

# **The study of an Alumina-Based Lean NOx Trap (LNT) for Diesel**

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# Outline

- Introduction
- Sample preparation and Lab test condition
- Activities
- De-SO<sub>x</sub>
- Applications
- Discussion
- Conclusions

## Introduction

- The exhaust temperature of light duty diesel vehicle is low (average cat inlet  $T < 180^{\circ}\text{C}$ ) in urban driving cycles; current existing LNTs operate poorly below  $200^{\circ}\text{C}$ .
- Looking for materials to improve diesel LNT activities at low temperature ( $150$  to  $300^{\circ}\text{C}$ ).
- Alumina was studied as  $\text{NO}_x$  storage materials in a new diesel LNT.
- The new diesel LNT has high  $\text{NO}_x$  activities at low temperature. Its de- $\text{SO}_x$  process can be very efficiently performed at  $600$  to  $650^{\circ}\text{C}$  without noticeable thermal damage to the LNT.

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## Catalyst preparation

- New (alumina) LNT preparation
  - Started from core samples with coated alumina washcoat ( $\text{Al}_2\text{O}_3$ : nominal loading)
  - Some alumina washcoats were modified by adding small amount of alkaline earth metal (2 to 3wt% of Mg, Ca, Sr or Ba) through soaking the samples in solution, such as Sr acetate, etc.
  - Precious metals were added to the new LNT through the Subtractive Deposition Method with similar loadings (typically Pt/Rh: 100/20g/ft<sup>3</sup>) to a conventional (BaO on alumina) LNT
- New LNTs were later prepared by one of suppliers with different alumina loadings (nominal & two times of nominal loading)

# Lab condition - evaluation and de-SOx

- Evaluation conditions
  - Sample size: 1 inch diameter & length
  - Lab test gas compositions (SV of 30,000 hr<sup>-1</sup>)
- Sulfur poisoning and de-SOx conditions
  - Load sulfur (SO<sub>2</sub>) 1.15g/lit at lean condition (30ppm for 3000 seconds)
  - De-SOx at 600 to 650°C slightly rich ( $\lambda = 0.98$  to  $0.987$ ) for 1 to 2 minutes

Lab test gas compositions

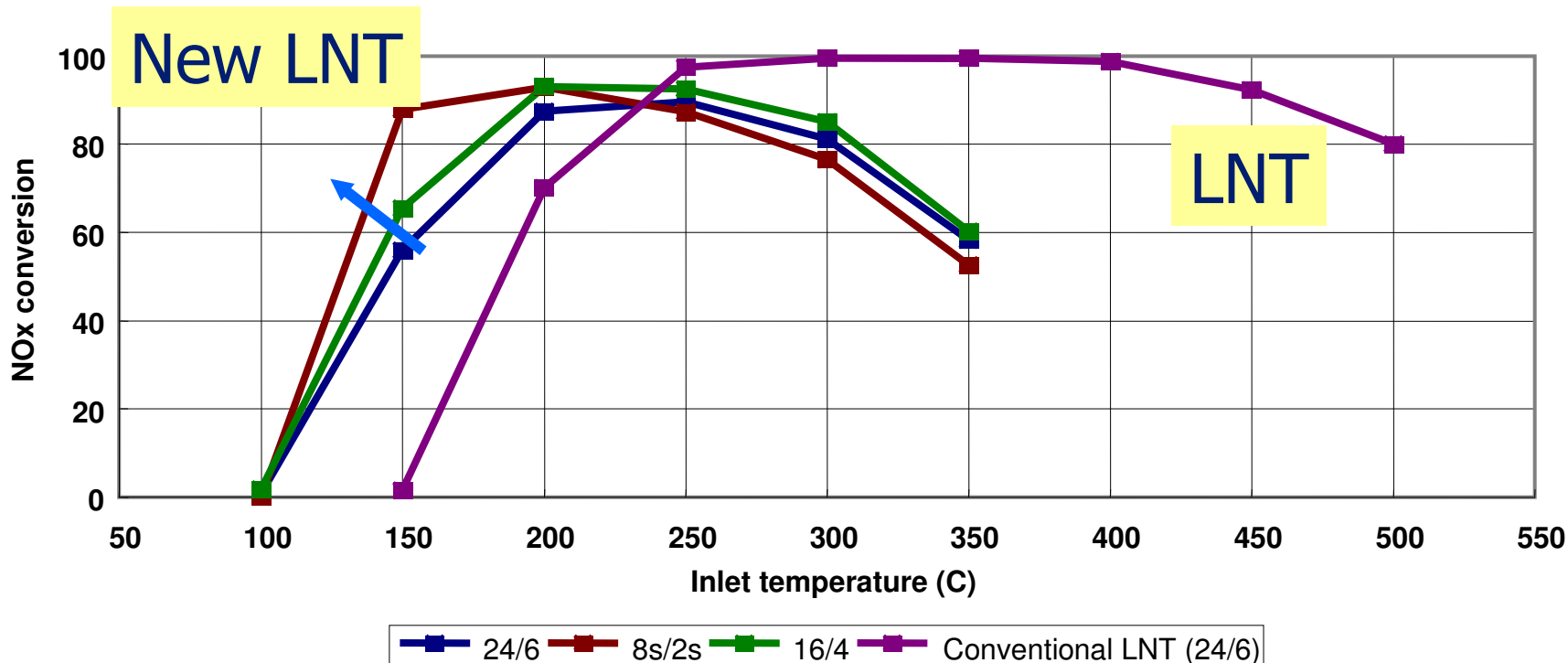
Gas	Lean	Rich
CO	500ppm	4%
H <sub>2</sub>	167ppm	1.33%
C <sub>3</sub> H <sub>6</sub>	300ppm C1	5000 ppmC1
NOx	500ppm	500ppm
O <sub>2</sub>	10%	1%
CO <sub>2</sub>	5%	5%
H <sub>2</sub> O	5%	5%
	$\lambda=1.96$	$\lambda=0.90$

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# Conversion Comparison: New LNT to LNT

New LNT (after S poisoning & de-SOx) compared with a de-greened conventional LNT



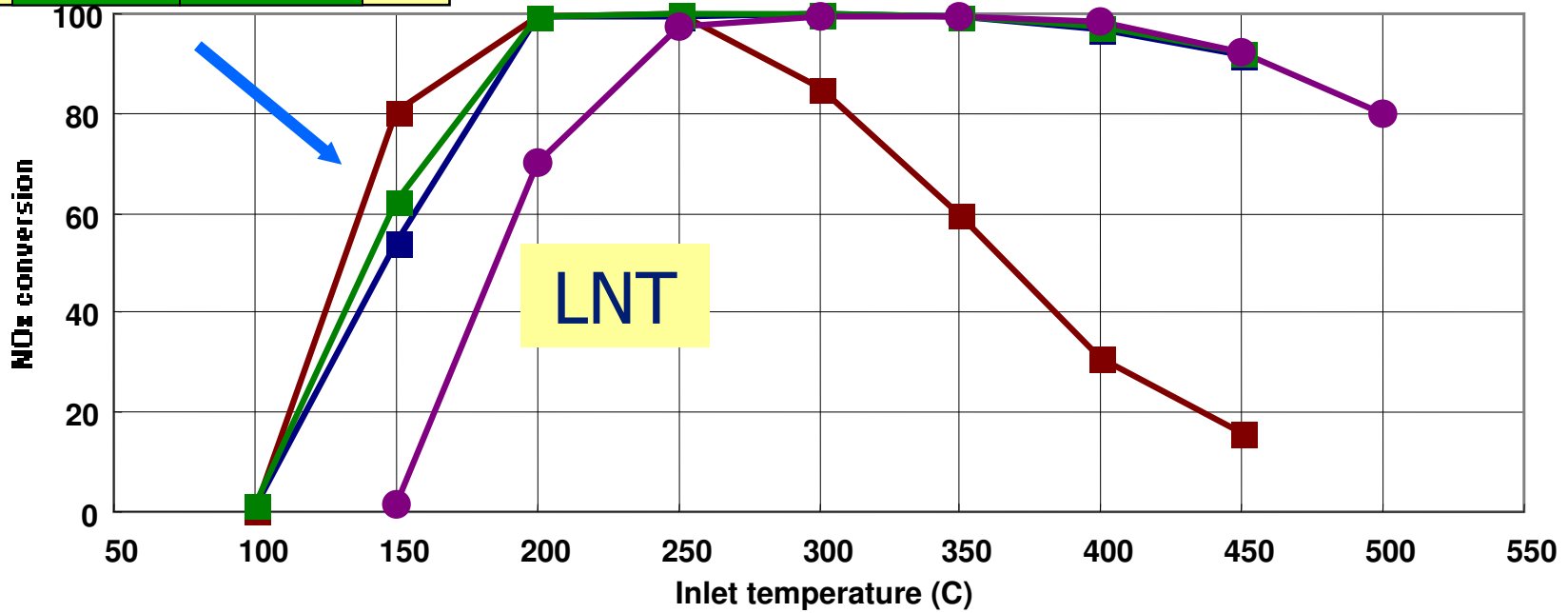
- Excellent low temperature conversion
- Better than any other catalyst to date
- Retained after sulfur loading and deSOx

\*\*\* 24/6: 24 second lean & 6 second rich



# New LNT and LNT In Series

New LNT (after S poisoning & de-SOx) plus a conventional LNT compared with the conventional LNT only



—■— 24/6    —■— 8/2    —■— 16/4    —●— conventional alone at 24/6

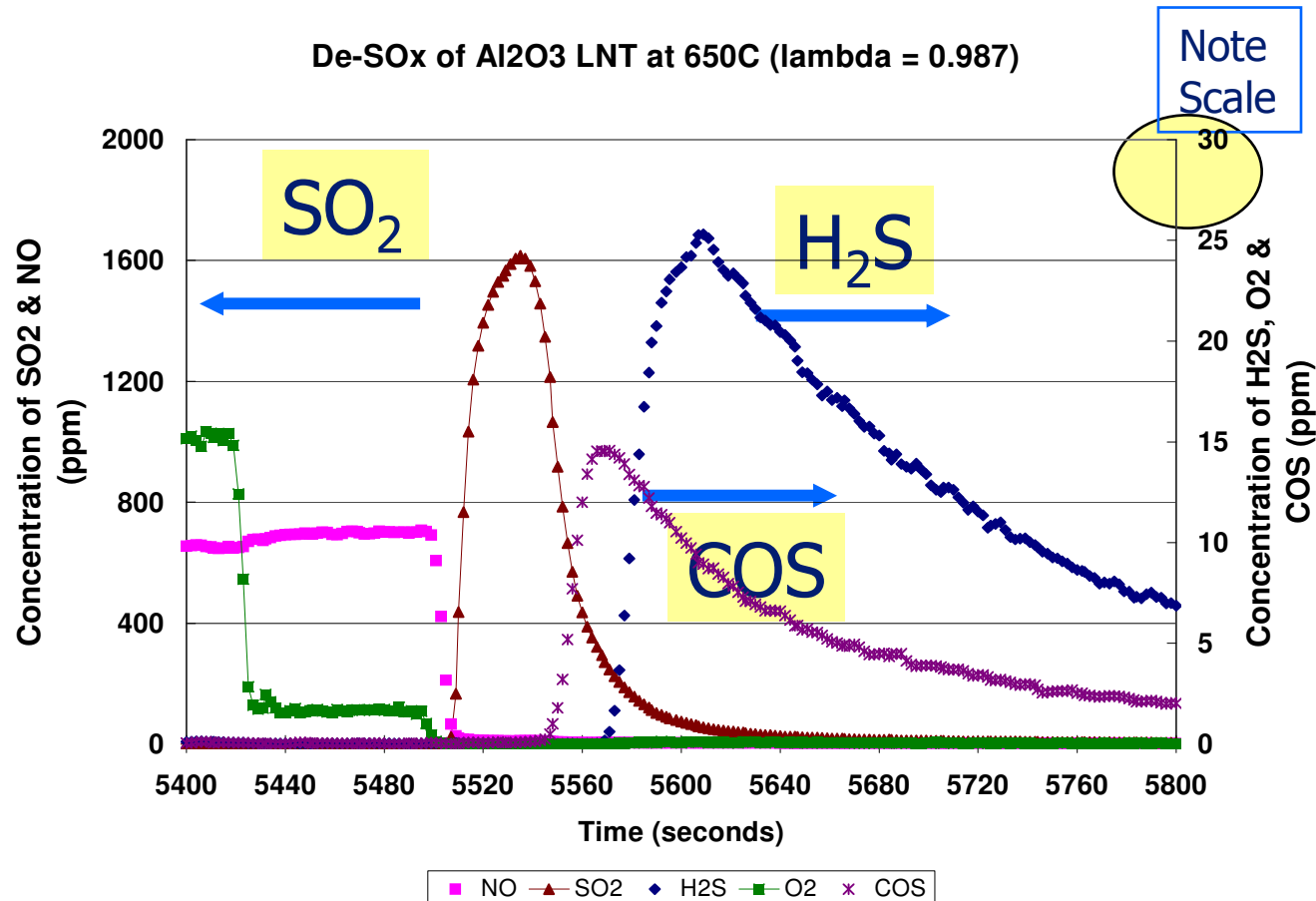
\*\*\* 24/6: 24 second lean & 6 second rich

- Excellent system NOx conversion over a very wide temperature window

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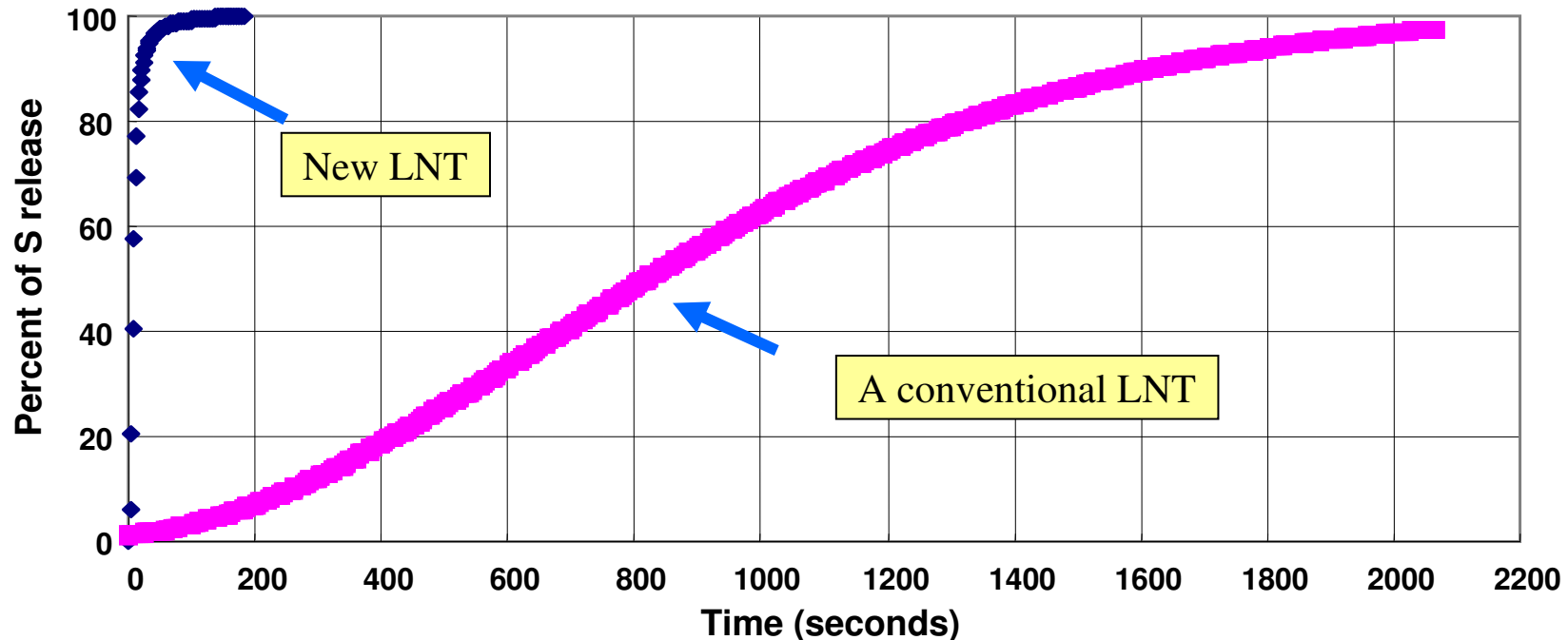
# De-SOx of New LNT (sulfur loading 1.14g/liter)



- Lambda slightly rich, at 650°C
  - I.e., leaner than conventional LNT de-SOx
- Sulfur released quickly in about 1 minute, as SO<sub>2</sub>
- Conventional LNT usually takes several minutes, gives H<sub>2</sub>S

## DeSOx of New LNT Versus LNT

De-SOx of New LNT at 650C and  $\lambda$  of 0.98 compared with a typical conventional LNT (starting at 650C, heated to 800C at 5C/min) at 5/15 (lean/rich: lambda 2.0/0.9)

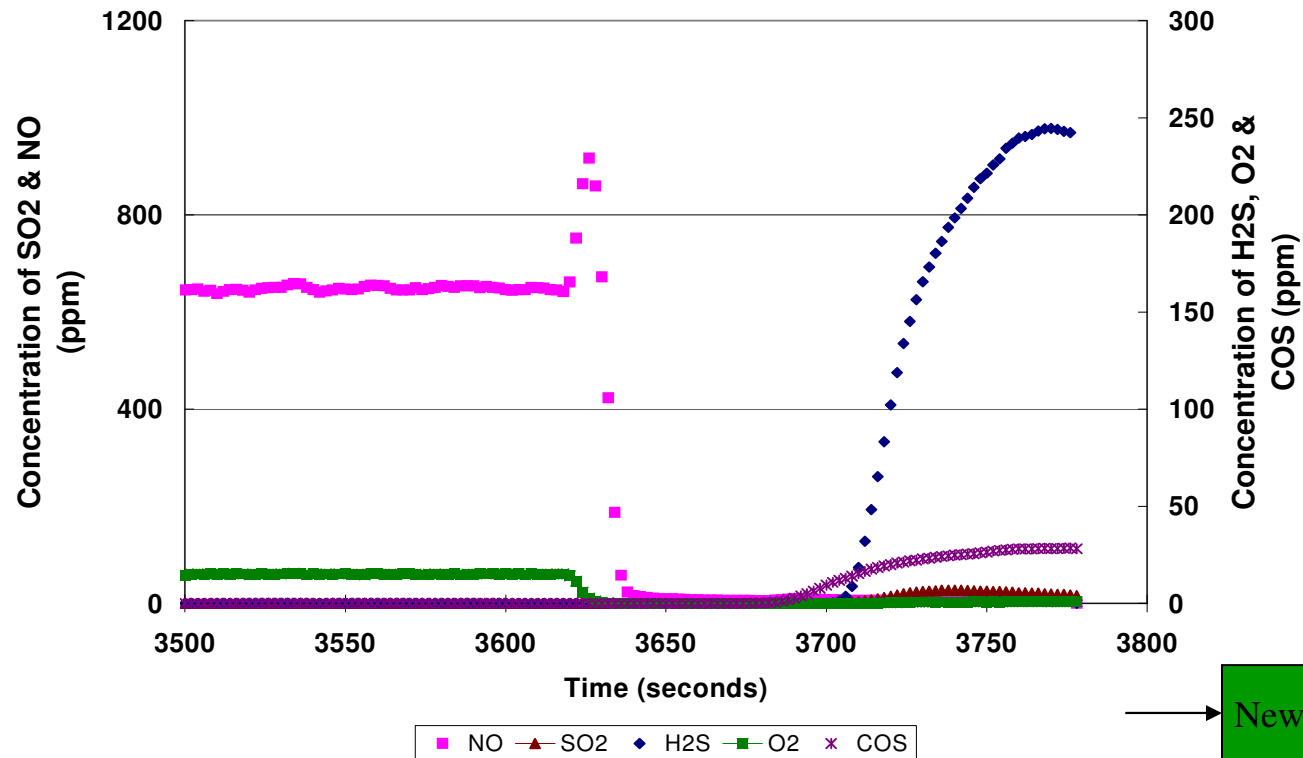


- Much faster rate of sulfur release
- Therefore, needs less time at high temperature
- Much less thermal damage
- Lower FE penalty

# De-SOxing New LNT in Series with LNT

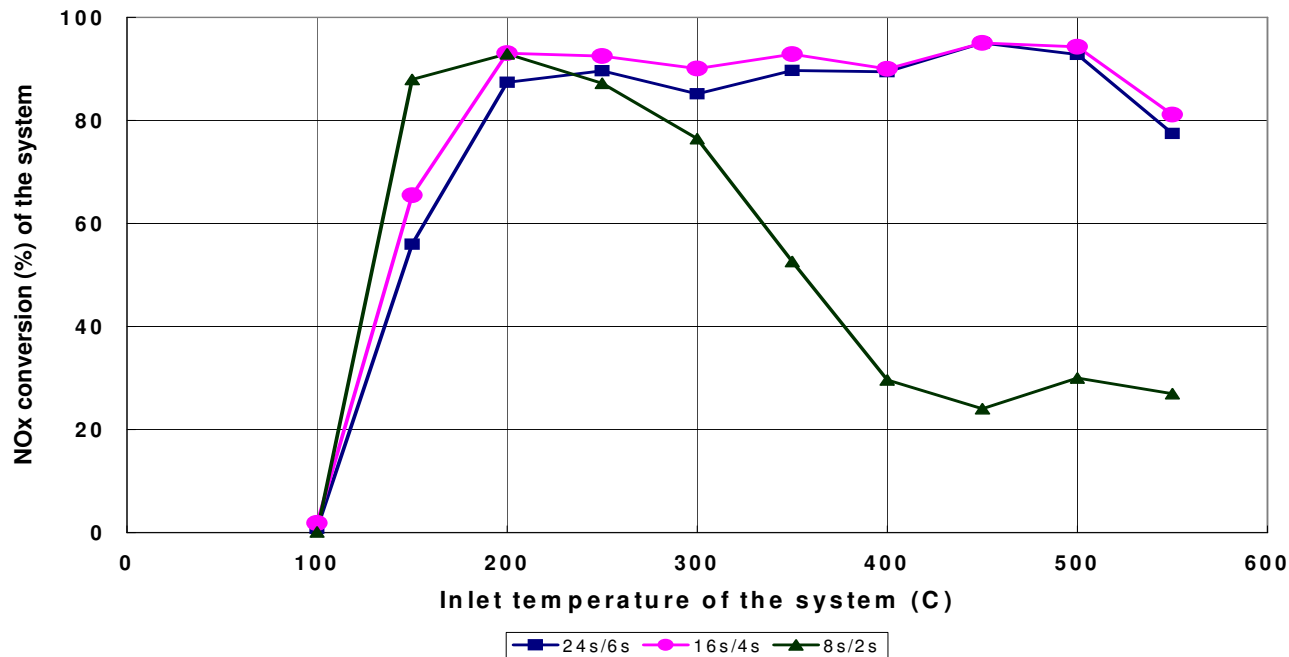
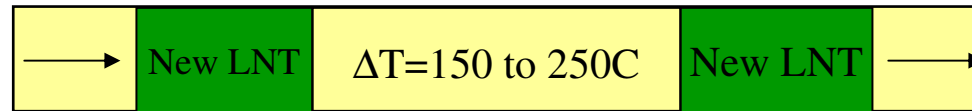
## sulfur loading 1.14g/liter at the New LNT

De-SOx of New LNT + LNT at 650C ( $\lambda = 0.984$ )



- SO<sub>2</sub> released from alumina LNT does *not* pass through LNT
- So, New LNT+LNT system would need conventional de-SOx

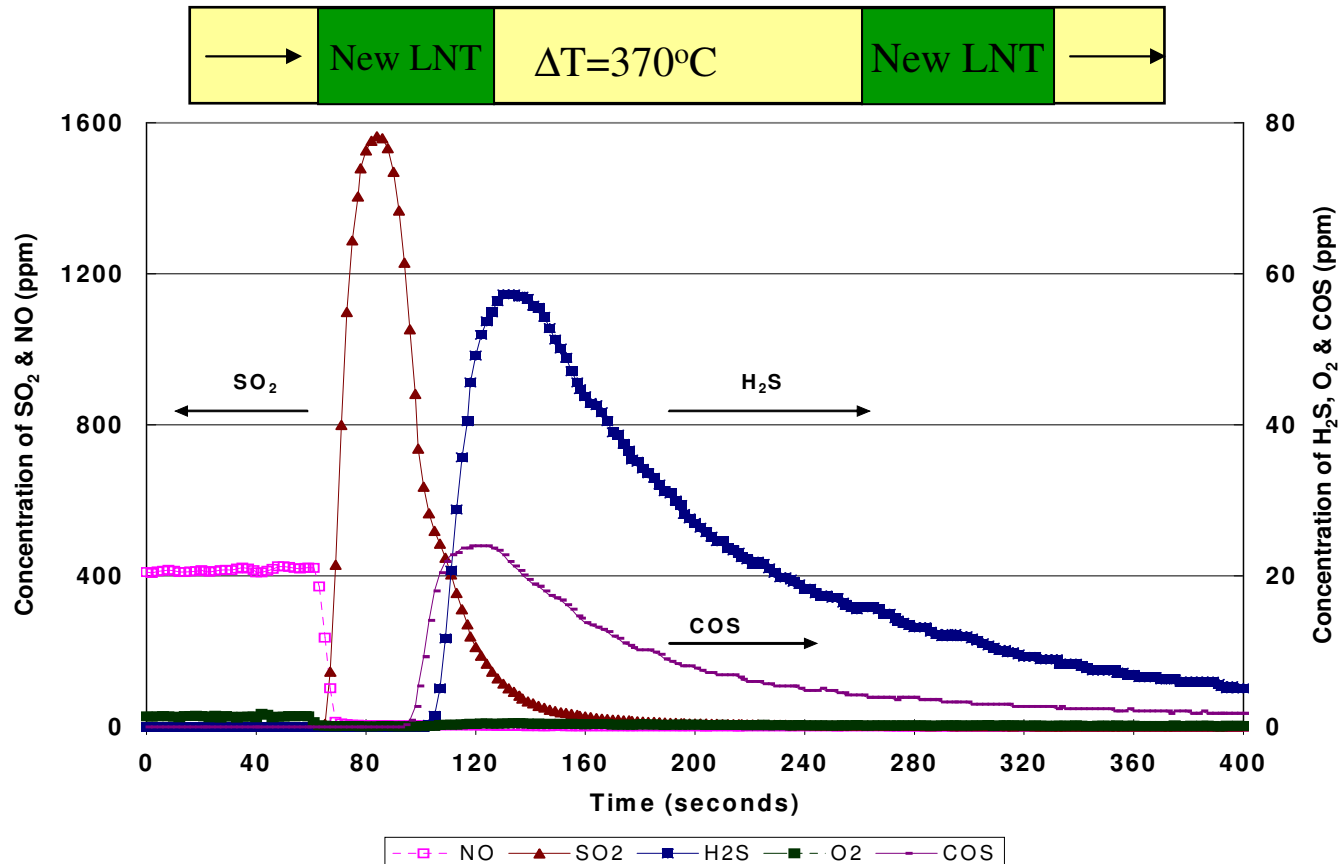
## Two New LNT in Series



- Two catalysts in series (half the space velocity)
- Separated so second bed is cooler
- Gives very wide temperature range

# De-SOx of two New LNT in Series

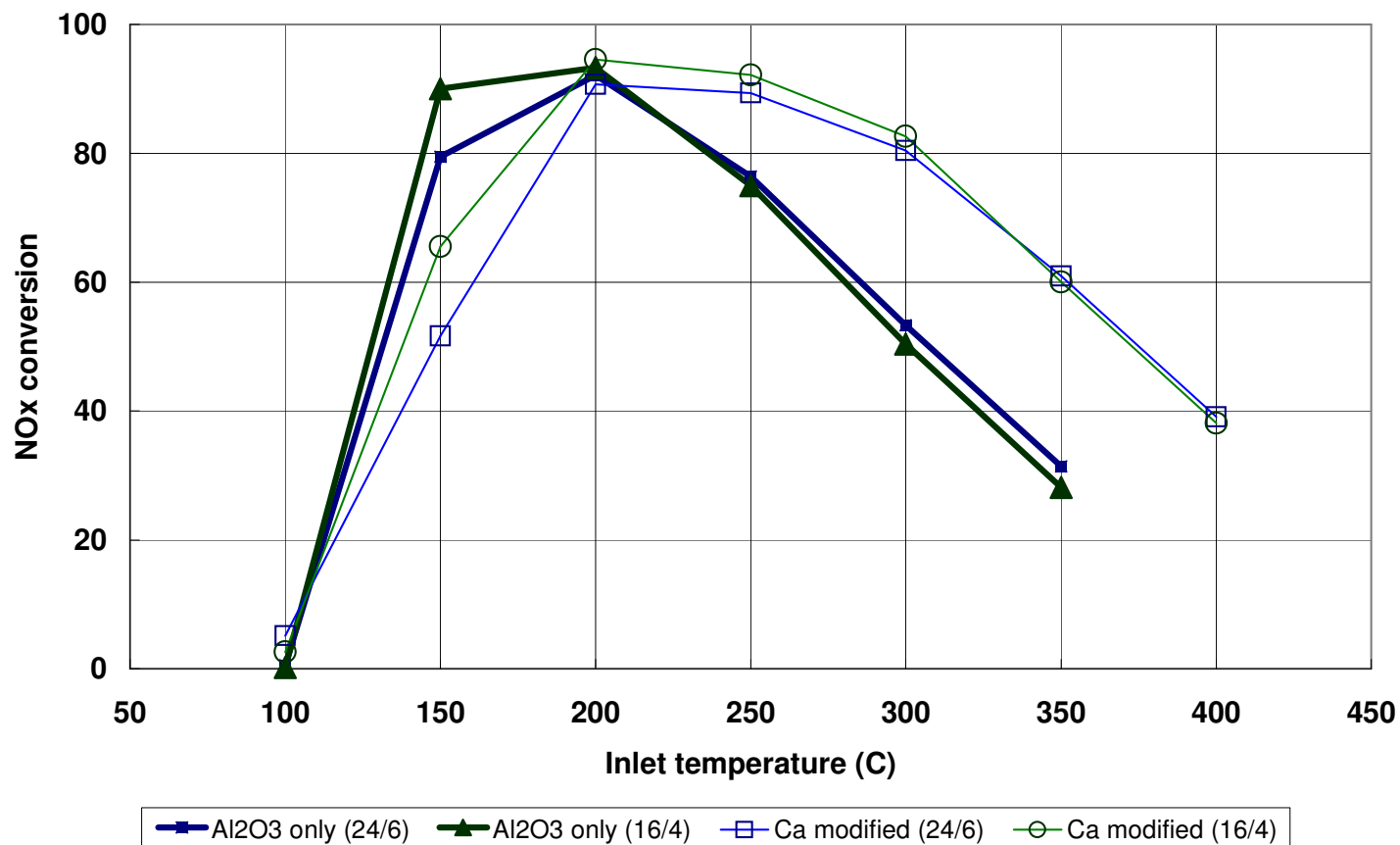
## First New LNT at 650°C and the second one at 280°C



- S loading at the first New LNT 1.14g/liter & w/o S at the second one
- $\text{SO}_2$  released from first bed passes through second bed
- System has easy, fast de- $\text{SO}_x$

# Modification of Alumina based LNT by alkaline earth metals (2 to 3 wt%)

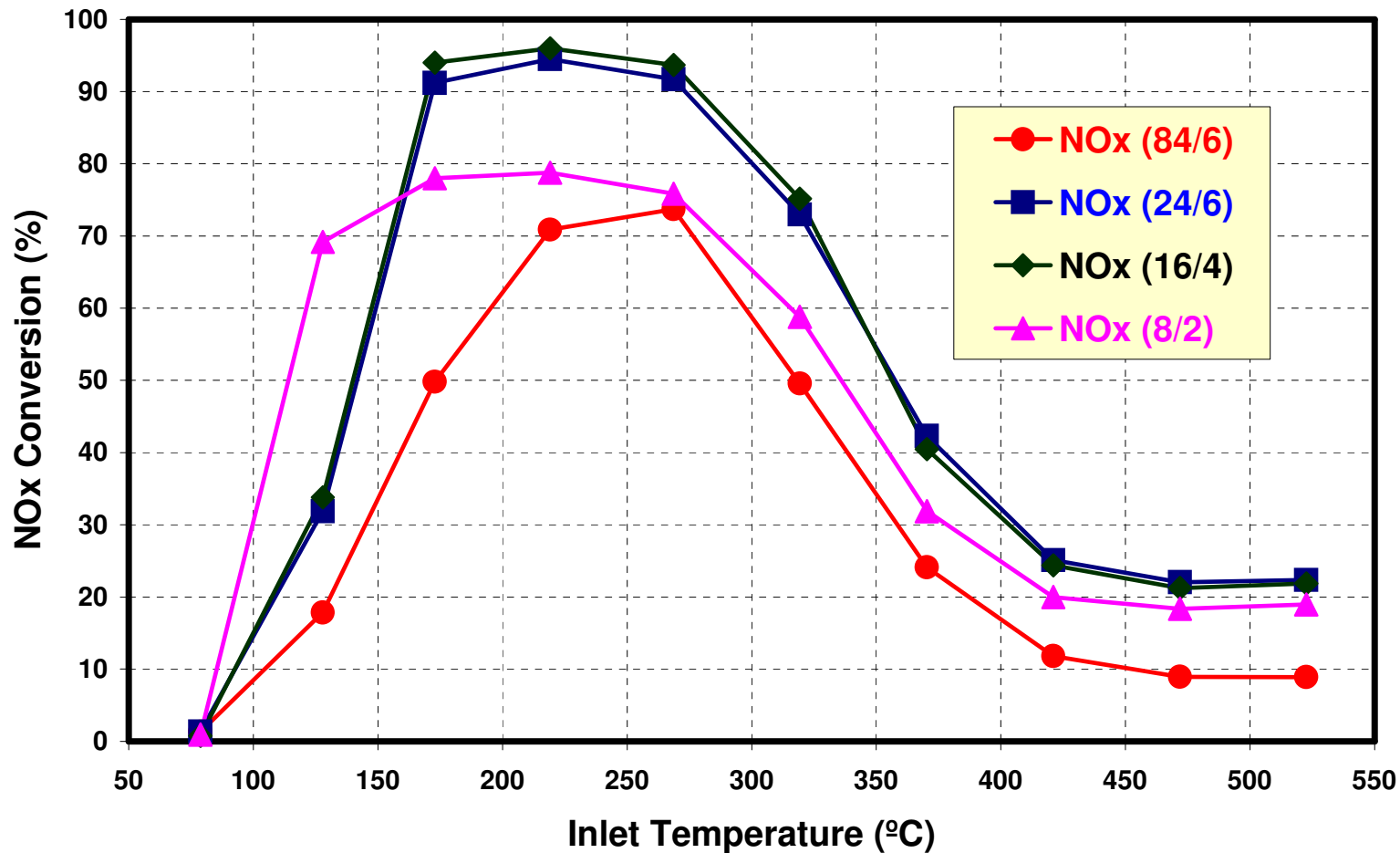
Alumina-based LNT (Pt:Rh/100:20) after S poisoning & de-SO<sub>x</sub> under different lean/rich cycles





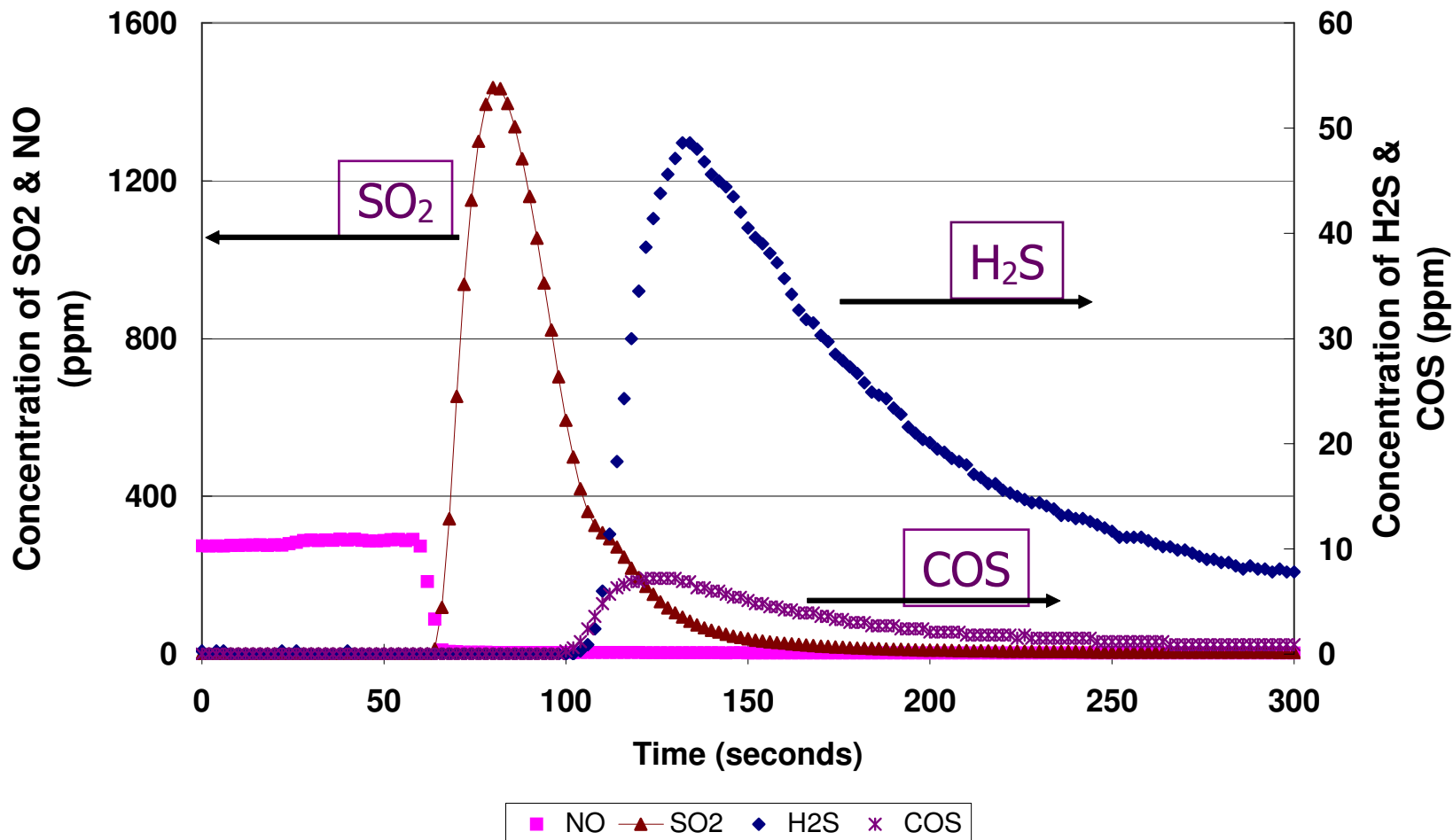
# New LNT produced by a supplier

New LNT ( $\text{Al}_2\text{O}_3$ : two times of nominal loading) after loading  $\text{SO}_2$  & de $\text{SO}_x$  for 2 times



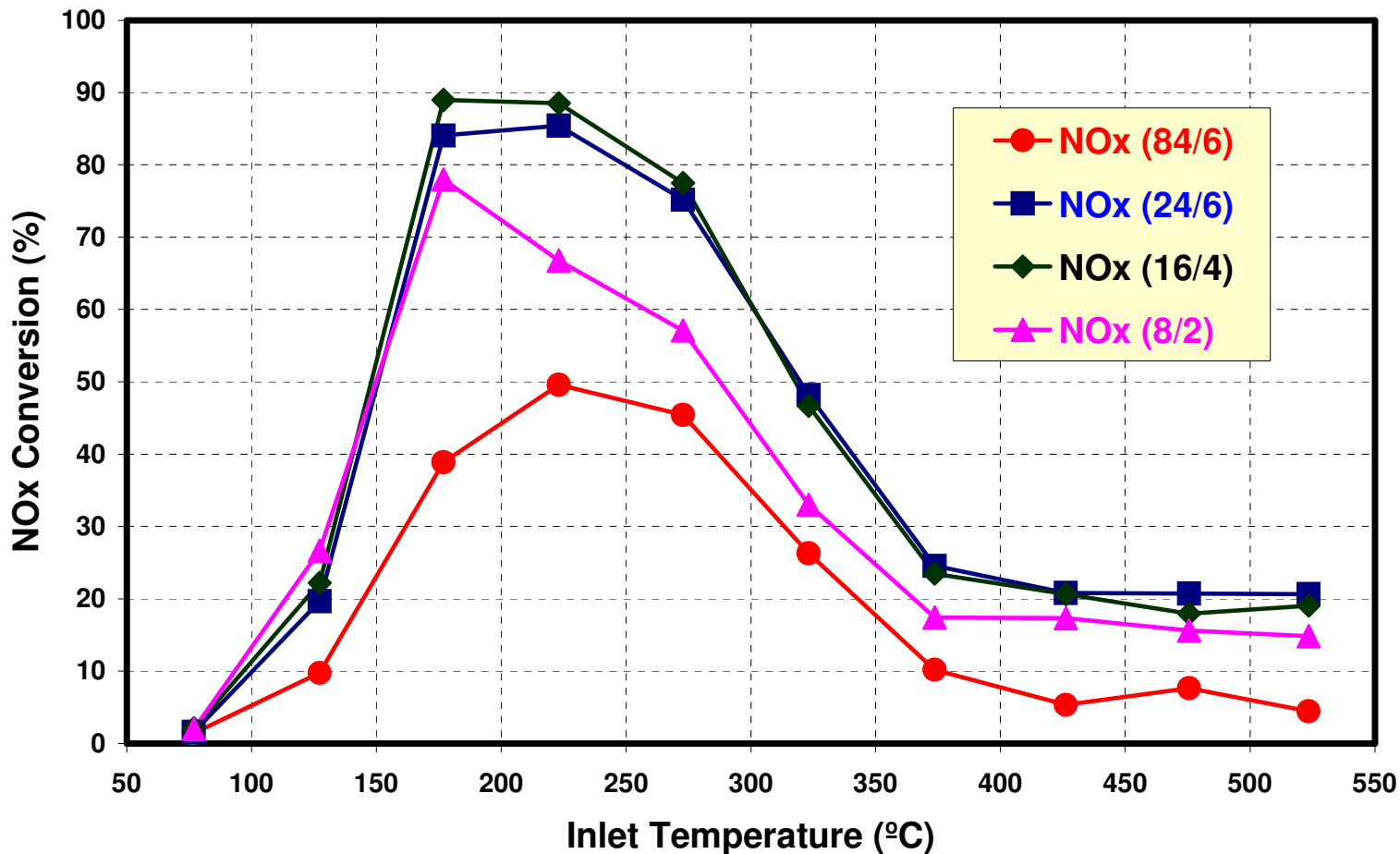
# New LNT produced by a supplier

De-SOx of New LNT (Al<sub>2</sub>O<sub>3</sub>: 2 times of nominal loading)  
at 650C (lambda = 0.987)



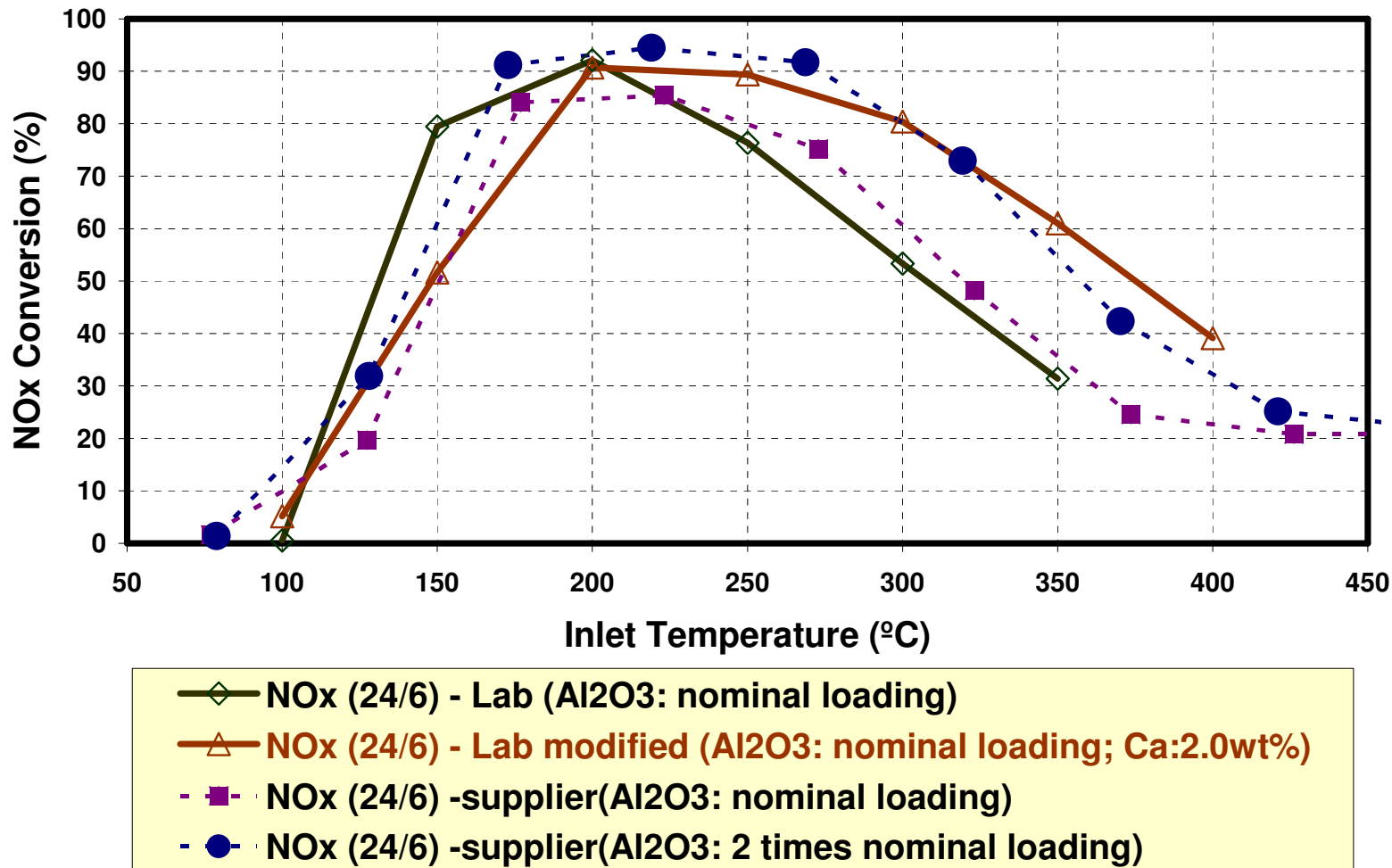
# New LNT produced by a supplier

New LNT ( $\text{Al}_2\text{O}_3$ : nominal loading) after loading  $\text{SO}_2$  & de $\text{SO}_x$  for 2 times



# Alumina based LNTs compared

New LNT ( $\text{Al}_2\text{O}_3$  based  $120\text{g}/\text{ft}^3$  Pt:Rh = 5:1) after loading  $\text{SO}_2$  & de $\text{SO}_x$  for two times



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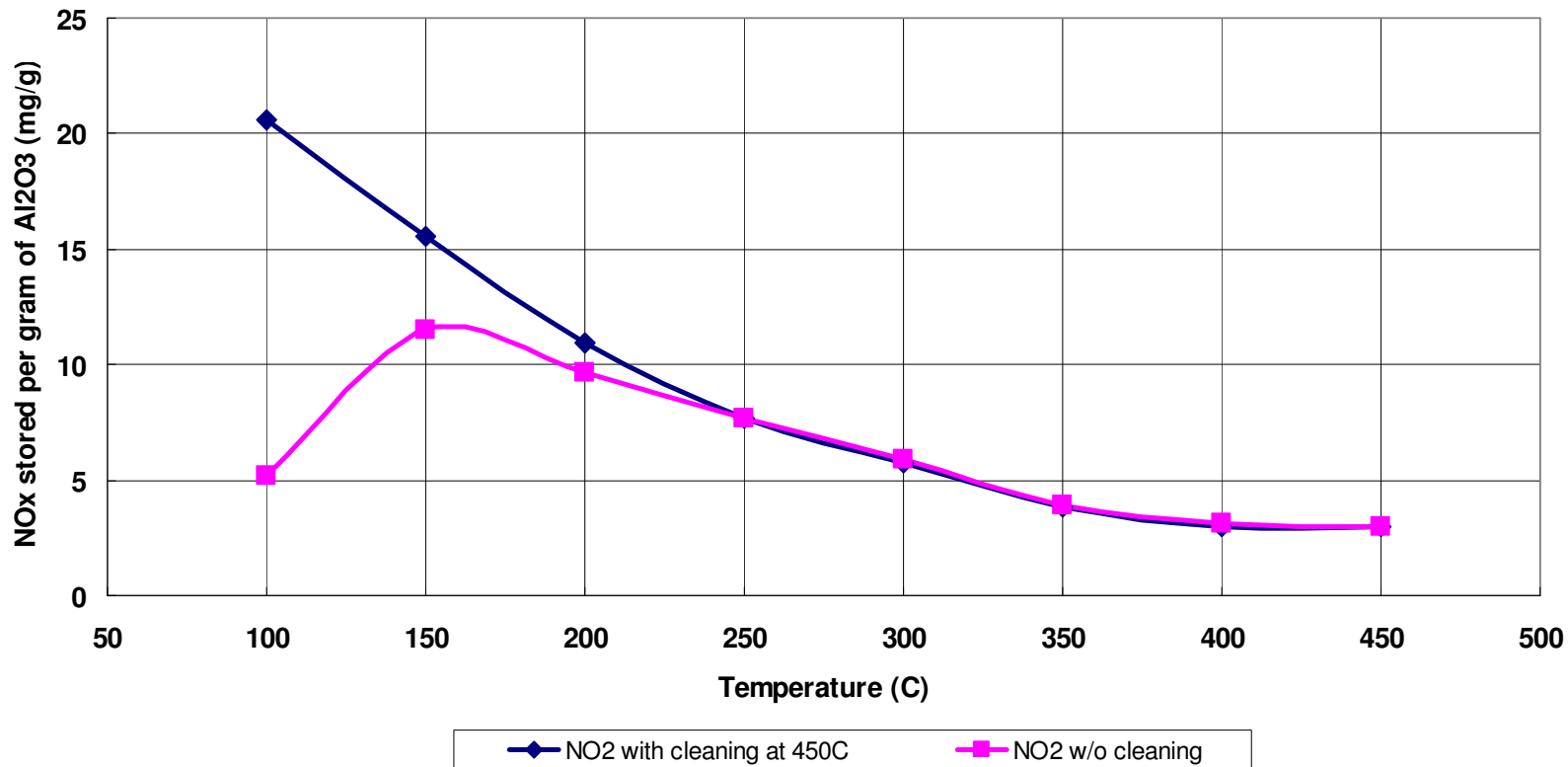
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# Discussion

NO<sub>2</sub> storage vs. Catalyst Temperature (C) - Al<sub>2</sub>O<sub>3</sub> based (nominal loading)

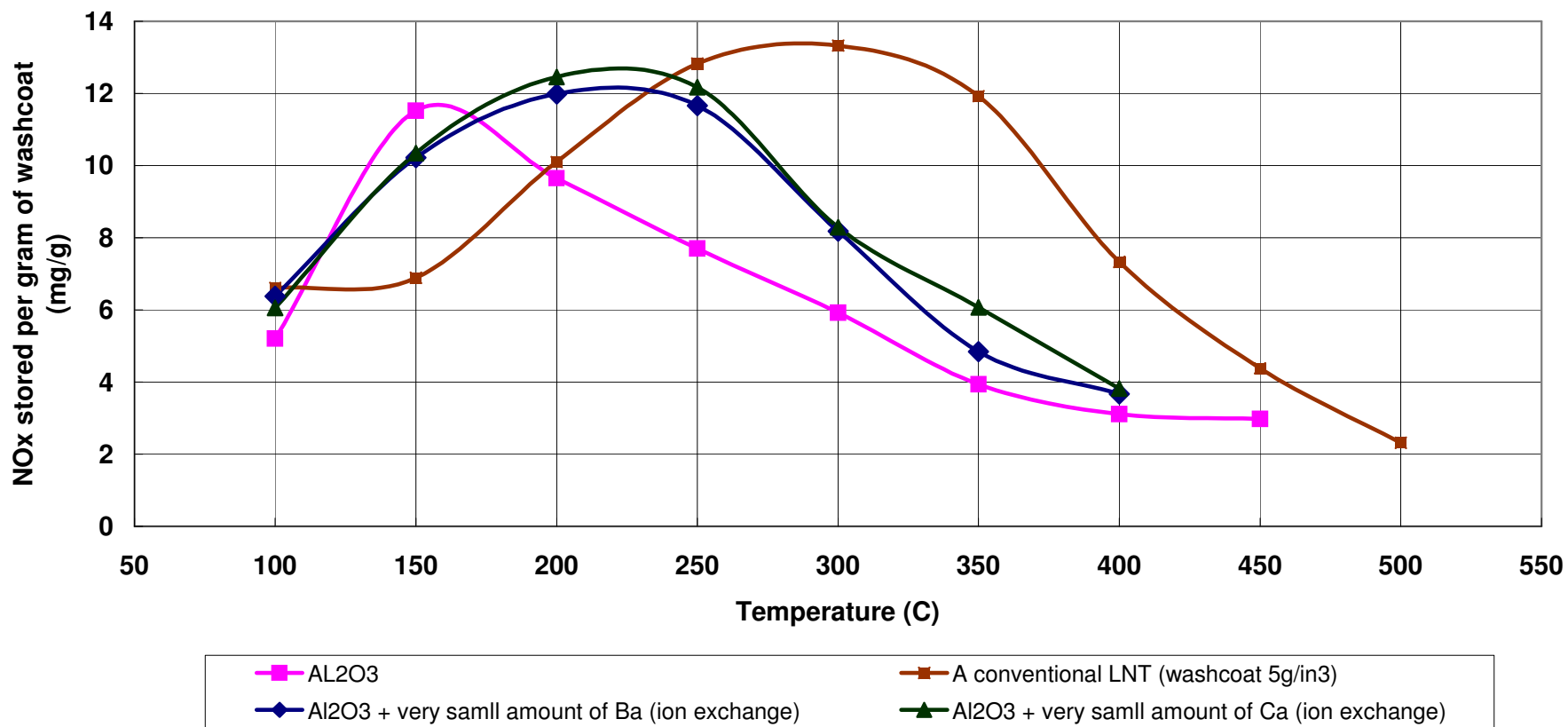


**With cleaning:** 1. heat sample to 450 to 550°C in N<sub>2</sub> for 10 min then cool down to the test temperature;  
2. load NO<sub>x</sub> in lean condition until saturation;

**Without cleaning:** only run 10 min/3min lean/rich cycle at test temperature until stabilized;

# Discussion (continued)

NO<sub>2</sub> storage (w/o cleaning at high temperature) in 10min/3min





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# Conclusions

- Alumina based (New) LNT provides high NO<sub>x</sub> conversion efficiencies at low temperature (150 to 300°C)
- Unique de-SO<sub>x</sub> process of the New LNT
  - Very efficiently removes the S at slightly rich conditions
  - Short thermal exposure & Low fuel penalty
  - It could provide a solution to the current LNT durability issue caused by de-SO<sub>x</sub> process
- A Multiple New LNT system
  - Covers a wide temperature window with high NO<sub>x</sub> conversion efficiencies
  - Maintains unique de-SO<sub>x</sub> process of the New LNT
  - Such a system would work well with the catalyzed DPF and TWC (as in HCCI exhaust system)

## **Conclusions (cont.)**

- Increased alumina loading provides high NO<sub>x</sub> shortage capacity and increases the NO<sub>x</sub> reduction efficiencies, especially in case of the lean/rich cycle with a long lean time (e.g. 84/6).
- Alkaline earth metal(2 to 3 wt%) modified alumina based LNTs also show high NO<sub>x</sub> activities at low temperatures with expanded temperature window and effective de-SO<sub>x</sub> with the same unique de-SO<sub>x</sub> process as the alumina only LNT.