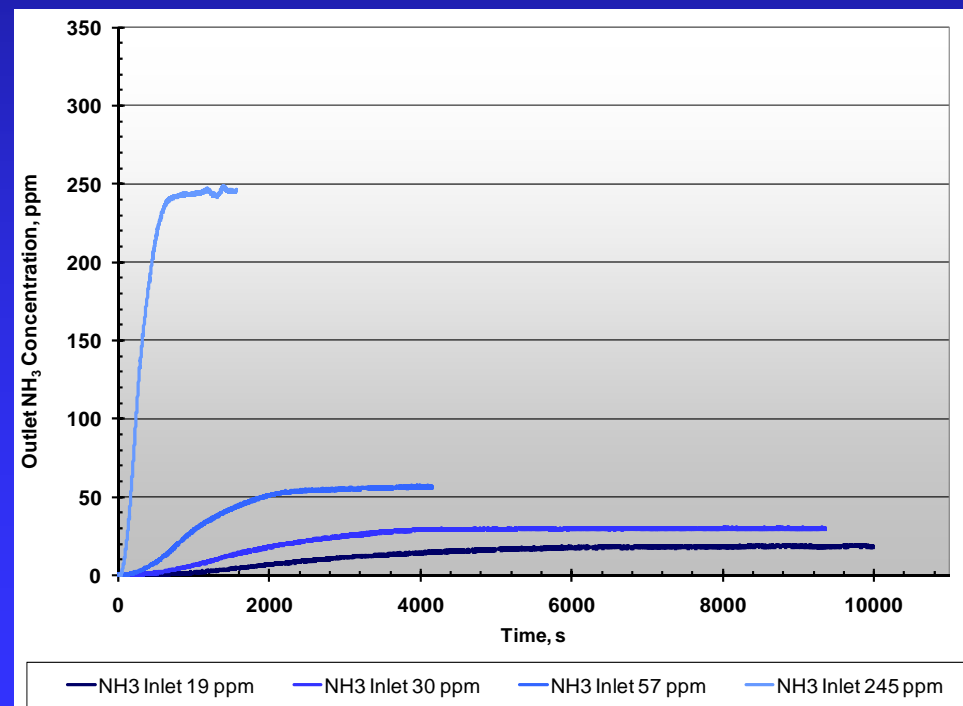
Equation 2



# Cu-Zeolite (New Data)

## NH<sub>3</sub> Adsorption Test Conditions

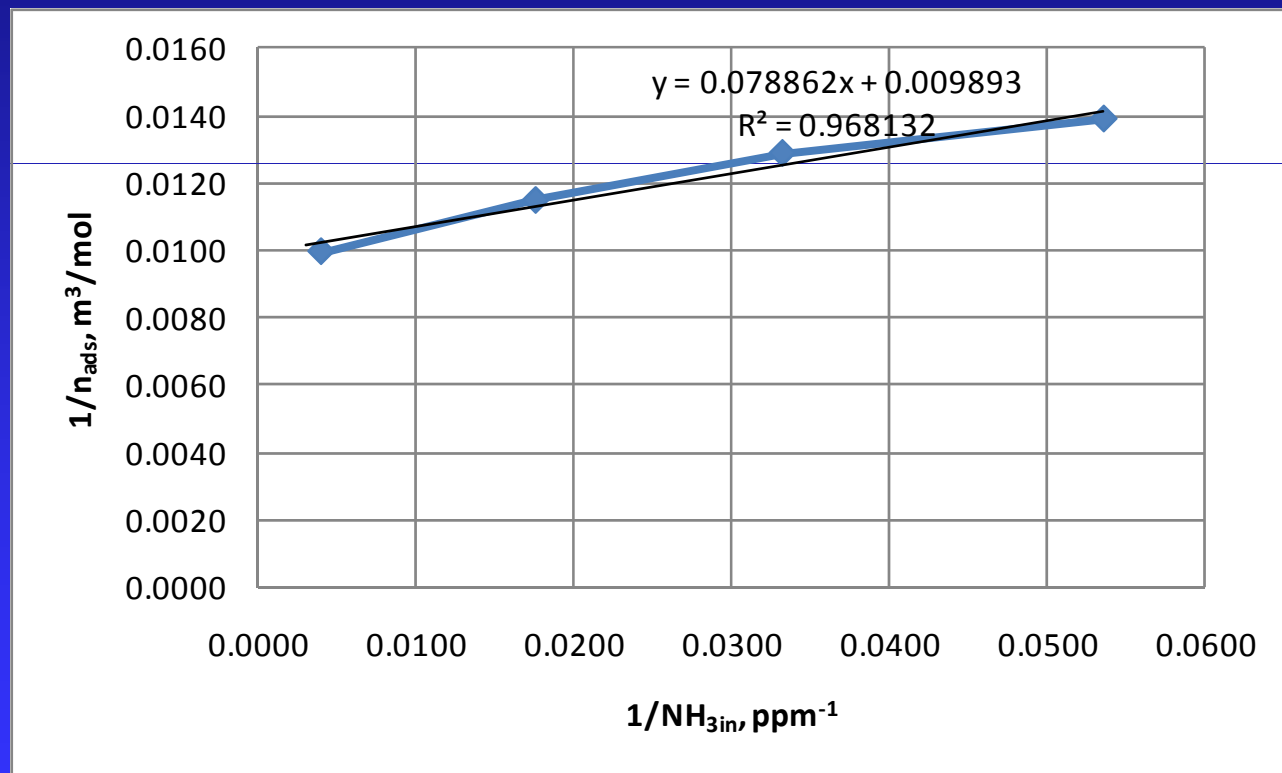
- Gas Mixture: 14% O<sub>2</sub>, 5% CO<sub>2</sub>, 5% H<sub>2</sub>O, X ppm NH<sub>3</sub>, balance N<sub>2</sub>
- Test Temperature 200°C
- Space Velocity 120,000 hr<sup>-1</sup>
- Catalyst 'cleaned' of NH<sub>3</sub> Between Tests (NO + NO<sub>2</sub> + NH<sub>3</sub> fast reaction used)
- NH<sub>3</sub> setpoints 20, 30, 50, 200 ppm
- Note Single Point Equilibration Times as Long as 2.8 Hours at 20 ppm NH<sub>3</sub> Concentration



# Cu-Zeolite (New Data)

## NH<sub>3</sub> Adsorption Test Results (1)

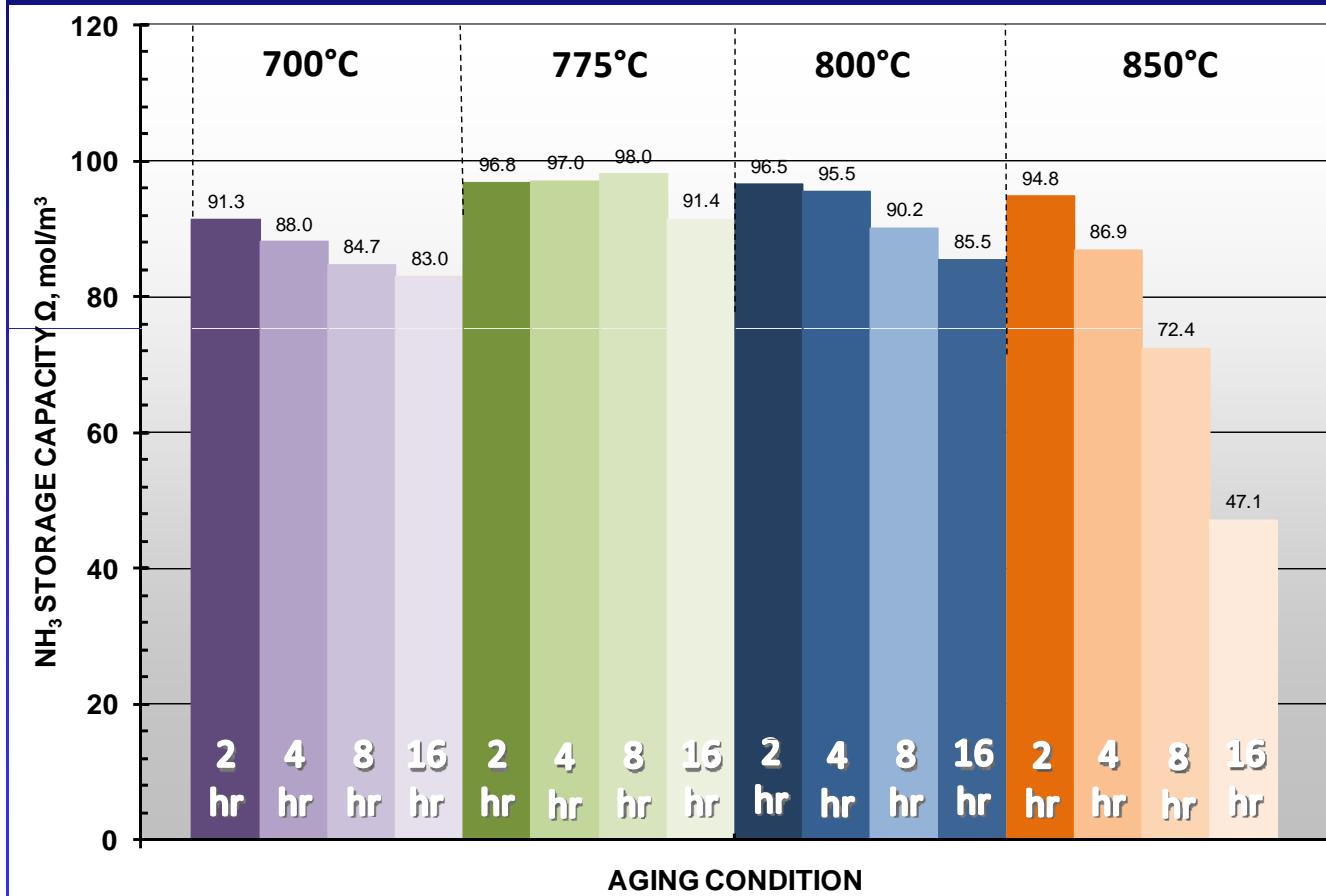
- Data fitted to Langmuir adsorption isotherm model by plotting the data in Langmuir coordinates
  - $R^2 \leq 0.97$ , NH<sub>3</sub> adsorption obeyed Langmuir type isotherm *reasonably* well



# Cu-Zeolite (New Data)

## NH<sub>3</sub> Adsorption Test Results (2)

- NH<sub>3</sub> Storage Capacity Decreased with Aging Time and Temperature



Maximum  $\Omega$  at 8 hours - 775°C

775°C data 'flat'. Not used in *Ed* calculations



# Cu-Zeolite (New Data)

## Deactivation Energy Determination, $E_d$ (1)

- A Zero Order Rate Equation Fit the Data Quite Well

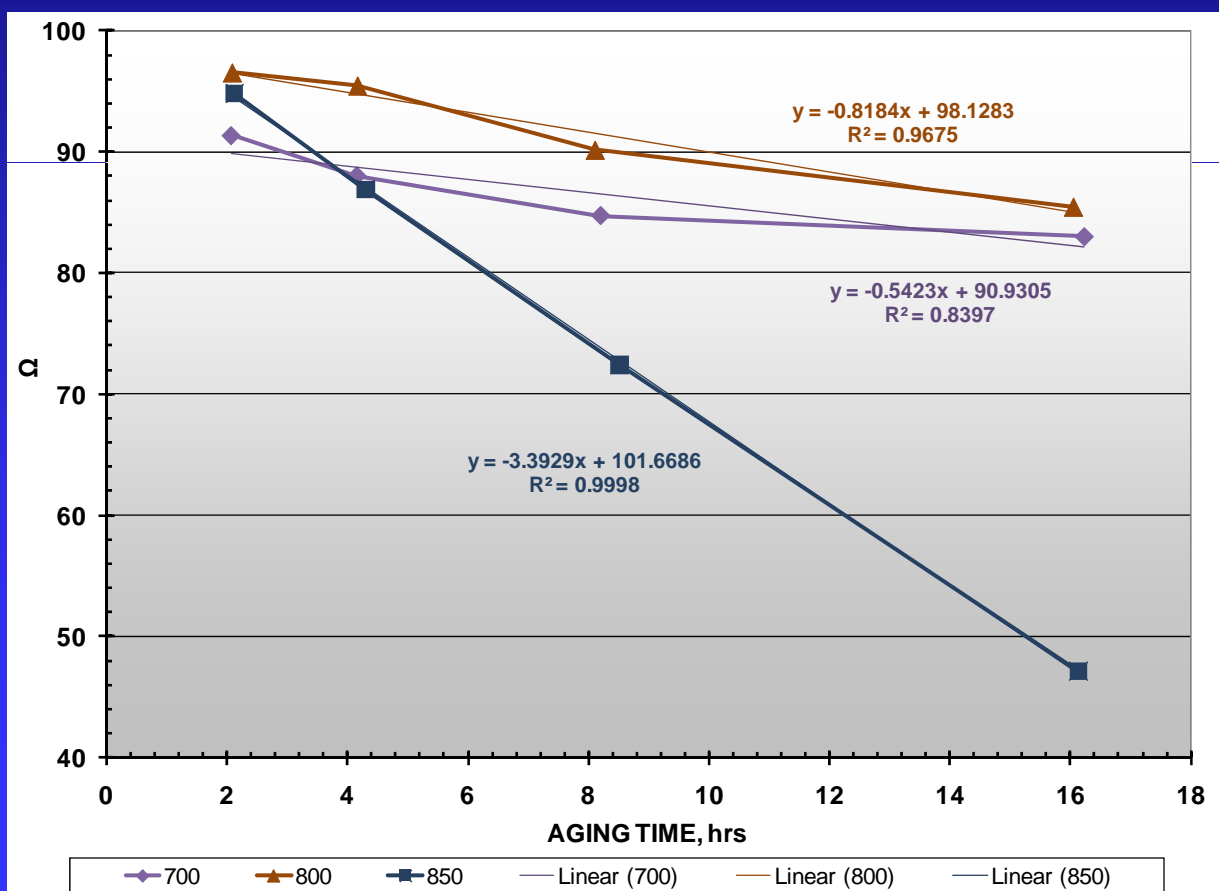
Rate Equation

$$-d\Omega/dt = k$$

$\Omega$   $\text{NH}_3$  storage capacity,  $\text{mol/m}^3$

$t$  time, hours

$k$  rate constant



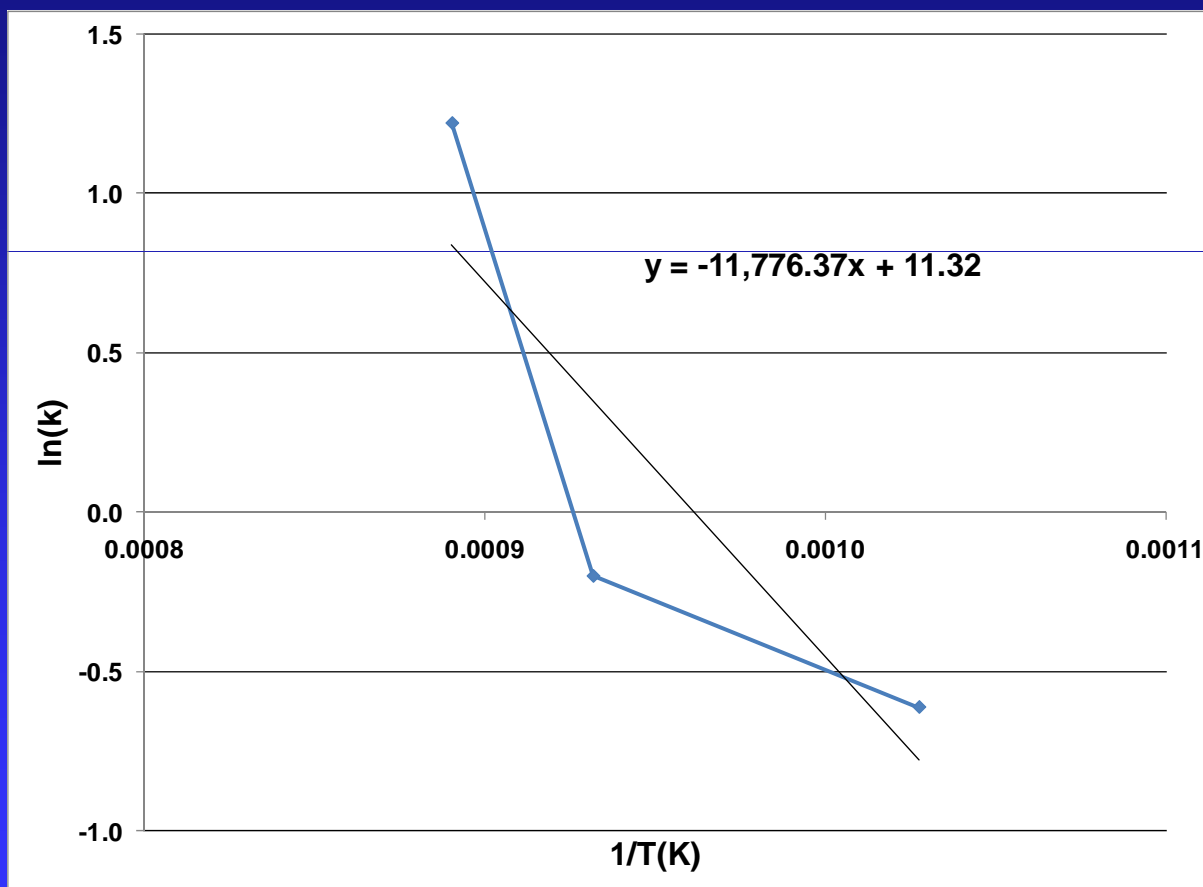
# Cu-Zeolite (New Data)

## Deactivation Energy Determination, $E_d$ (2)

- Arrhenius Equation Plot Using Zero Order Data Returns Values of:

■  $E_d = 98$  kJ/mol

■  $A = 82702$



# Cu-Zeolite (New Data)

## Deactivation Energy Determination, $E_d$ (3)

- MS Excel Solver Used to Obtain Best Fit Constants
- Best fit -  $E_d = 96$  kJ/mol  $A = 82703$

	MEASURED $\Omega$			
	TEMPERATURE, Kelvin			
Aging, Hrs	973.15	1048.15	1073.15	1123.15
2	91.4		96.5	94.8
4	88.0		95.5	86.9
8	84.7		90.2	72.4
16	83.0		85.5	47.1

Test Data

	CALCULATED $\Omega$			
	TEMPERATURE, Kelvin			
Aging, Hrs	973.15	1048.15	1073.15	1123.15
2	91.3		96.5	94.8
4	90.2		93.0	89.1
8	87.8		85.9	77.6
16	83.1		71.6	54.6

Calculated Values using  
Rate Equation  
-  $d\Omega/dt = k$   
and Best Fit Constants

	PERCENTAGE ERRORS			
	TEMPERATURE, Kelvin			
Aging, Hrs	973.15	1048.15	1073.15	1123.15
2	0.0		0.0	0.0
4	2.4		2.6	2.5
8	3.6		4.8	7.1
16	0.1		16.2	15.8
Average % error =		6.1		

Comparative Errors



# Cu-Zeolite

## Summary and Conclusions (1)

- Aging of Catalyst for 2, 4, 8 and 16 Hours at 700, 775, 800 and 850°C  
Generally Decreased  $\text{NH}_3$  Storage Capacity ( $\Omega$ )
- Deactivation Energy  $E_d$  determined to be 96 kJ/mol
- Pre-Exponential Factor A determined to be 82703



# Cu-Zeolite

## Summary and Conclusions (2)

- Possible to Predict  $\text{NH}_3$  Storage Capacity In-Field using equations:

$$t_c = t_{c-1} + e \left[ -\frac{Ed}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right) \right]$$

Equation 1

$$\Omega = \Omega_0 - t_c * \left[ \left( A * e^{\left( \frac{Ed}{RT_1} \right)} \right) \right]$$

Equation 3



## Summary and Conclusions

SCR Formulation	Maximum NH <sub>3</sub> Storage Capacity $\Omega$ , mol/m <sup>3</sup>	Deactivation Energy $E_d$ , kJ/mol
Fe-Zeolite	51	43
V/W/TiO <sub>2</sub>	72	98
Cu-Zeolite	97	96

- For SCR Catalysts, In-Use NH<sub>3</sub> Storage Capacity can be Calculated in Real Time using Only Operating Time and Temperature Measurements
  - Model-based controllers that rely on  $\Omega$  can utilize this methodology



# Acknowledgements

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- SwRI Advisory Committee for Research - Funding
- Johnson Matthey – V/W/TiO<sub>2</sub> Catalyst
- BASF – Cu/Zeolite and Fe/Zeolite Catalysts
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- SwRI - Dr. Reggie Zhan
- SwRI - Jason Miwa

