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11th DOE CLEERS Workshop

May 13-15, 2008

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# <u>Outline</u>

- Soot Reactivity
  - Definition
  - Determining Factors
  - Significance
  - Activities at Penn State
- Experimental
- Thermal & Kinetic Analysis
- Conclusions



### Soot Reactivity

Soot oxidative reactivity can be defined as the ease to burn-off Soot at low temperature and/or short time

- ✤ Fuel source
  ➢ Biodiesel soot vs. diesel soot
- Combustion conditions
  Low engine load vs. high engine load
  EGR effects



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2hr





# Soot Morphology and Nanostructure



TEM of diesel soot aggregate composed of many primary particles.

HRTEM of diesel soot primary particles exhibit "*turbostratic*" structure : randomly oriented fringes in the core, long and concentrically arranged fringes at the outermost



# Soot Issues and Implications

- Diesel soot is a byproduct carcinogenic carrier results from poor combustion
- Diesel particulate filter (DPF) and exhaust gas recirculation (EGR) to control PM and NOx emissions, respectively.
- EGR suppresses NOx formation but increases PM emissions
  - The DPF physically captures the resulting PM and prevent its release to the atmosphere

#### **PROBLEM:**

- Diesel soot requires temperature higher than 500°C to oxidize in air in DPFs
- Diesel exhaust temperature range is 250 350°C.

#### **SOLUTIONS:**

- Increase engine exhaust temperature (e.g., engine management) → DPF damage
- Enhance soot oxidative reactivity (FBC, nanostructure manipulation).





# Activities at Penn State

- 1. Previous observations on impacts of fuel formulation on diesel soot nanostructure and reactivity
  - Enhanced reactivity of B100 soot arises from surface oxygen functional groups and leads to a unique oxidation process
  - Diesel soot (from neat FT diesel) follows a "shrinkage core" oxidation process
- 2. How will EGR affect the formation, maturation, and oxidation kinetics of diesel soot?
  - Reduced temperature may affect the pool of soot precursors and alter the transition to an ordered and graphitic structure
  - Shift gas composition from EGR (less O<sub>2</sub> and more CO<sub>2</sub>) may exert chemical effects on the soot formation process
  - i.e., three effects may be present- thermal, chemical, and

### **Experimental Approach**

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# **Experimental Techniques**

- Thermogravimetric Analysis (TGA) Instrument
  - Reactivity Measurements
    - ✓ Isothermal in Air @ 450 °C
    - $\checkmark$  Oxygen chemisorption  $\rightarrow$  active sites
  - □ Kinetic Analysis
    - ✓ Non-isothermal in Air, heating rates ( $\beta$ ) of 1.5, 3, 5, and 7 °C/min
      - o Compared to Isothermal
        - fast
        - allows for multiple runs / day (repeatability check)
        - less expensive
        - yet, less accurate
  - $\Box$  All soot samples were heat-treated in N<sub>2</sub> to remove the volatile fraction
- Supportive Techniques
  - ✤ X-Ray Diffraction (crystallite width → active sites)
  - HRTEM (burning mode)



### Soot Active Sites

Active Sites are defined as the carbon atoms which have high affinity to *chemisorb* and *react* with oxygen →analogous to catalyst







Specific rate vs. conversion profiles of flame and diesel engines soot.

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### Impact of Oxidizer Diluents Isothermal TGA in air @ 450 °C.

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# Characterization of *Initial* Active Sites

 $C = C^* + (C_s) + C(O)$ 

Soot Symbol	Soot Origin	Amount of Chemisorbed Oxygen		
		Oxygen Uptake (g <sub>oxygen</sub> / g <sub>soot</sub> )	<i>ASA<sub>i</sub></i> (m² / g)	
FO	Diffusion flame (0% CO <sub>2</sub> )	0.00704	22.0	
F15	Diffusion flame (15% CO <sub>2</sub> )	0.0144	45.0	
SCE0	SCE (0% CO <sub>2</sub> )	0.00544	17.0	
SCE8	SCE (8% CO <sub>2</sub> )	0.01056	33.0	
MCE0	MCE (0% EGR)	0.00352	11.0	
MCE20	MCE (20% EGR)	0.00832	26.0	

To retain the initial nanostructure of the soot, no heat-treatment was applied to remove the oxygen complexes C(O) from soot surfaces



# Nanostructural Analysis

#### The Edge Site Carbon



Reactivity of edge site carbon is much higher than that of basal plane carbon:  $C_e/C_b \alpha ASA_i \alpha (1/L_a)$ 

Soot Symbol	Soot Origin	L <sub>a</sub> (nm)	<b>C</b> <sub>e</sub> / <b>C</b> <sub>b</sub>	ASA <sub>i</sub> (m² / g)
F0	Diffusion flame (0% CO <sub>2</sub> )	2.587	0.184	22.0
F15	Diffusion flame (15% CO <sub>2</sub> )	<b>*</b> 2.049	0.218	45.0
SCE0	SCE (0% CO <sub>2</sub> )	3.030	0.165	17.0
SCE8	SCE (8% CO <sub>2</sub> )	2.477	0.190	33.0
MCE0	MCE (0% EGR)	2.919	0.169	11.0
MCE20	MCE (20% EGR)	<b>•</b> 2.526	0.188	26.0

L<sub>a</sub> from XRD

C<sub>e</sub>/C<sub>b</sub> was determined in accordance to a theoretical assessment performed by Belenkov [Belenkov, 2000]



# **Soot Oxidation Kinetics**

How do EGR and CO<sub>2</sub> change soot oxidation kinetics?

• Determination of the kinetic parameters of soot oxidation of diverse soot samples: Activation Energy (*Ea*), Pre-exponential Factor (*A*), reaction order *w.r.t.* soot (*n*)

#### **APPROACH**

- The analysis is based on multiple nonisothermal TGA experiments
- Determine (*Ea*) without knowledge about the reaction model *a priori*
- Estimate (A) by using the compensation effect correlation
- Estimate (*n*) by assuming an appropriate reaction model
- Develop a simplified model that describes the oxidation process



### Soot Oxidation Kinetics 1. Activation Energy

#### **Theoretical Background**

- A model-free isoconversional method from nonisothermal data was used
- Basis: Kissinger, Akahira, and Sunose (KAS)

$$\ln\frac{\beta}{T^2} = \ln[\frac{AE}{Rg(X)}] - \frac{E}{RT}$$

T: T (X,  $\beta$ ) X: conversion  $\beta$  : heating rate g(X): reaction model



#### Conversion model functions g(X) for solid state reactions

No.	Reaction model	Symbol	$g(\alpha)$
1	Nucleation and growth (Avrami-Erofeev equation)	A <sub>1.5</sub>	$(-\ln(1-\alpha))^{1/1.5}$
2	Nucleation and growth (Avrami–Erofeev equation)	$A_2$	$(-\ln(1-\alpha))^{1/2}$
3	Nucleation and growth (Avrami–Erofeev equation)	$A_3$	$(-\ln(1-\alpha))^{1/3}$
4	Nucleation and growth (Avrami-Erofeev equation)	$A_4$	$(-\ln(1-\alpha))^{1/4}$
5	Phase boundary controlled reaction (contracting linear)	$P_1$	α
6	Phase boundary controlled reaction (contracting area)	$P_2$	$(1 - (1 - \alpha)^{1/2})$
7	Phase boundary controlled reaction (contracting volume)	$P_3$	$(1 - (1 - \alpha)^{1/3})$
8	One dimensional diffusion	$D_1$	$\alpha^2$
9	Two dimensional diffusion	$D_2$	$(1-\alpha)\ln(1-\alpha)+\alpha$
10	Three dimensional diffusion	$D_3$	$(1 - (1 - \alpha)^{1/3})^2$
11	Ginstling-Brounshtein equation	$D_4$	$(1-2/3\alpha) - (1-\alpha)^{2/3}$
12	Chemical reaction (first order)	$R_{1}, A_{1}$	$(-\ln(1-\alpha))$
13	Chemical reaction (second order)	$R_2$	$(1-\alpha)^{-1}-1$
14	Power law I	$L_1$	$\alpha^{1/4}$
15	Power law II	$L_2$	$\alpha^{1/3}$
16	Power law III	$L_3$	$\alpha^{1/2}$
17	Power law IV	$L_4$	$\alpha^{3/2}$
18	Zhuravlev equation	$D_5$	$[(1-\alpha)^{-1/3}-1]^2$



### Soot Oxidation Kinetics 1. Activation Energy

#### Isoconversional plots at various degrees of conversions









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- Ea is not affected by soot formation condition
- · Ea averaged values are Identical for both cases



### Soot Oxidation Kinetics 2. Pre-exponential factor

$$\ln \frac{\beta}{T^2} = \ln \left[\frac{AE}{Rg(X)}\right] - \frac{E}{RT}$$
  
Which g (x)??  
Compensation effect relationship

$$\ln(A_j) = a + bE_j$$



Linear relationship of the compensation effect for (a) MCE0 soot and (b) MCE20 soot.





### Soot Oxidation Kinetics 3. Reaction order w.r.t. soot

Non-isothermal oxidation can be expressed as

$$\frac{dX}{dt} = \left(\frac{A}{\beta}\right) \exp\left(\frac{-E_a}{RT}\right) f(X)$$

Integrating this equation and assuming a proper model to describe soot oxidation:

$$g(X) = [-\ln(1-X)]^{\frac{1}{n}}$$

yield

$$\ln(\frac{\beta R}{E}) - \ln[p(y)] = \ln(A) - (\frac{1}{n})\ln[-\ln(1-X)]$$



Estimation of soot reaction order, *n*, for (a) MCE0 soot and (b) MCE20 soot





### Soot Oxidation Kinetics Summary

	F0	F15	SCE0	SCE8	MCE0	MCE20
E <sub>a</sub> (kJ/mol)	165	165	152	153	165	165
A (1/s)	7.3E8	1.3E9	1.86E8	2.7E8	2.8E8	4.3E8
n	0.79	0.79	0.90	1.0	0.97	0.77

E<sub>a</sub> is not affected by soot properties



RDS is the same & soot follows the same oxidation mechanism irrespective of its formation condition Formation of oxygen complex  $2Cs + O2 \rightarrow 2Cs(O)$ 

Decomposition of oxygen complex  $C_s(O) \rightarrow CO + Cs$  $2Cs(O) \rightarrow CO2 + Cs$ 

Pre-exponential factor (A) correlates with the observed decrease of  $(L_a) \rightarrow$  increased (ASA) Effects of active sites are incorporated implicitly in (A)



(a) MCE0 soot, and (b) MCE20 soot.



#### Oxidation consequence of soot generated under 0% EGR



#### Oxidation consequence of soot generated under 20% EGR



unreacted

25% oxidized

50% oxidized

∠ 75% oxidized



# CONCLUSIONS

#### **CONCLUSIONS:**

- The addition of EGR
  - enhances the oxidative reactivity of the soot
  - has no effect on the activation energy of soot oxidation, the observed increased in reactivity is attributed solely to the increase of active sites which are incorporated implicitly in the pre-exponential factor
  - facilitates oxygen dissociation on soot surfaces
  - does not affect the rate-limiting step of the oxidation reaction



# ACKNOWLEDGMENTS

- Linda Blevins (former project manager) and Phil Westmoreland (current project manager) of National Science Foundation (Grant# CTS-0553339)
- US DOE-National Energy Technology Laboratory
- This presentation was prepared with partial support from the U.S. Department of Energy under Contract No. DE-FC26-03NT41828. The Government reserves for itself and others acting on its behalf a royalty-free, nonexclusive, irrevocable, worldwide license for Governmental purposes to publish, distribute, translate, duplicate, exhibit, and perform this copyrighted paper.
- **\*** Ryan Harrier and Keith Cavallini of CAV Engineering
- Barry Dobar and Diana Dupuie of VM Motori NA
- Yu Zhang, Vince Zello, Dr. Joe Kulik (Materials Research Institute) and Prof. John Badding (Dept. of Chemistry) of Penn State University



### Thank you for your attention!