

### Three Way Catalyst and Lean NO<sub>x</sub> Trap Modeling for a Lean Burn SIDI Gasoline engine

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### Outline

- Background and objectives
- DeNO<sub>x</sub> modeling
  - Three way catalyst (TWC)
  - Lean NO<sub>x</sub> trap (LNT)
- Experimental setup
- Simulation results
- Summary

## Background

- Lean-burned SIDI engines show great benefit on fuel efficiency and CO<sub>2</sub> reduction

   Relatively higher nitrogen oxides (NO<sub>x</sub>)
- Reduce dependency on conventional fuels
  - Flexible fuel (fuel neutral) engines (e.g. gasoline & ethanol blends)
- Worldwide tightening emission regulations for light duty vehicles
  - NO<sub>x</sub>: Tier 2 Bin 5: 70 mg/mile;
  - LEV III: (NO<sub>x</sub>+NMOG) 30 mg/mile in 2025;
  - Euro 5+: 96 mg/mile
- Passive ammonia SCR system

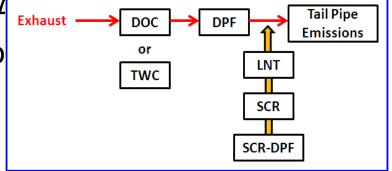
TWC

NH<sub>2</sub>

SCR

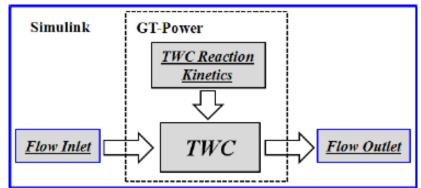
### **Objectives: Fuel-neutral AT Modeling**

- Development of DeNO<sub>x</sub> models with global kinetics
  - Reasonable accuracy over a wide range of (fuel neutral) engine exhaust conditions
  - NH<sub>3</sub> kinetics (global)
- Study the overall engine aftertreatment system (e.g. DeNO<sub>x</sub> + DeSoot)
  - Interactions among different A
  - Feedback to the engine perfo



### **TWC Reaction Kinetics**

- A single-channel, one-dimensional model
- Using GT-Power to solve conservation equations and chemistry
- 20 surface reactions (Ramanathan et al. 2011) ( in Langmuir-Hinshelwood structure)
  - Include kinetics for oxidation of CO, HC, and NO to  $CO_2$ ,  $H_2O$  and  $NO_2$
  - NO<sub>x</sub> reduction reactions
  - Water-gas shift and steam
  - Oxygen storage reactions
  - NH<sub>3</sub> kinetics
  - Proposed N<sub>2</sub>O kinetics

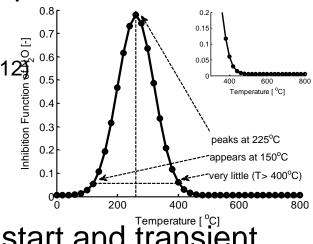


The detail of the TWC kinetics is reported in SAE paper 2013-01-1572

# NH<sub>3</sub> and N<sub>2</sub>O

#### NH<sub>3</sub>

- Commonly formed auries TWC/LNT Global mechanism (Ramanathan et al. 2012  $NO+2.5H_2 \rightarrow NH_3+H_2O$  $NO+1.5H_2O$  Commonly formed during the rich operation of

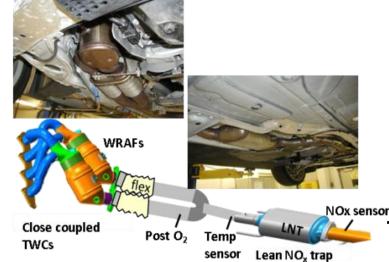


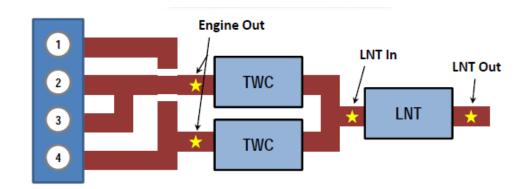
#### $N_2O$

- Predominantly formed during cold start and transient operations
  - A byproduct of NO<sub>x</sub> reduction by HCs during light-off
- Global mechanism
  - NO+1/18C<sub>3</sub>H<sub>6</sub>  $\rightarrow$  0.5N<sub>2</sub>O+1/6CO<sub>2</sub>+1/6H<sub>2</sub>O
  - $N_2O+1/9C_3H_6 \rightarrow N_2+1/3CO_2+1/3H_2O$

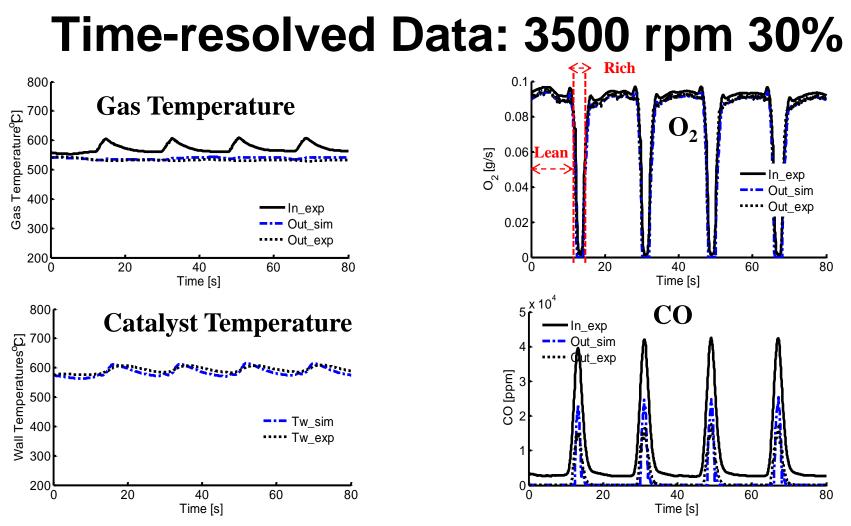
### **Experimental Setup**

 Lean gasoline vehicle (BMW120i – 2.0L L4) on a chassis dynamometer at ORNL (Parks et al. 2011)



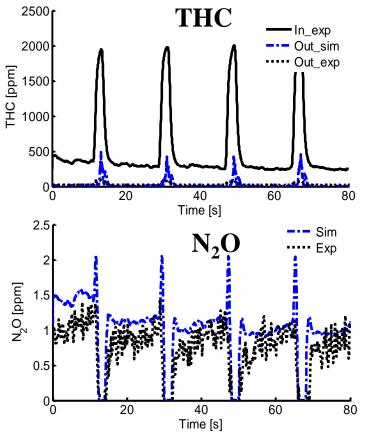


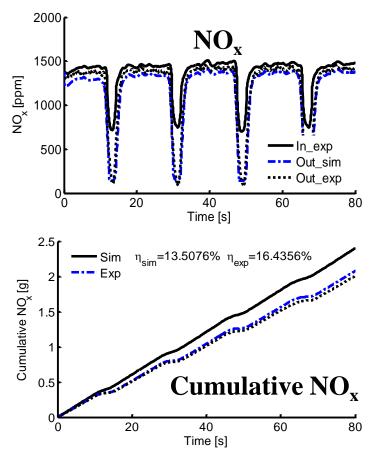
- Three different types of data for model validations
- Time-resolved (transient lean/rich cycle)
- Time-averaged (steady state lean/rich cycle)
- Transient driving cycle



- Gas & Catalyst temperatures match data
- O<sub>2</sub> and CO predictions are good

#### 3500 rpm 30%: THC/NO<sub>x</sub>/N<sub>2</sub>O

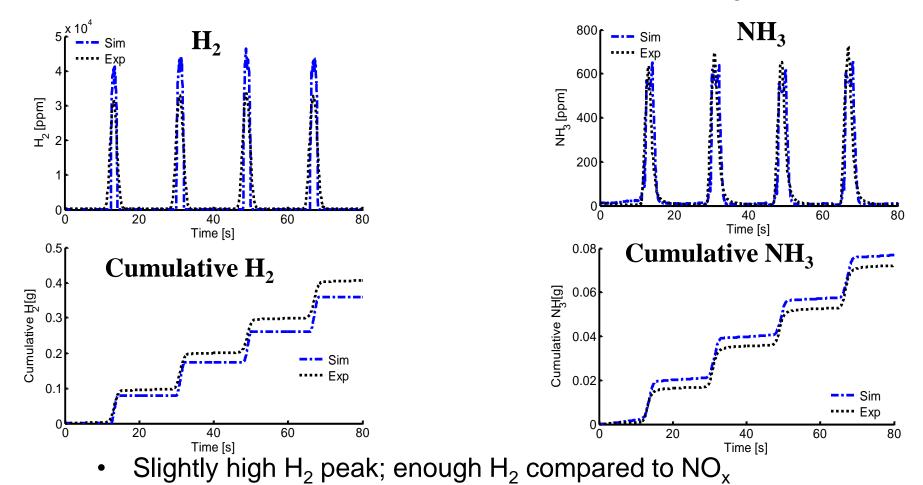




- Good predictions of THC
- Transient N<sub>2</sub>O is captured
- Instantaneous NO<sub>x</sub> and accumulative NO<sub>x</sub> are very comparable

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#### 3500 rpm 30%: H<sub>2</sub> & NH<sub>3</sub>



- Instantaneous NH<sub>3</sub> and accumulative NH<sub>3</sub> are very comparable
- NH<sub>3</sub>/inlet NO<sub>x</sub> = 0.072/2.4 ~ 3%

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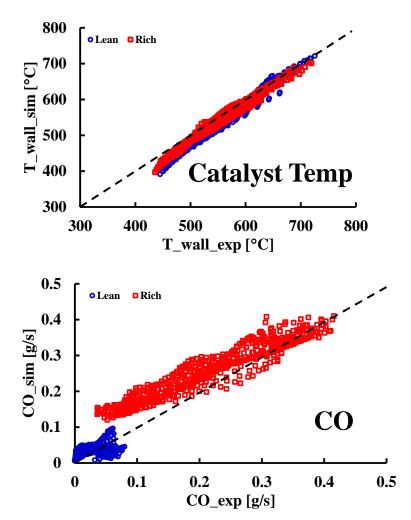
#### **Time-averaged Data**

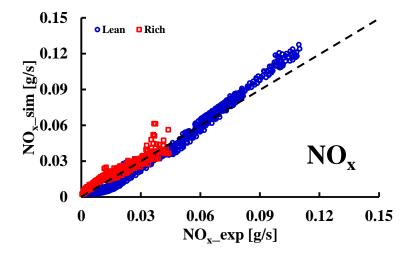
- Speed: 1500 to 4500, Load: 0~120 N·m
  - Total # of steady state operating conditions: 1550 (lean+rich)

Exhaust	Lean	Rich	3.5
Mass flow rate [g/s]	6.7 ~ 72.1	7.0 ~ 46.8	2.5 Lean period
Space velocity [1/s]	246.5 ~ 3737.4	291.0 ~ 2483.1	
Exhaust temp [°C]	336.6 ~ 716.4	412.7 ~ 681.7	$ \begin{array}{cccccccccccccccccccccccccccccccccccc$
Engine equiratio [-]	0.46 ~ 0.75	1.15 ~ 1.25	1
NO <sub>x</sub> [ppm]	156 ~ 2527.6	482.6 ~ 1532.7	0.5-
CO [ppm]	264.6 ~ 4125.7	13937 ~ 34680	0 100 200 300 400 500 600
HC [ppm]	19.4 ~ 870.5	294.7 ~ 1176.4	Time [s]

No detailed instantaneous species concentrations
 Examining the kinetics in a wide window of exhaust conditions

#### **Time-averaged Data**

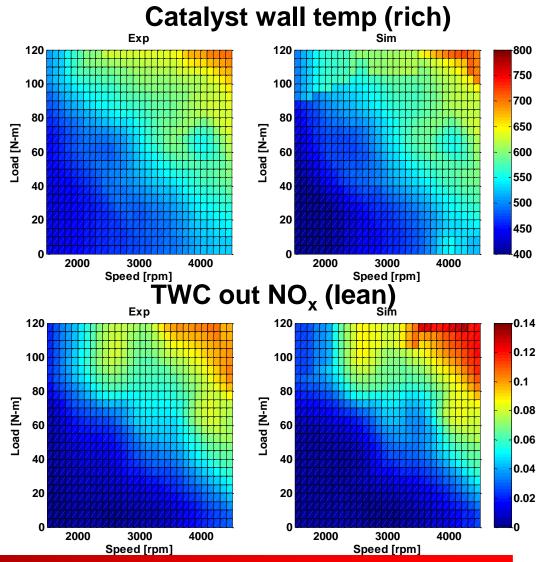




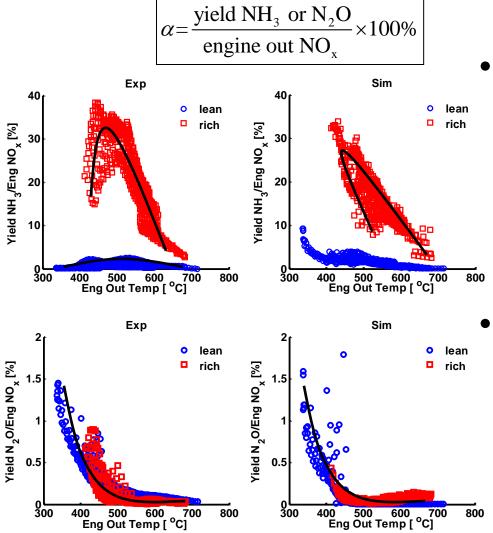
- Good agreement of temperatures and NO<sub>x</sub> emissions at lean & rich
- Some discrepancy in CO
  - Consistent with underpredictions of temperatures

### **Phasing Comparisons**

 A good agreement between predicted catalyst temperature, NO<sub>x</sub> and experimental data



## NH<sub>3</sub> & N<sub>2</sub>O kinetics



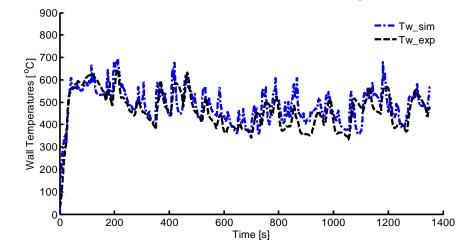
NH<sub>3</sub>

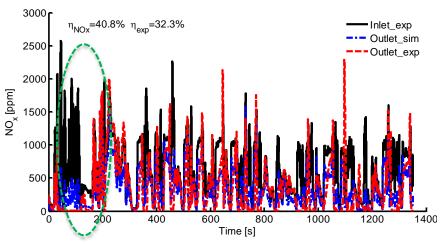
- mainly formed at rich
- Some discrepancy at low exhaust
  - temperatures (<400 °C)
- Over-predicted at lean

N<sub>2</sub>O – Independent of AFR

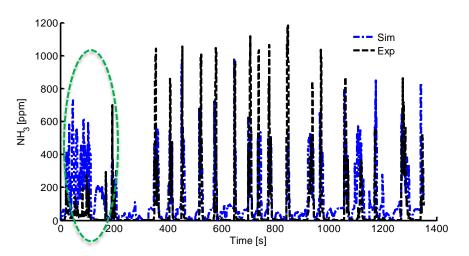
- Significantly depends on exhaust temperature
  - Favors at low temp

#### FTP Cycle (cold start)





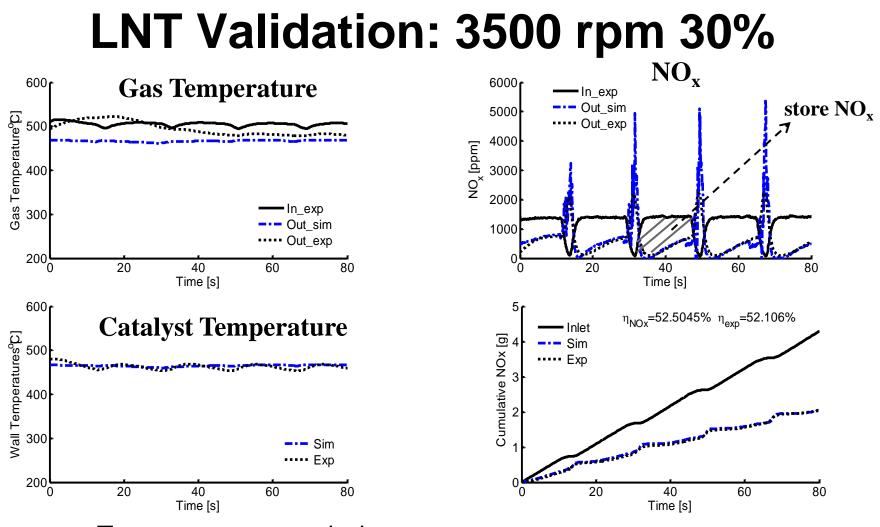
- Model captures the trends of catalyst temp, NO<sub>x</sub> and NH<sub>3</sub>
- Higher NO<sub>x</sub> and NH<sub>3</sub> in the first 200 seconds
  - Might be some NOx storage functionality in the TWC (not in the model)



#### **LNT Kinetics**

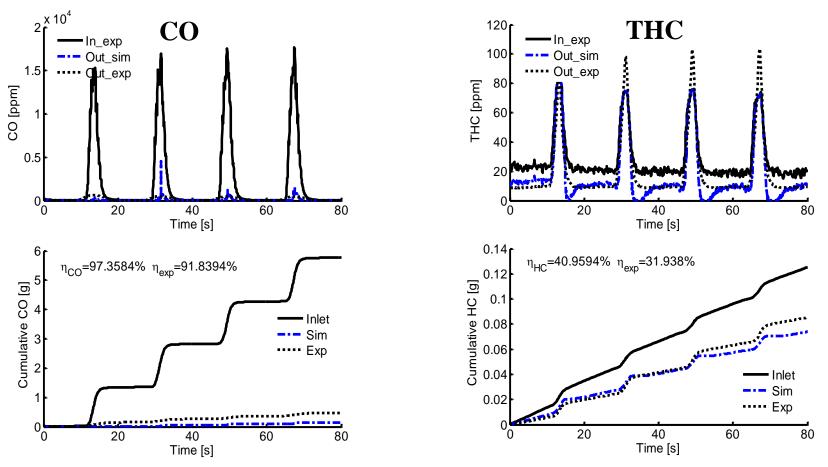
LNT kinetics				
1	$CO+0.5O_2 \rightarrow CO_2$			
<b>2</b> $C_3H_6+4.5O_2 \rightarrow 3CO_2 + 3H_2O$		Oxidation reactions		
<b>3</b> $C_3H_8 + 5O_2 \rightarrow 3CO_2 + 4H_2O$				
4	$H_2 + 0.5O_2 \leftrightarrow H_2O$			
5	NO+0.5 $O_2 \rightarrow NO_2$	NO NO <sub>2</sub> transition		
6	$CO + NO \rightarrow CO_2 + 0.5N_2$	NO reduction		
7	$1/9C_{3}H_{6}+NO \rightarrow 1/3CO_{2}+1/3H_{2}O+1/2N_{2}$			
8	0.5BaCO <sub>3</sub> +NO+0.75O <sub>2</sub> →0.5Ba(NO <sub>3</sub> ) <sub>2</sub> +0.5CO <sub>2</sub>	NO adsorption		
9	0.5BaCO <sub>3</sub> +NO <sub>2</sub> +0.25O <sub>2</sub> →0.5Ba(NO <sub>3</sub> ) <sub>2</sub> +0.5CO <sub>2</sub>	NO <sub>x</sub> adsorption		
10	$0.5Ba(NO_3)_2+1.5CO \rightarrow 0.5BaCO_3+NO+CO_2$			
11	$Ba(NO_3)_2 + 1/3C_3H_6 + CO_2 \rightarrow BaCO_3 + 2NO + H_2O$	NO <sub>x</sub> desorption		
12	$Ba(NO_3)_2 + 8H_2 + CO_2 \rightarrow 2NH_3 + BaCO_3 + 5H_2O$	NH <sub>3</sub> formation from nitrates		
13	$NH_3 + 0.5Ba(NO_3)_2 + 0.5CO_2 \rightarrow N_2O + 0.5BaCO_3 + 1.5H_2O$	N <sub>2</sub> O formation from nitrates		
14	$NH_3 + 4NO \rightarrow 2.5N_2O + 1.5H_2O$	N <sub>2</sub> O formation		
15	$NO+2.5H_2 \rightarrow NH_3 + H_2O$	NH <sub>3</sub> formation		
16	$NH_3+1.25O_2 \rightarrow NO+1.5H_2O$	$NH_3$ oxidation		
17	NH <sub>3</sub> +1.5NO→1.25N <sub>2</sub> +1.5H <sub>2</sub> O	NH <sub>3</sub> and NO		

• Total 17 reactions (Olsson et al. 2005)



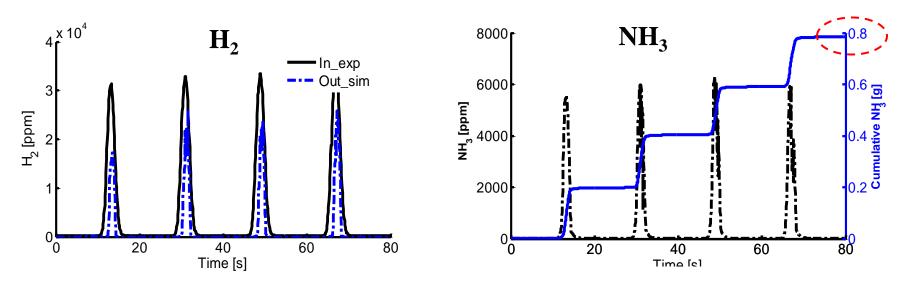
- Temperatures match data
- NO<sub>x</sub> adsorption & desorption & reduction are well captured

#### **LNT Validation: CO & THC**



- Slightly lower CO but with reasonable overall conversion rate
- Both instantaneous and accumulative HCs are good

### LNT Validation: H<sub>2</sub> & NH<sub>3</sub>



- A large amount of H<sub>2</sub> from TWC
- Peak  $NH_3$  is higher than  $NO_x$  (6000 vs. 5000)
  - Generated from nitrates (different from TWC)
  - $NH_3$ /inlet NO<sub>x</sub> = 0.8/4.2 ~ 20%

### Summary

A TWC and a LNT model were developed with global kinetics and validated using experimental data from a lean burn DISI engine

- TWC
  - Validated over a wide range of exhaust conditions
  - Temperature dependences of the conversion rate of  $NH_3$ and  $N_2O$  from  $NO_x$  were examined
- LNT
  - NO<sub>x</sub> adsorption, desorption and reduction were well captured
  - NH<sub>3</sub> formation from LNT could be much more than TWC
  - Need NH<sub>3</sub> kinetics from nitrates

<u>The DeNO<sub>x</sub> models are able to predict the temperatures</u> as well as species concentration with a good accuracy.

### Acknowledgment

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# Thank You !

#### For further questions, please contact:

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