

# Effectiveness of Desulfation Protocols on Dynamometer Aged LNT-SCR Systems

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# Presentation Outline

- Dynamometer Aging
  - Experimental Set-up
  - 2- Desulfation Protocols (50,000 miles equivalent)
  - System Performance after Aging
- Effect of Protocol Sulfur Release
- Effect of Aging on Sulfur Release
- Accelerated Aging Conditions
  - Average/Peak Temperatures
  - Rich Time
  - HC and CO

# LNT-SCR Concept for Lean NOx Reduction

## Typical System

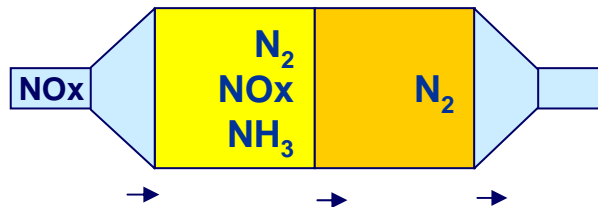
NOx Adsorber



NOx Adsorber Vol = 2x PGM = 2y

## New System

NOx Adsorber In-situ-SCR



NOx Adsorber  
In-situ SCR

Vol = 1x PGM = 1y  
Vol = 1x PGM = 0

- Products of LNTs NOx reduction include N<sub>2</sub> and NH<sub>3</sub>.
- Replace 1/2 of lean NOx trap volume with ammonia SCR catalyst.
- Improves Net NOx conversion (to N<sub>2</sub>)



# 50,000 mile Equivalent Aging Protocol for LNT-SCR System on Engine Dynamometer

Steady Engine Operation at 2000 rpm / 4 bar

## MODE #1

Sulfur Exposure

DeNO<sub>x</sub> = 345°C

L(s)/R(s) = 120/5

## MODE #2

DeSO<sub>x</sub>\* = ~670°C

L(s)/R(s)

## MODE #3

DPF Regen – 600°C

Lean Only

## Desulfation Targets:

**System A: 700°C ± 20°C**

**System B: 650°C ± 70°C**

*Average midbed temperature controlled by alternating between rich and lean post-injected engine operation.*

# Experimental Set-up and Measurement

Temperature at LNT Midbed

Midac FTIR  
(NO, NO<sub>2</sub>, NH<sub>3</sub>)

DOC (1.25L)

Diesel  
Engine  
2.2L

FTIR measurement taken  
sequentially at each  
location for evaluations.

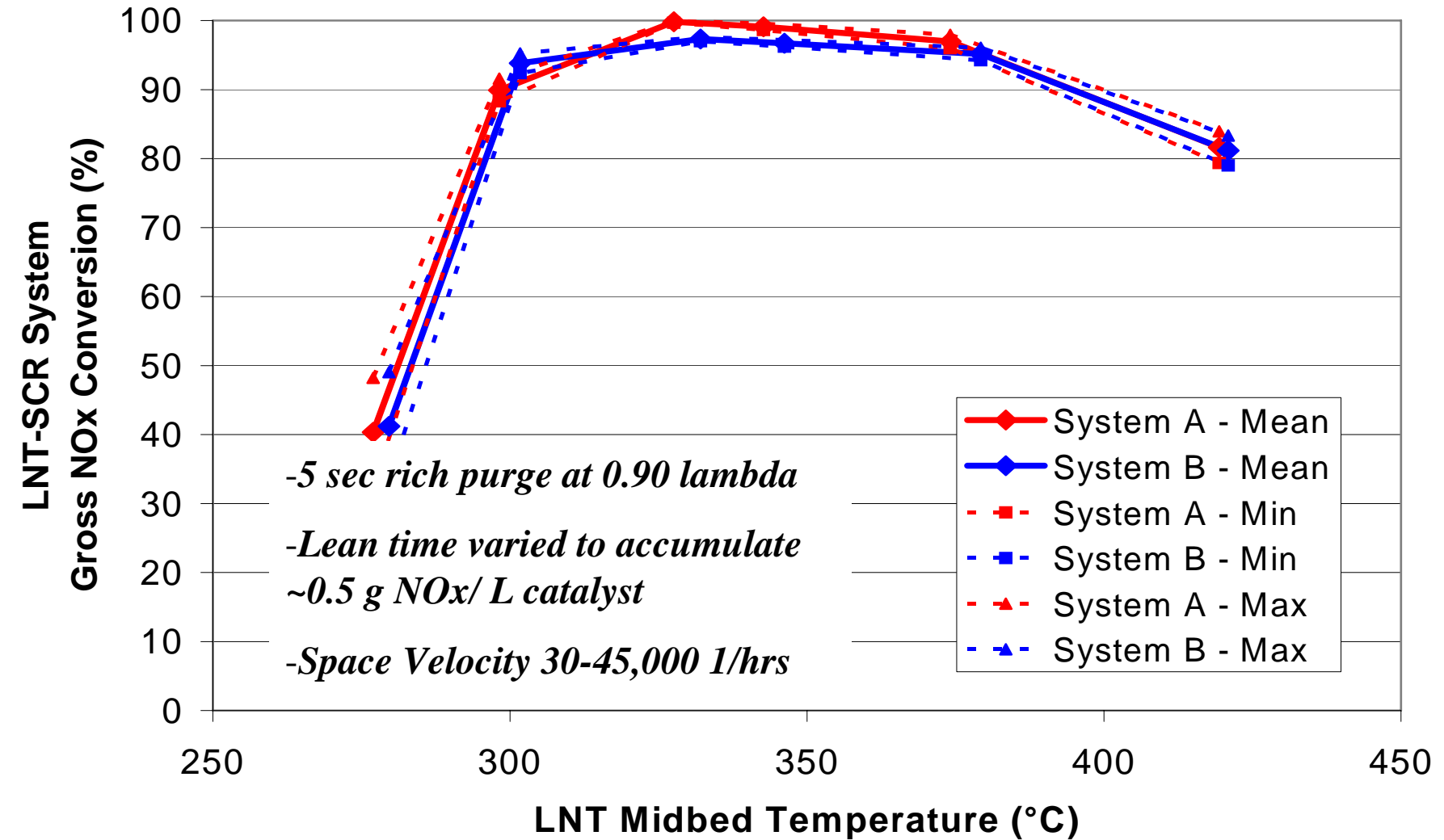
Horiba MEXA 7100 Gas  
Analyzers (CO, THC)

LNT (2.5L)

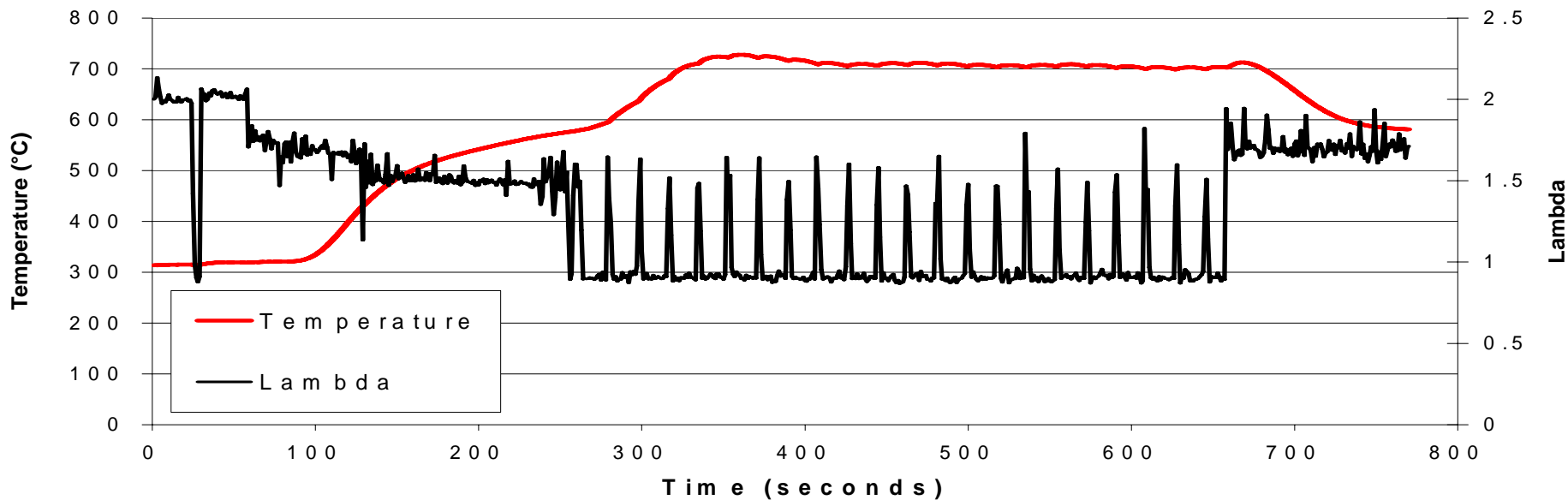
SCR (2.5L)

V&F Mass  
Spectrometer  
(SO<sub>2</sub>, H<sub>2</sub>S, COS)

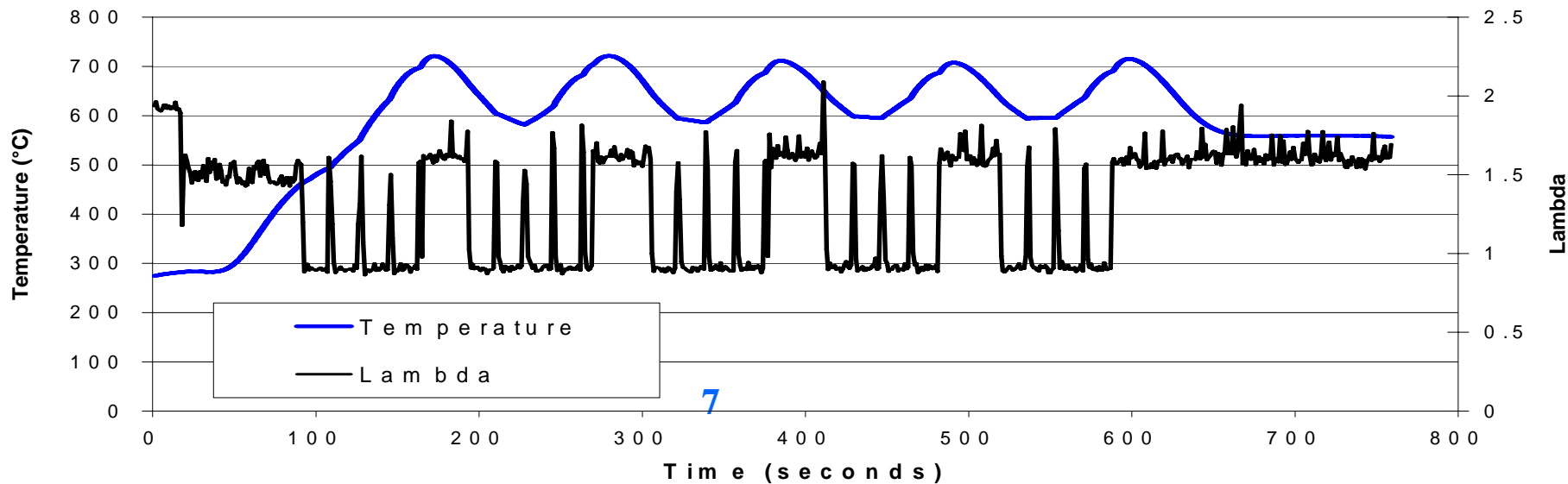
# LNT-SCR Gross NO<sub>x</sub> Conversion After 50,000 mi Equivalent Aging on Engine Dynamometer



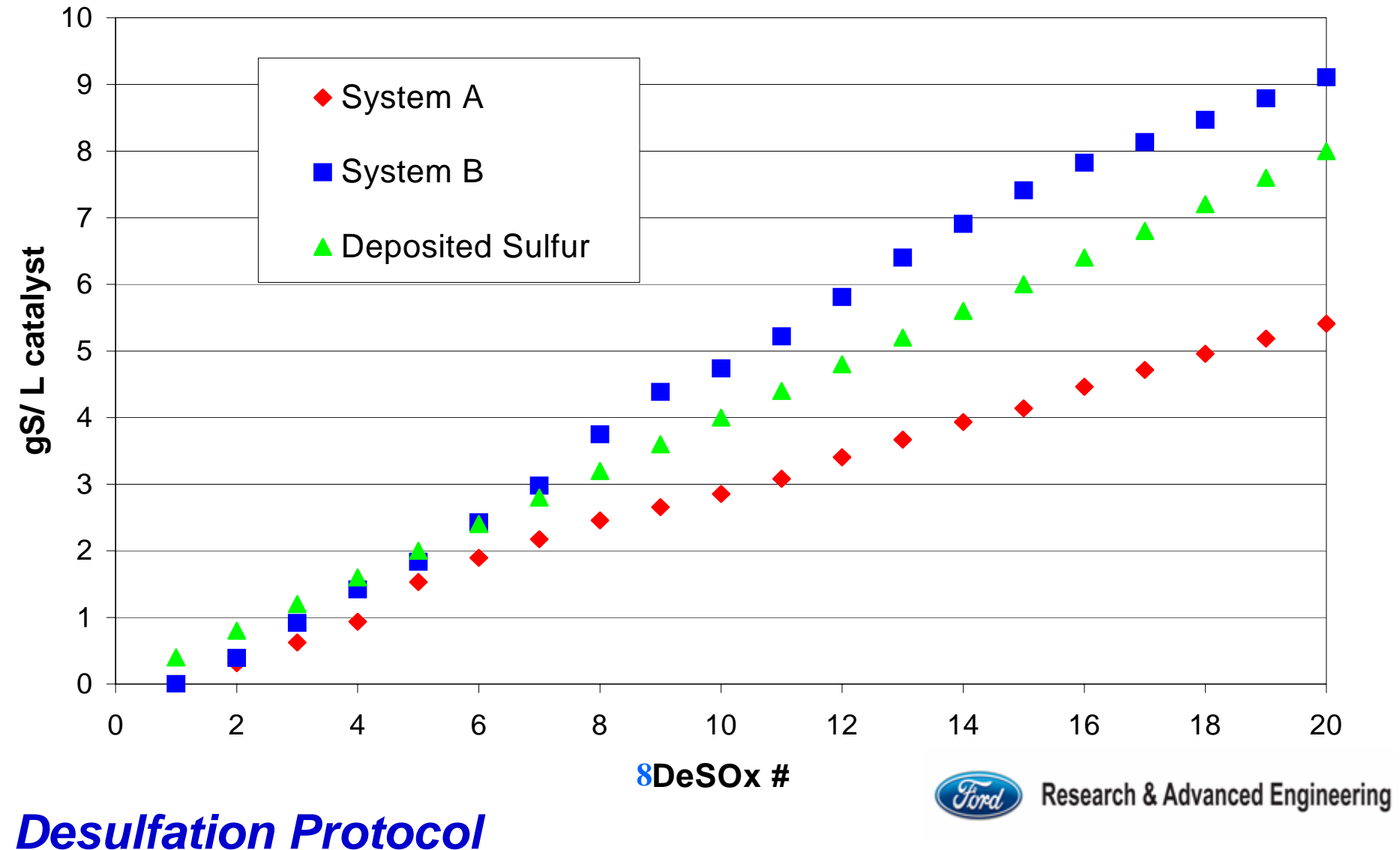
## Desulfation Protocol: System A



## Desulfation Protocol: System B

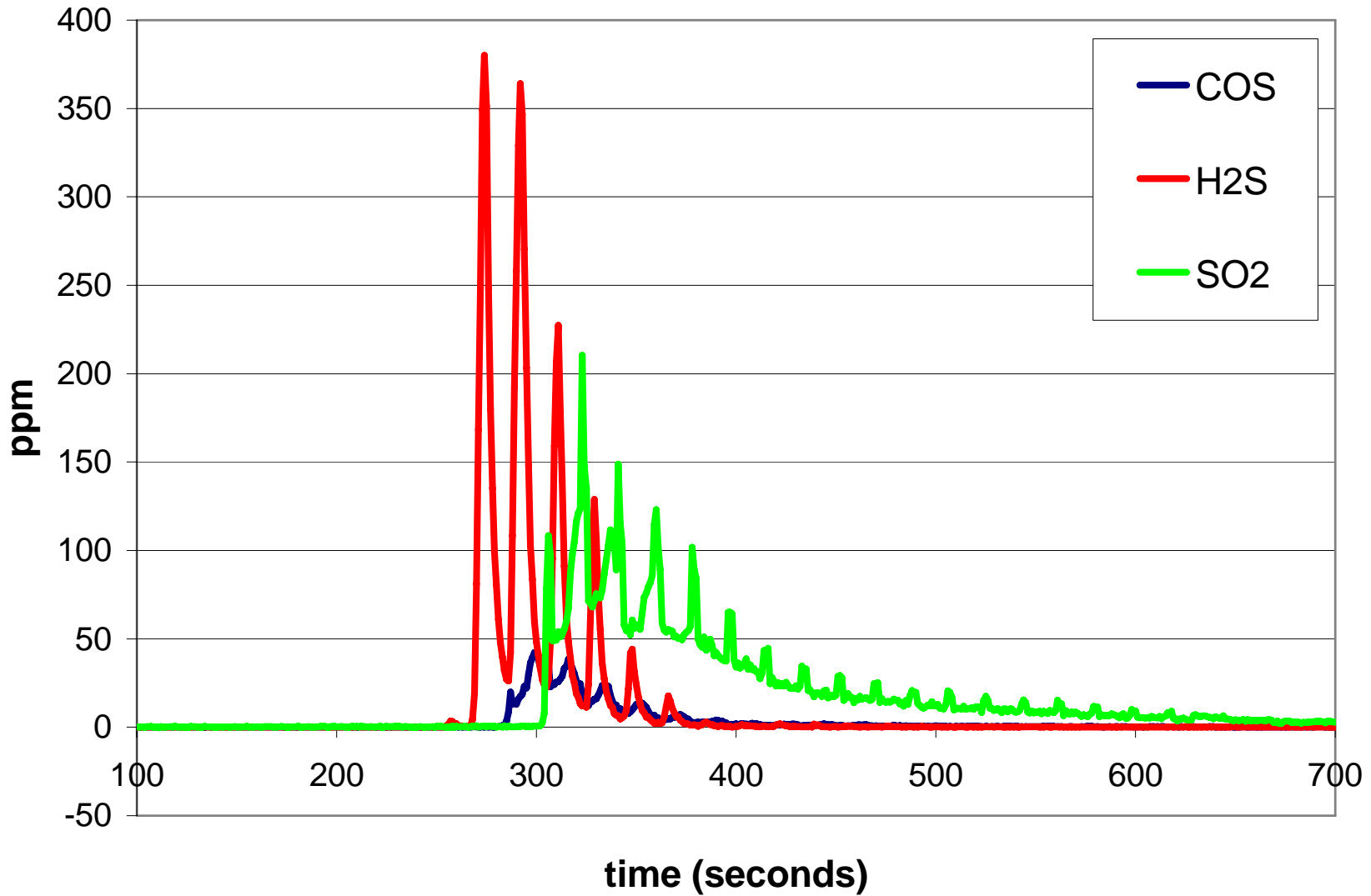


# Sulfur Release at Outlet of SCR During DeSO<sub>x</sub> (H<sub>2</sub>S, SO<sub>2</sub>, and COS Measured w/ a Mass Spectrometer)

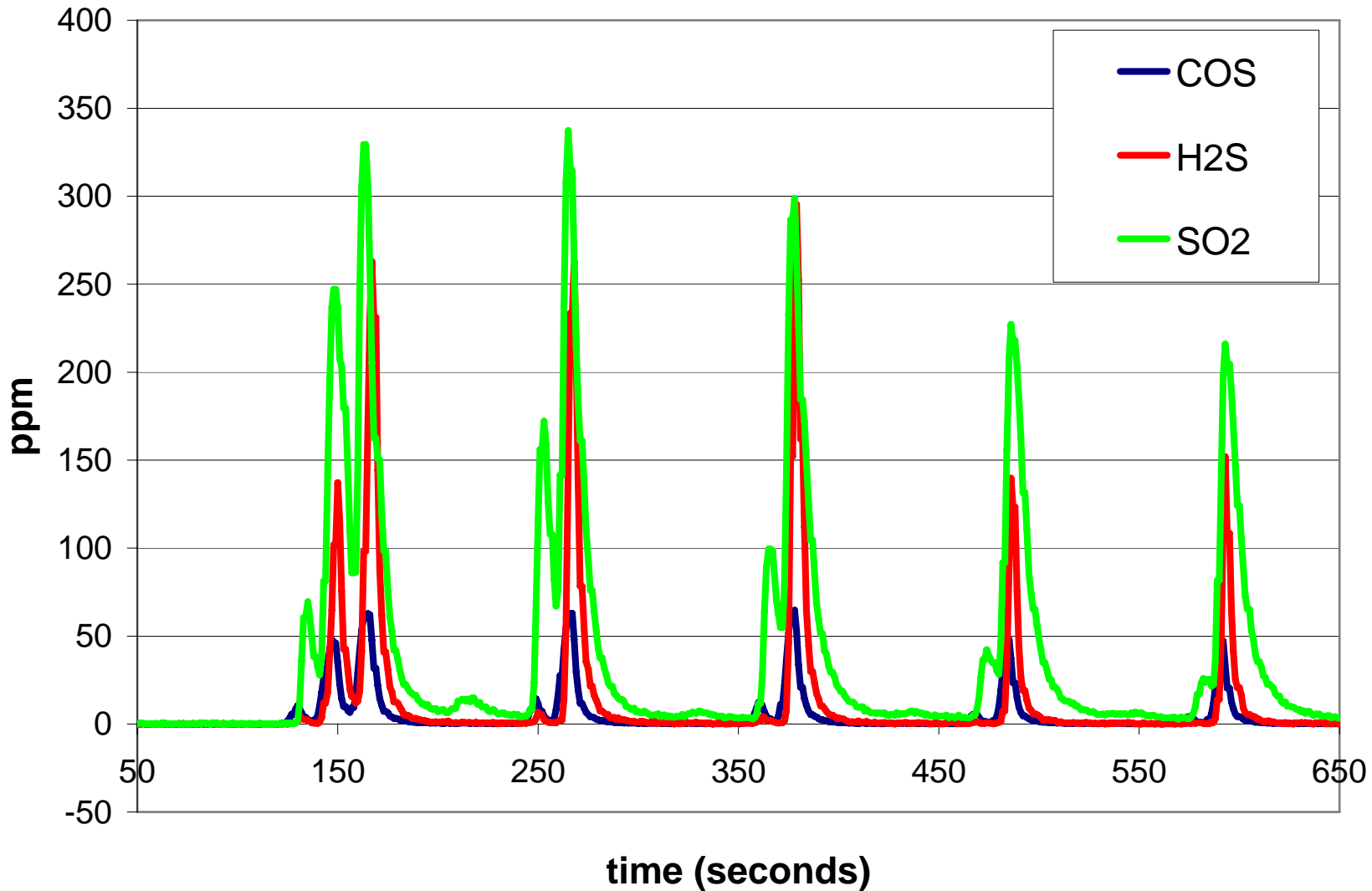




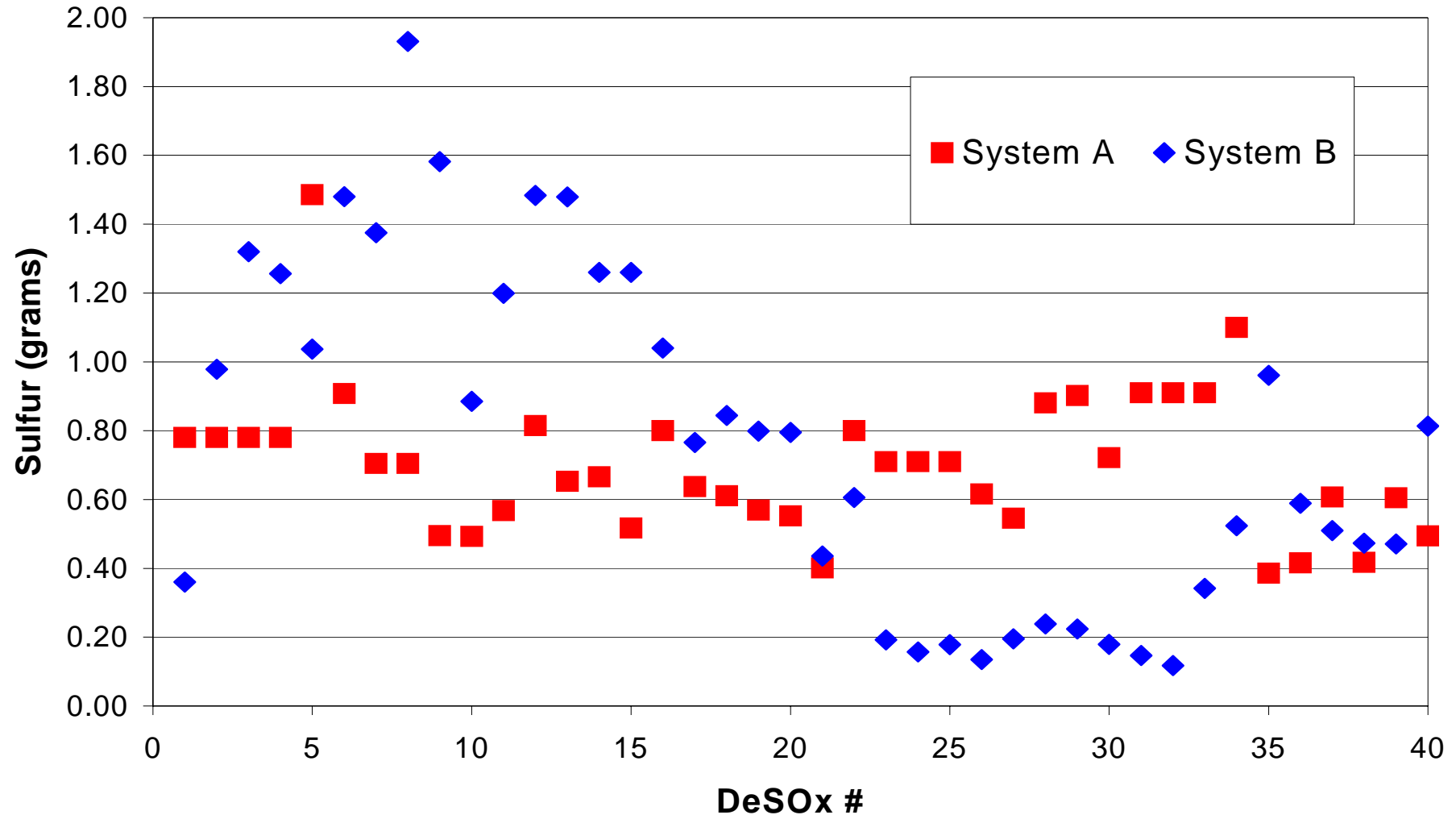
# System A Desulfation: #12



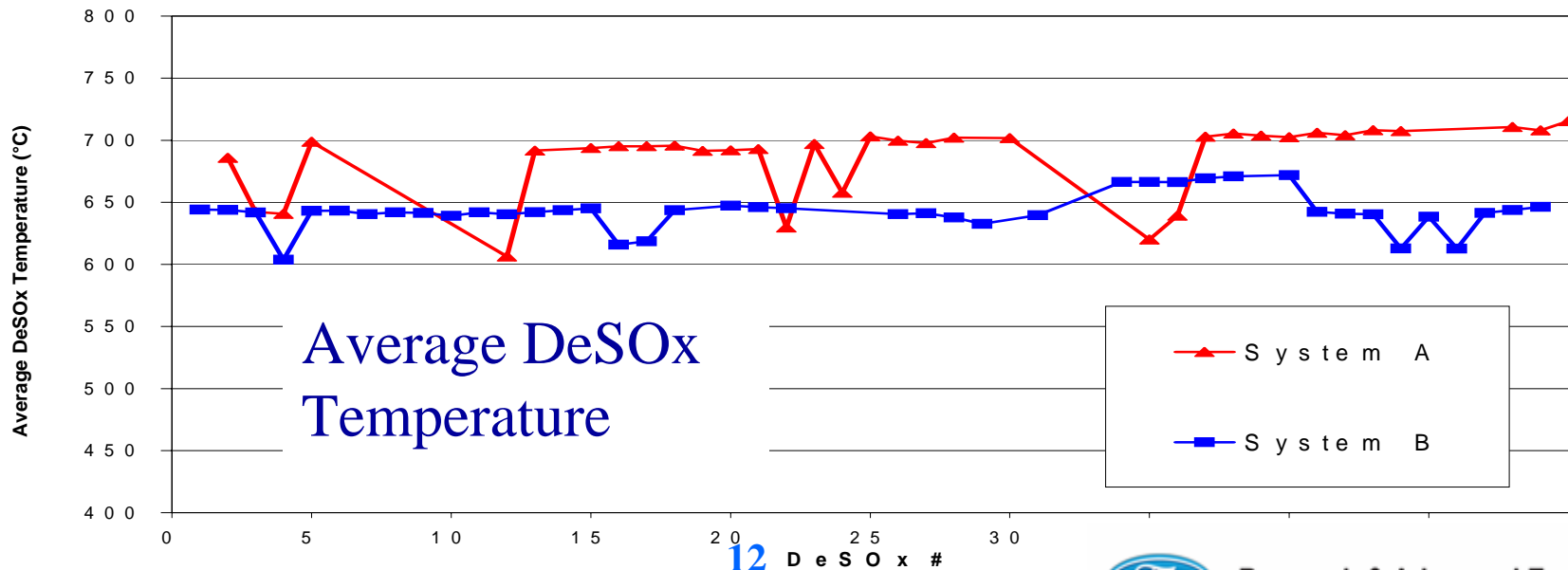
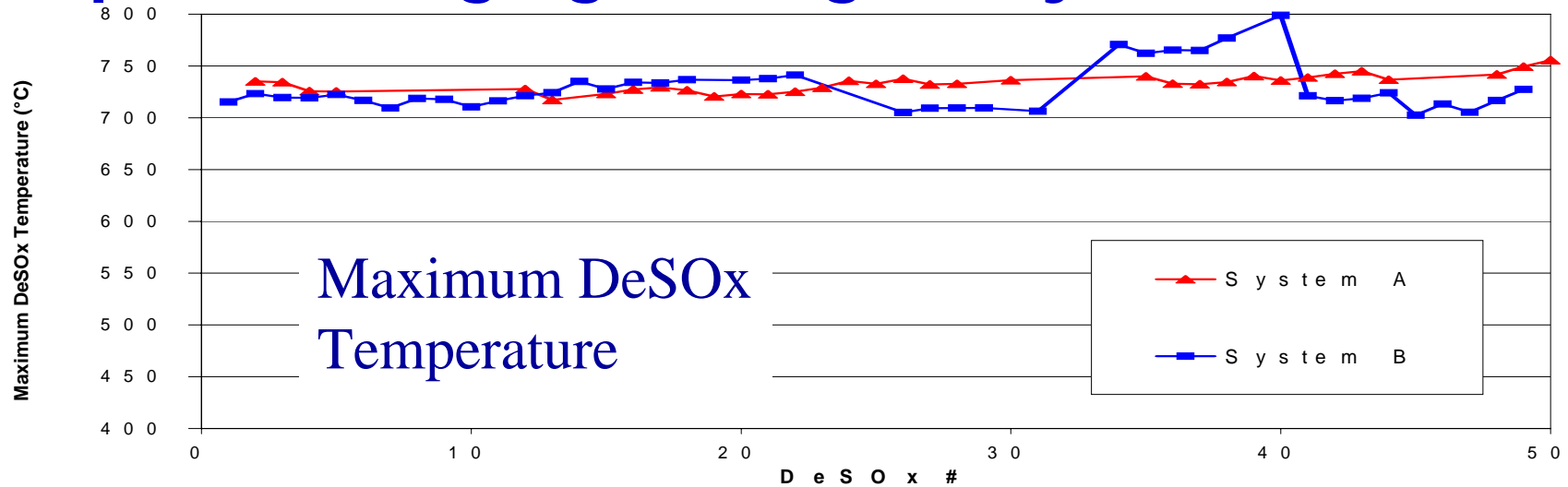
# System B Desulfation: #12



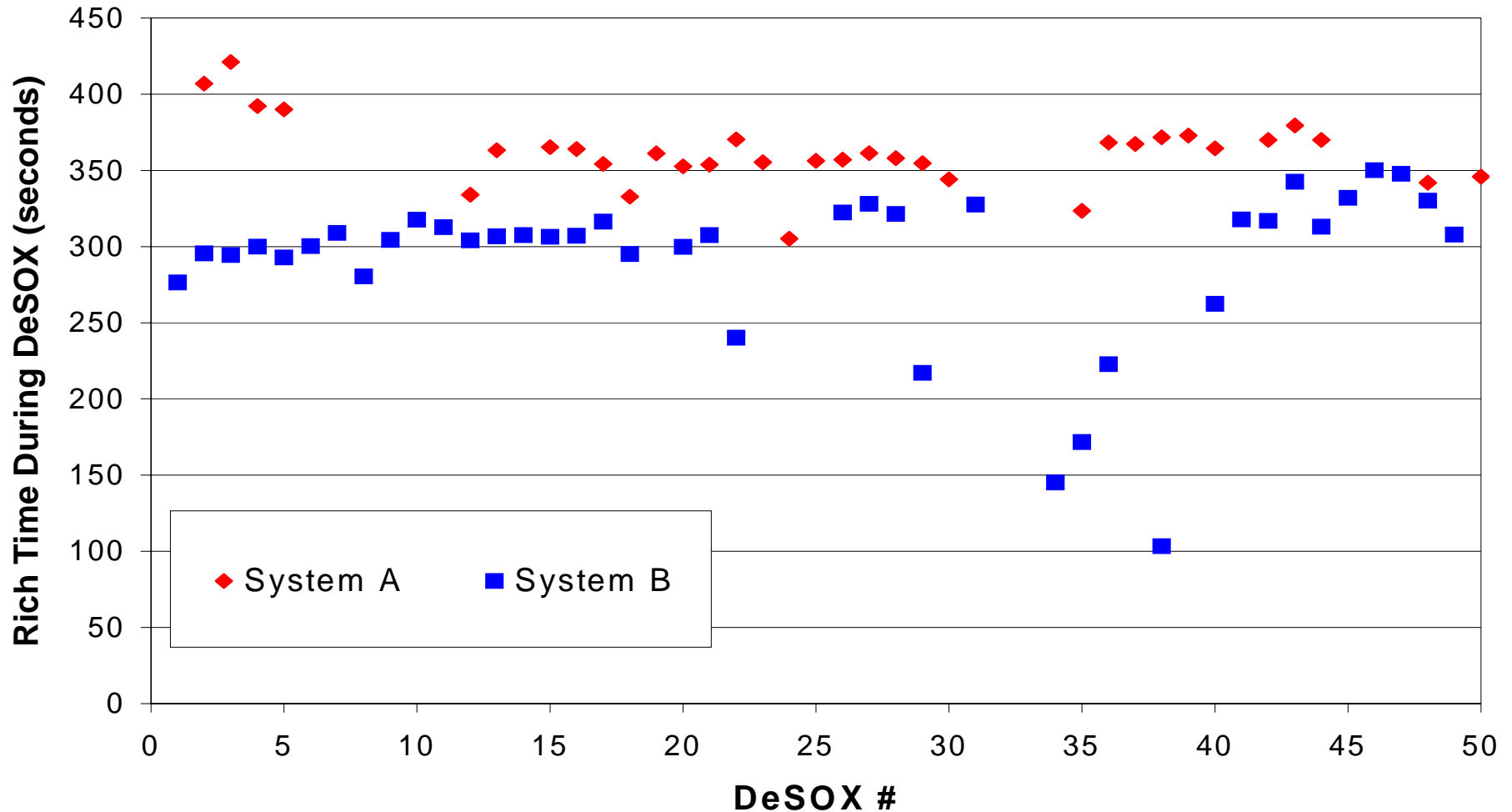
# Total Sulfur Removal per Desulfation



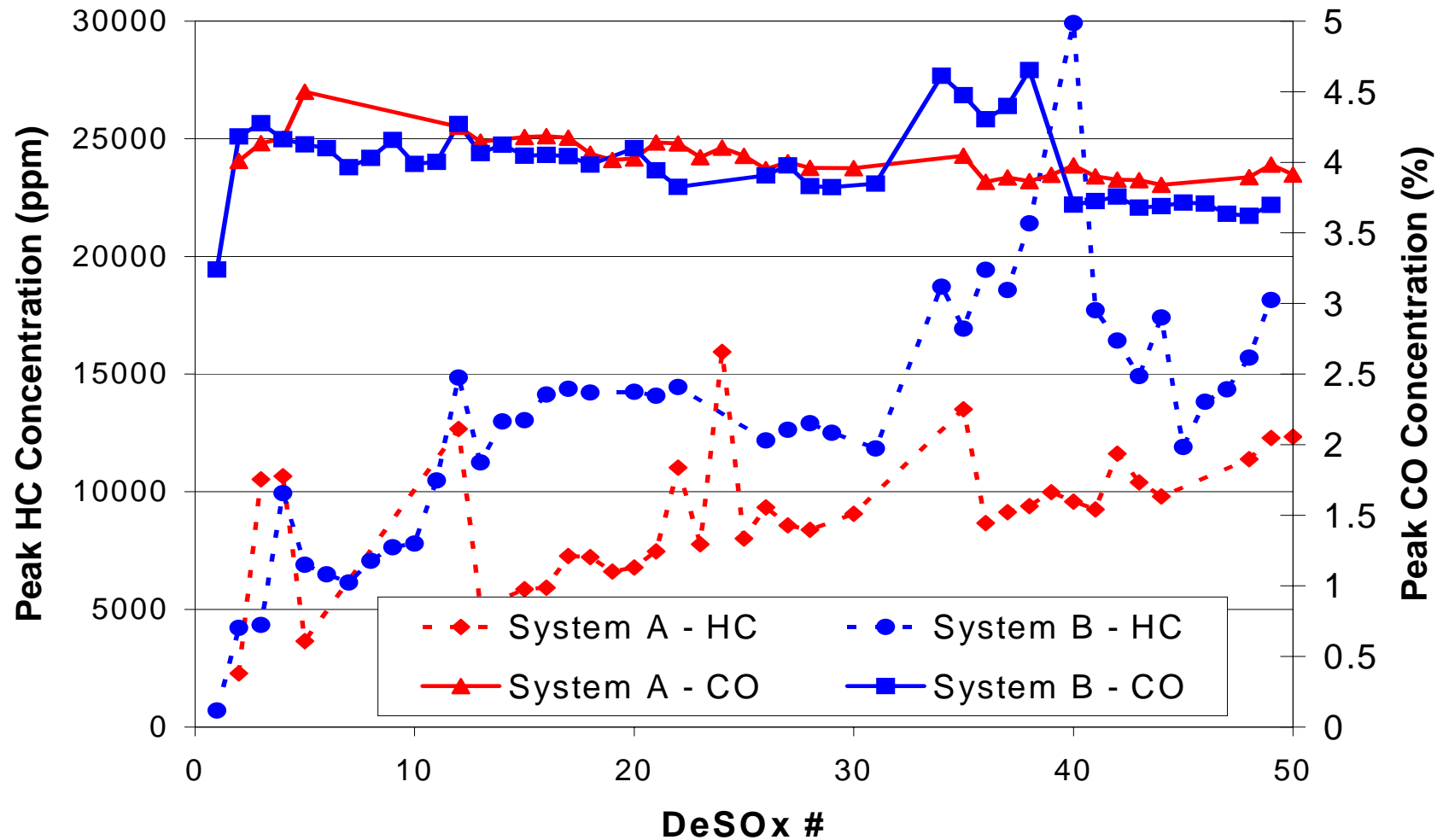
# LNT Desulfation Temperatures over 50,000 mi Equivalent Aging on Engine Dynamometer



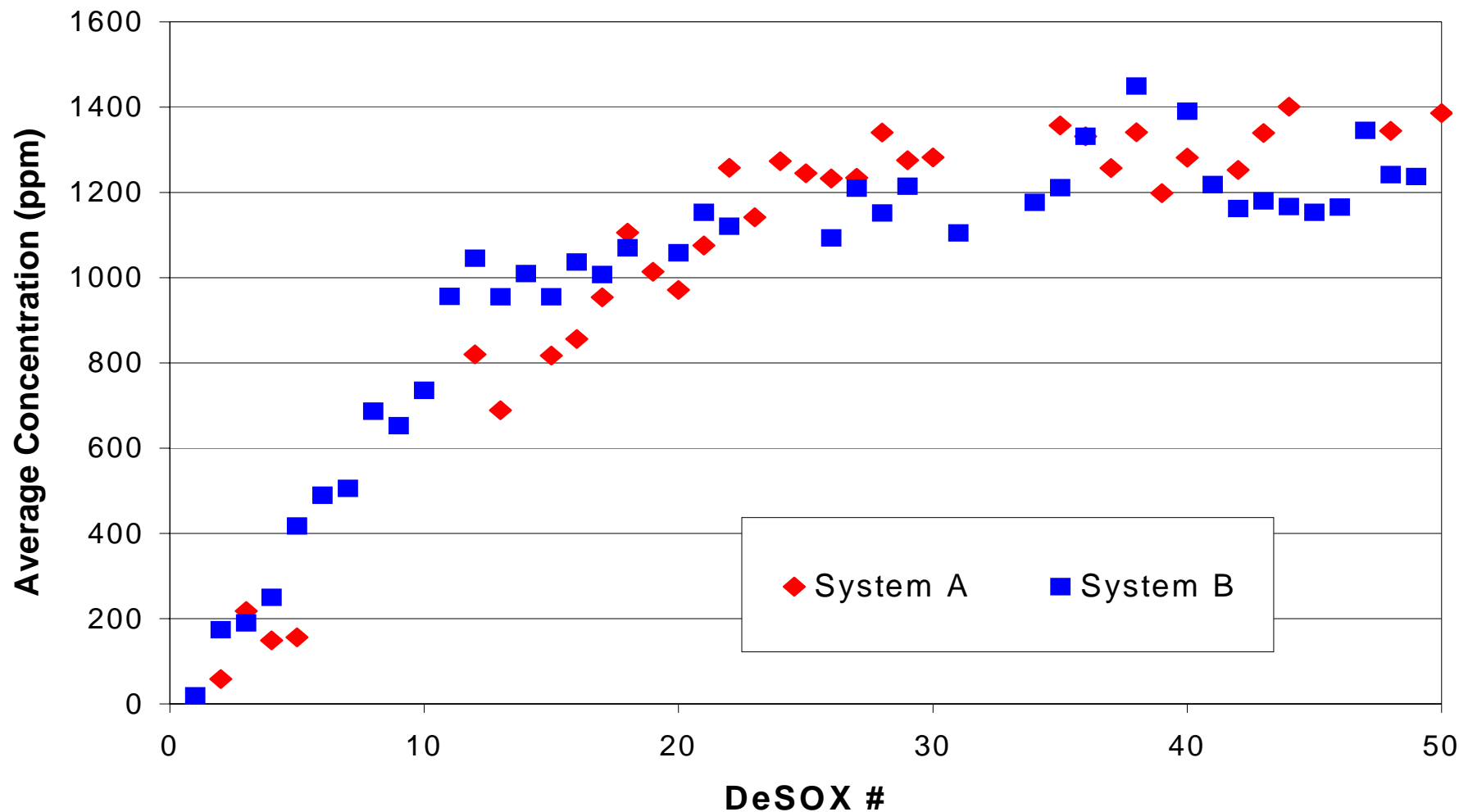
# Desulfation Rich Time During 50,000 mile Equivalent Aging on Engine Dynamometer



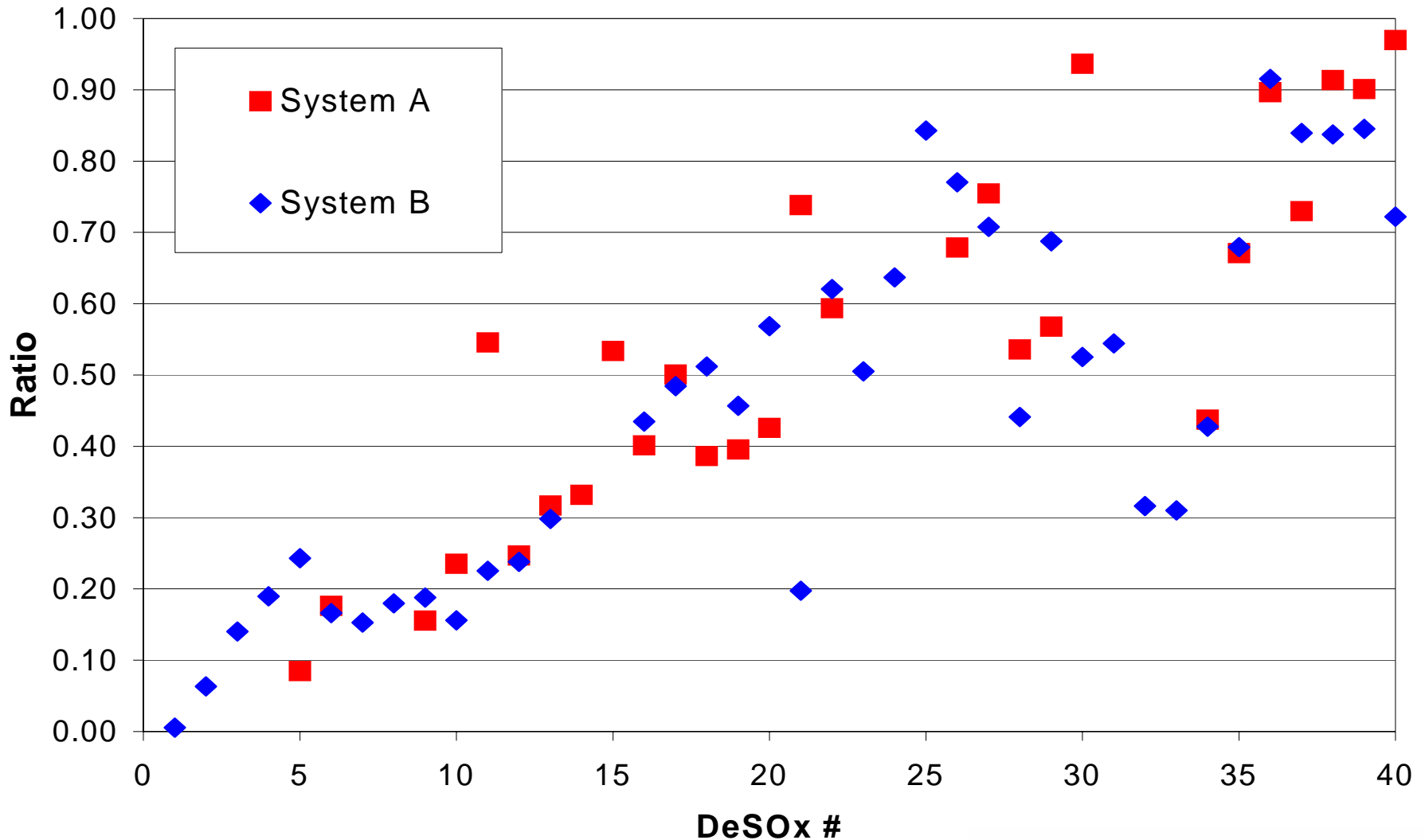
# CO and HC Emissions at the Inlet to the LNT during Desulfations over 50,000 mi Equivalent Aging



# Average HC Concentration at Inlet to LNT During Desulfations over 50,000 mile Equivalent Aging

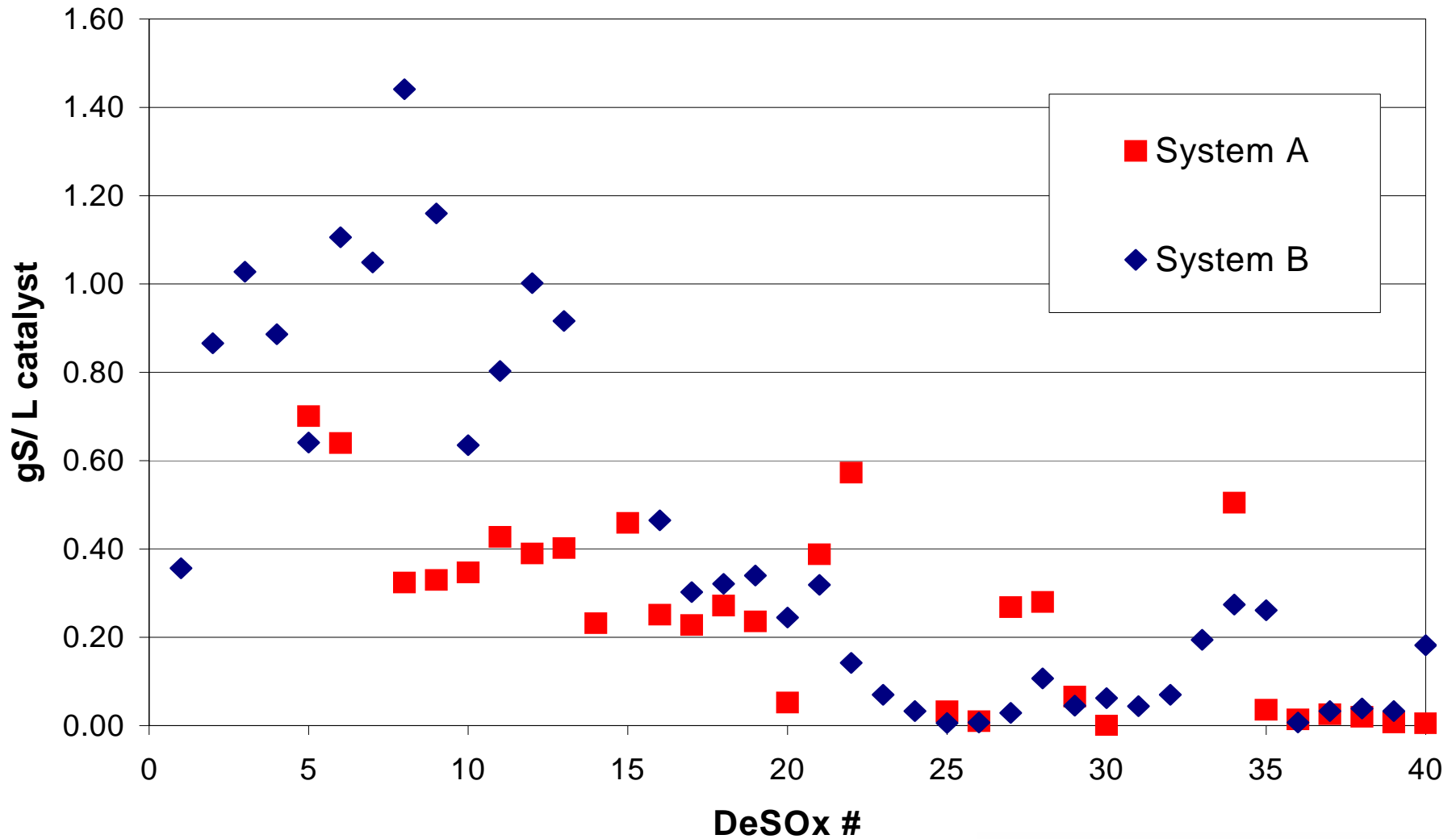


# Fraction of Sulfur Removed as H<sub>2</sub>S

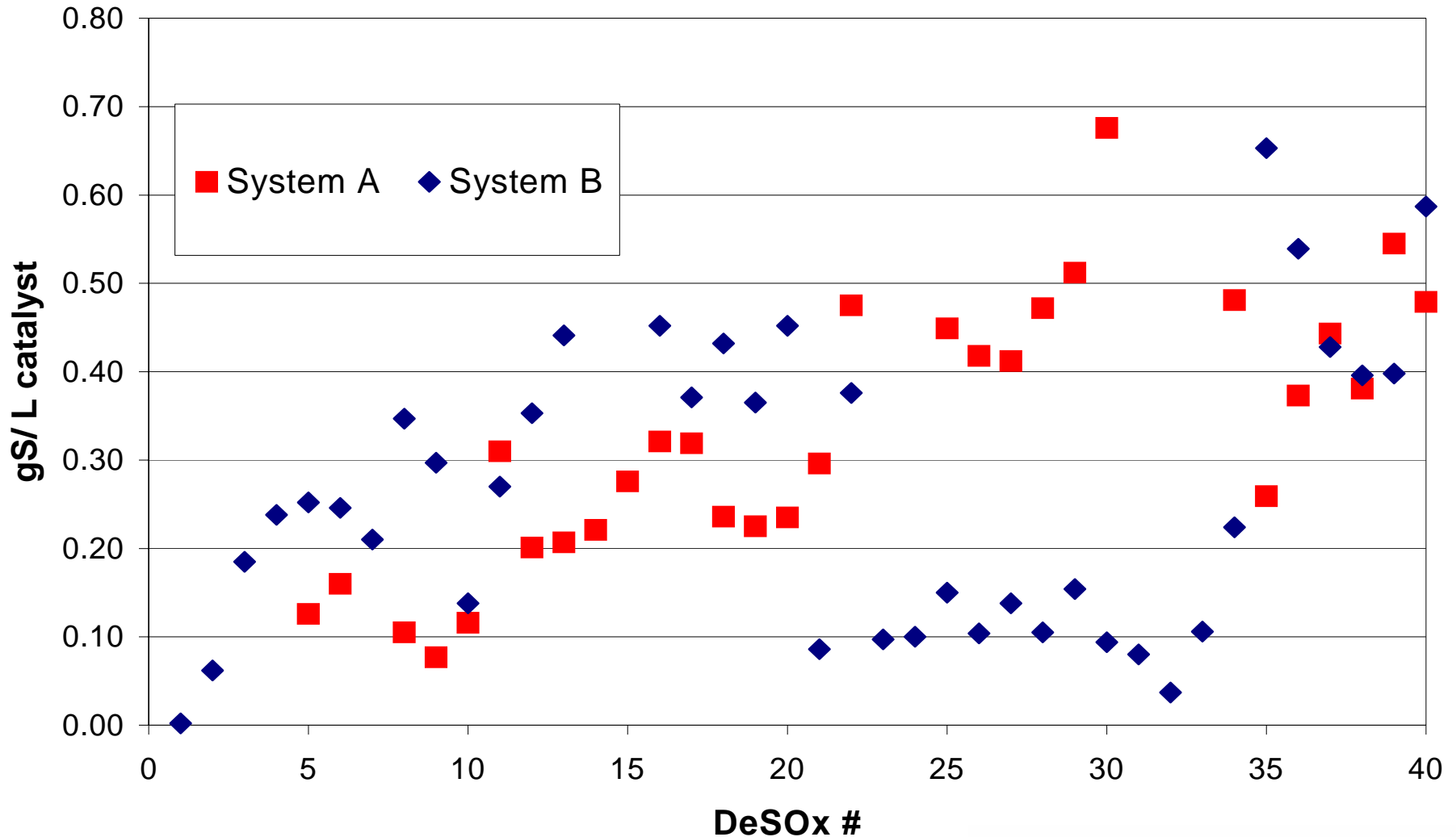




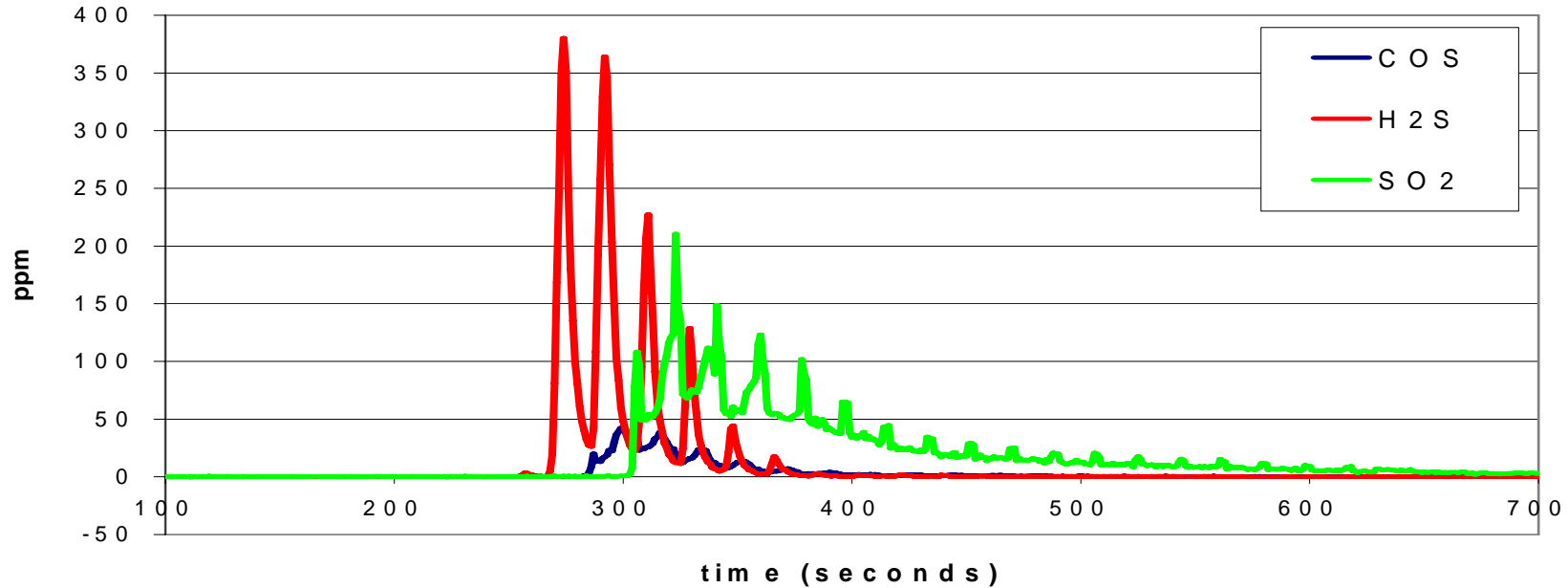
# Sulfur Removed as SO<sub>2</sub>



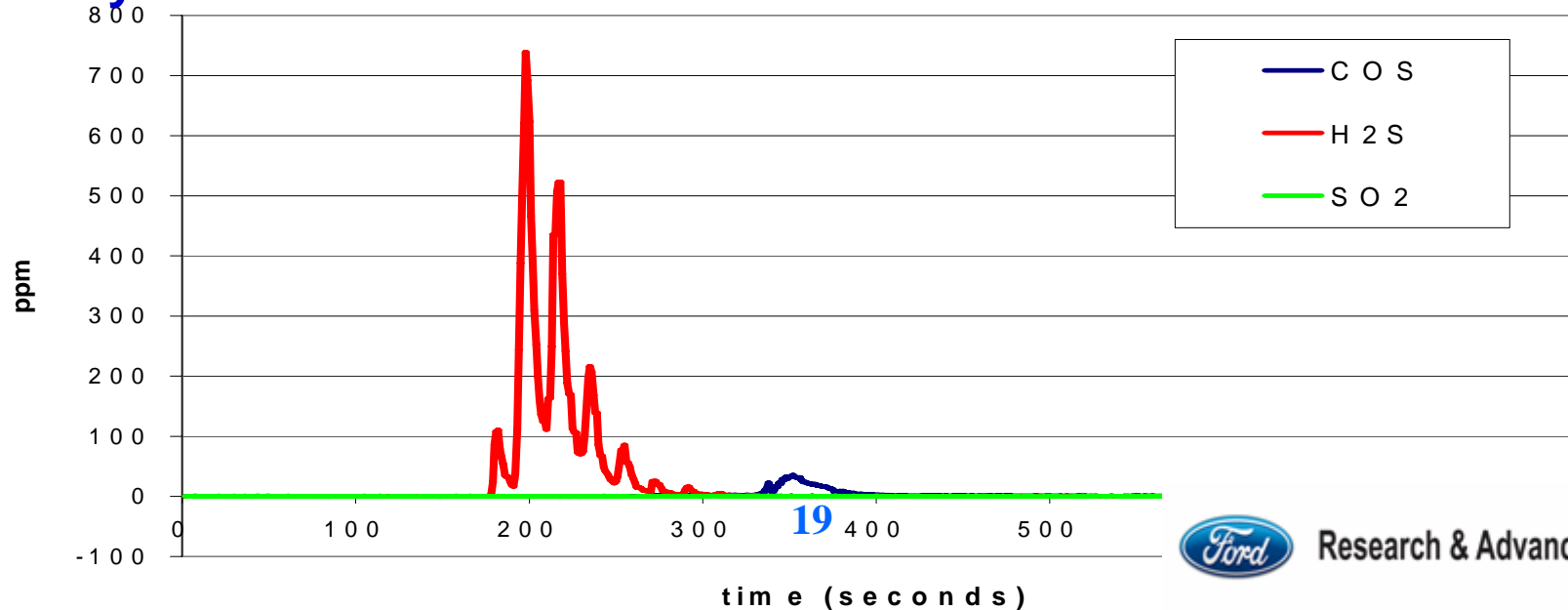
# Sulfur Removed as H<sub>2</sub>S



## System A: Desulfation #12



## System A: Desulfation #40

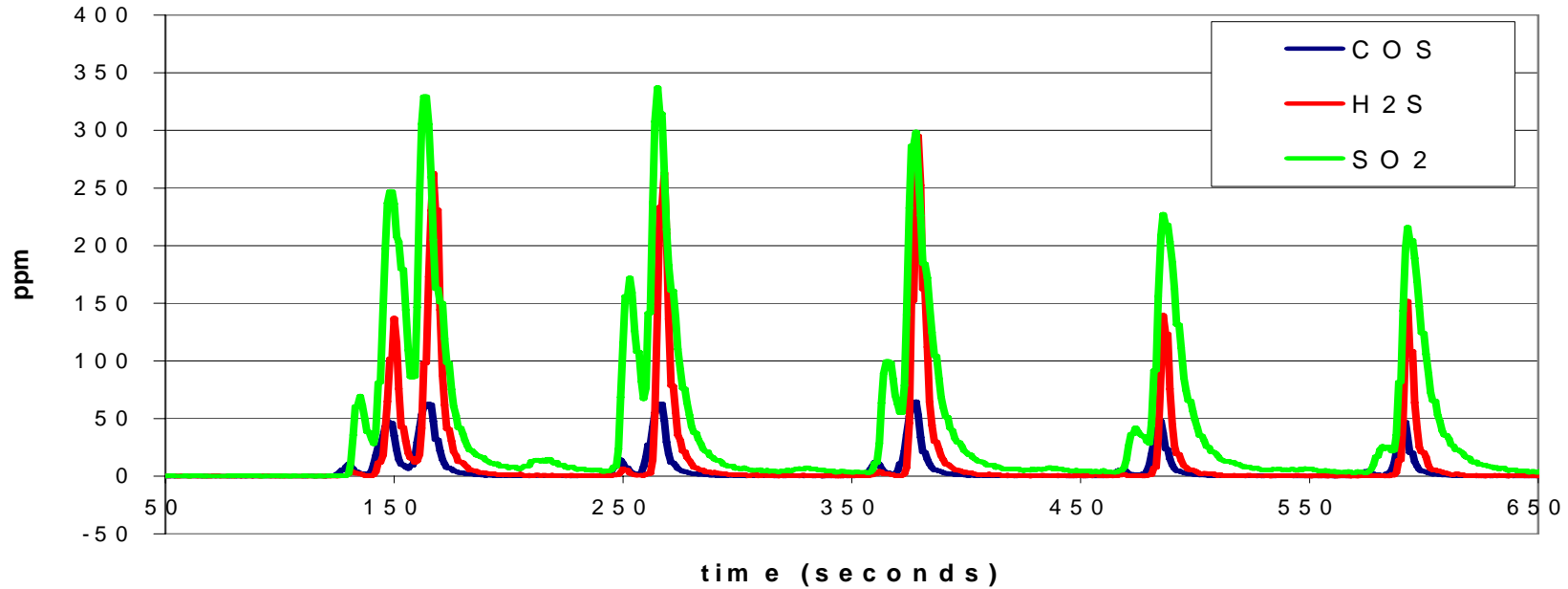


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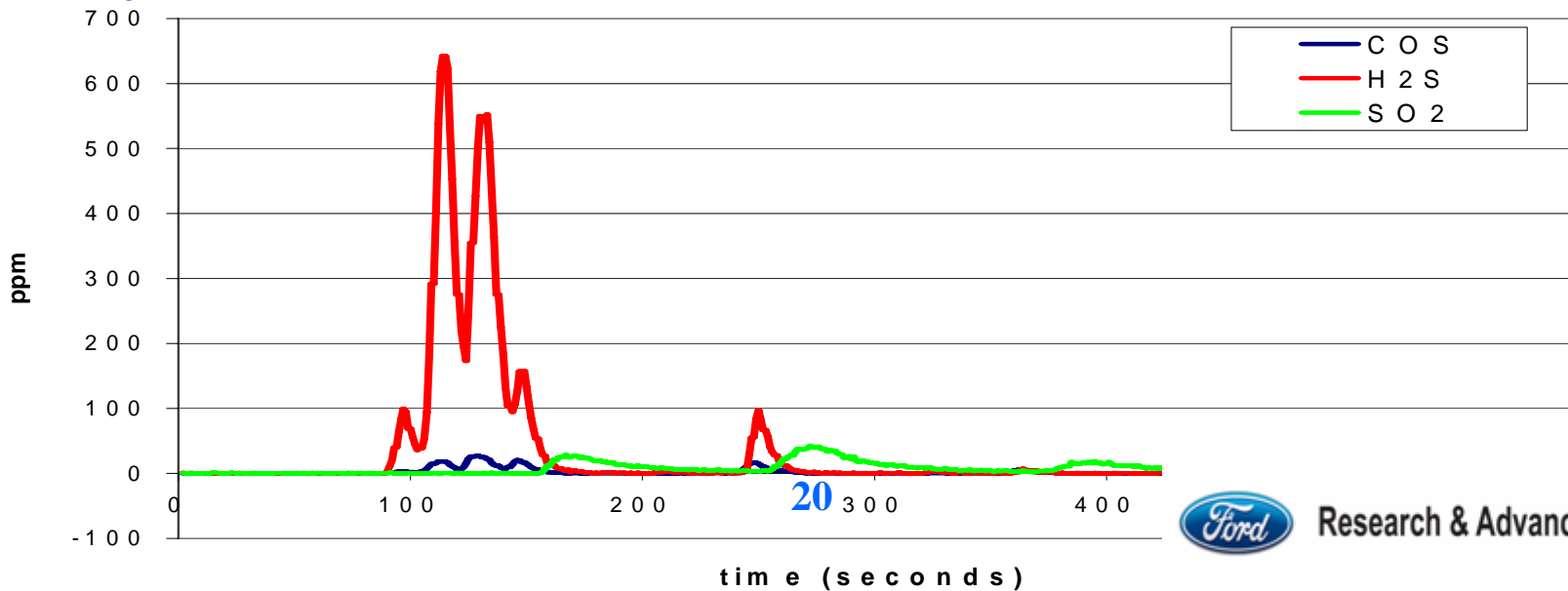


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## System B: Desulfation #12



## System B: Desulfation #40



# Summary

- Rich conditions are necessary for the sulfur removal, however extending the rich time beyond a couple of minutes was not beneficial.
- Most of the sulfur release occurred at onset of switching to rich conditions after an extended lean period.
- The protocol used on System B better utilized the 10 minutes desulfation period due to lean/rich switching.

# Summary

- For both protocols, SO<sub>2</sub> production diminished over the course of the aging.
- The reduced amount of SO<sub>2</sub> was offset by higher H<sub>2</sub>S emissions, although the total sulfur removed was still lower at the end of aging.
- The advantage of the lean/rich switching during desulfation diminished as the catalyst aged.