# Lean NOx Trap Regeneration Studies on a Light-Duty Diesel Engine with In-Cylinder Air-to-Fuel Control

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# Outline

- Reductant Production from In-Cylinder Regeneration Strategies
- N<sub>2</sub> Selectivity of Lean NOx Trap Regeneration Processes
  - Bench Flow Reactor Studies
  - Engine Studies

# Acknowledgements

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## Schematic of Experimental Setup [MECA Supplied DOC and LNT]



# **Comparison of three strategies for achieving intermittent rich combustion**

- Two strategies employ no EGR for highest engine-out NOx (fastest adsorber loading)
- Rich excursion is achieved by a combination of intake throttling and the following injection strategies:



## 3<sup>rd</sup> strategy investigated uses high EGR to enter LTC during rich excursion



#### **Real-time data highlights approach of strategies**



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## **Total Reductant Moles for Strategies: Reductant Split Differs for Strategies**

**Engine Out Total CO-equivalent milli-moles** 



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### DEM Generates High Level of PM; P80 and LTC Strategies Produces Very Low PM



#### **Comparison of Mass of NOx Reduced and Fuel Efficiency of NOx Reduction**

Strategies not optimized for FEP, NOx, torque, etc.



## Summary 1: Regeneration Exhaust Species Highly Dependent on Strategy

- DEM (Delayed Extended Main) Strategy
  - High H<sub>2</sub> and CO Levels
  - Best Overall NOx Reduction
  - High PM Levels
- P80 (80° After Top Dead Center) Strategy
  - High HC Levels, Lower  $H_2$  and CO
  - NOx Reduction Performance Less than DEM
  - Lowest PM Levels
- LTC (Low Temperature Combustion) Strategy
  - Low PM Levels (less than typical lean/EGR operation)
  - Best Fuel-Efficiency for Regen (g NOx/g excess fuel)

#### **Engineered Systems May Use Portfolio of Regeneration Strategies**



#### **General Observations Regarding N<sub>2</sub> Selectivity**

- ORNL bench reactor results for engine-aged core sample shown
- N<sub>2</sub>O and NH<sub>3</sub> are both formed during regeneration, but ...
  - <u>only</u> when NOx has been stored on the catalyst
    - >  $N_2$  + reductant =  $NH_3$  is not likely
- NH<sub>3</sub> appears <u>after</u> initial main NOx release/reduction spike



See Castoldi et. al, Cat. Today 96 (2004) 43-52 for NH<sub>3</sub> vs. sorbate loading



#### **NH**<sub>3</sub> **Production During Extended Regeneration Observed** in Engine Studies

- NH<sub>3</sub> and N<sub>2</sub>O measured at tailpipe via FTIR (cycle averaged analysis)
- Experimental parameters <u>chosen</u> to enhance NH<sub>3</sub> formation
  - DEM, 13:1, 300°C, 60s Cycle
  - "Over-regeneration" with high NOx saturation of LNT
- Excess reductant leads to high  $\rm NH_3$  emissions and reduced NOx to  $\rm N_2$  reduction efficiency







#### **Engine Regeneration Strategies Can Be Developed to Optimize N<sub>2</sub> Selectivity**

In-Cylinder

- Comparison for (2) regeneration strategies
  - Same fuel penalty
  - Same base parameters
    - Temperature=300°C
    - Cycle period=60 sec
    - Engine Out NOx~500 ppm
    - DEM regeneration strategy
    - > 13:1 A/F target



#### Pulsed Strategy Gives Lower NH<sub>3</sub> <u>AND</u> Equivalent NOx Reduction

	Standard	Pulsed	Difference
Engine Out NOx (ppm)	472.1	457.3	-3.1%
Avg. Tailpipe NOx (ppm)	138.7	98.6	-29.0%
Avg. Tailpipe NH3 (ppm)	217	73	<b>-66.4%</b>
NOx Capacity (g/l)	0.311	0.317	2.2%
BSFC (lb/bhp-hr)	0.381	0.390	2.3%
Catalyst Temperature (C)	331.5	342.6	3.4%





Tailpipe O<sub>2</sub> Analysis Shows O<sub>2</sub> Purge for Pulsed Case



#### N<sub>2</sub> Selectivity Highly Dependent on Reductant:NOx Ratio

- Bench Flow Reactor Temperature Programmed Reduction (TPR) Experiments at 100,000/hr SV
- Reducing Conditions: CO and NO Into Catalyst
  - At CO:NO=1, N<sub>2</sub> Selectivity High N<sub>2</sub> Preferred
  - At CO:NO=10, N<sub>2</sub> Selectivity Low NH<sub>3</sub> Preferred
- Same Trend Holds for H<sub>2</sub> Reductant and NOx as NO<sub>2</sub>
- See Josh Pihl (U. of Wis.) Poster for More Details



# **Theories for NH<sub>3</sub> Formation**

- N<sub>2</sub> and reductant (H<sub>2</sub>, etc.) react to form NH<sub>3</sub> on precious metal site during regeneration
  - No supporting data found to date
- Isocyanate surface species formed on Pt plays role in NH<sub>3</sub>
  formation [Lesage et.al., *Phys. Chem, Chem. Phys.*, 5 (2003)]
  - 2 NCO + 3 H<sub>2</sub>O → 2 NH<sub>3</sub> + 2 CO<sub>2</sub> + 0.5 O<sub>2</sub> [Rich: NCO → NH<sub>3</sub>]
  - 2 NCO +  $O_2$  →  $N_2$  + 2 CO<sub>2</sub> [Lean: NCO →  $N_2$ ]
  - Engine studies show reduced NH<sub>3</sub> formation via O<sub>2</sub> purge during regeneration
- NH<sub>3</sub> formed from gaseous NOx released from catalyst in reactions with surrounding reductants (H<sub>2</sub>, CO, etc)
  - High dependence on reductant to NOx ratio observed
  - Bench reactor experiments show decay of NH<sub>3</sub> formation with time suggesting slow NOx release from catalyst is source of NH<sub>3</sub>

No - Supporting Data

Supporting Data Observed



# Summary 2: Strategy Dictates N<sub>2</sub> Selectivity

- NH<sub>3</sub> and N<sub>2</sub>O can be formed during LNT regeneration
  Produced from NOx stored on catalyst
- Selectivity toward N<sub>2</sub> vs. NH<sub>3</sub> is highly dependent on ratio of reductant to NOx during regeneration
  - It is critical to match reductant to NOx ratio in dynamic process
- Strategy details critical for minimal fuel penalty and optimal NOx reduction to N<sub>2</sub>
- Lean-rich pulsing during regeneration gives lower NH<sub>3</sub> formation <u>AND</u> Equivalent NOx reduction
  - Transient analysis of tailpipe O<sub>2</sub> with SpaciMS shows:
    - O<sub>2</sub> purge during regeneration (supports isocyanate and other theories)

