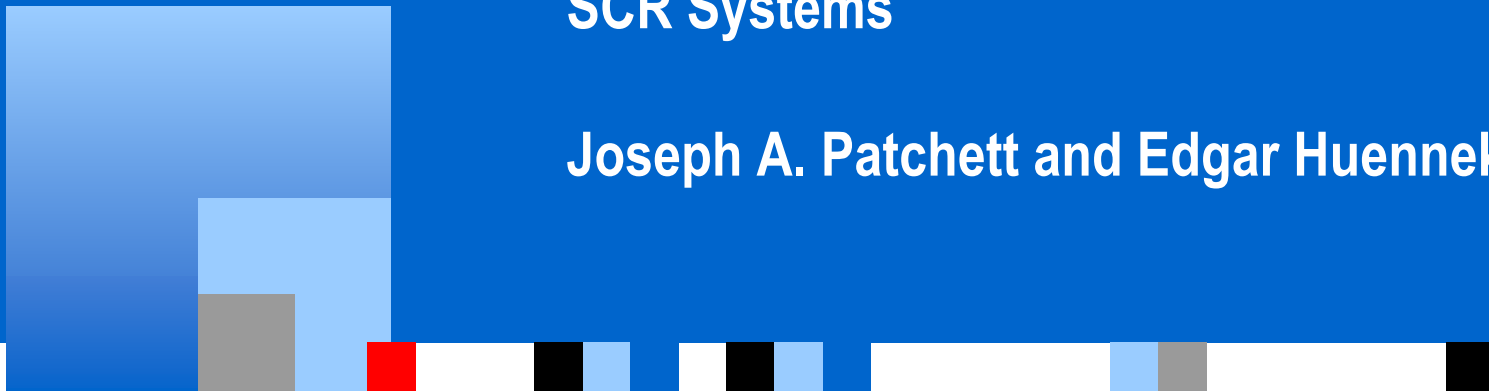


# The Case for Ammonia Oxidation Catalysts in SCR Systems

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**ENGELHARD**



## Presentation Outline

- Background for ammonia oxidation catalysts
- Characterization of ammonia oxidation catalysts
- Typical laboratory evaluations
  - Aged with and without NO<sub>x</sub>
- Evaluations using heavy duty diesel engine
  - transient conditions (ETC)
  - steady state



## Why use an Ammonia Oxidation (AMOX) Catalyst ?

- While only NO<sub>x</sub> is regulated....
  - ammonia has a distinctive odor – similar to the H<sub>2</sub>S problem in TWC
  - ammonia can contribute to particulate
- Target ammonia emissions are peaks of about 20 ppm
- Depending on engine out NO<sub>x</sub> and the desired level of NO<sub>x</sub> conversion; SCR systems are really designed to remove ammonia.
- Potential to make the after treatment system smaller
- Relaxed dosing requirements



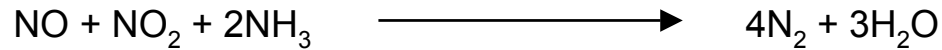
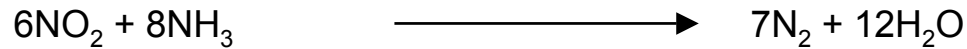
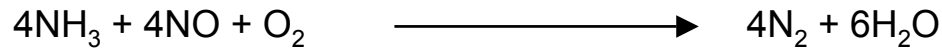
## Sources of Ammonia Emissions

- Incomplete reaction of ammonia with NOx
- Sudden release of ammonia from the decomposition / hydrolysis of urea deposits in the exhaust line
- Ammonia release from the catalyst surface during a temperature increase. Result of changes in the equilibrium concentration of ammonia stored on the catalyst.
  - For example: Idle to A100 transition in the ESC

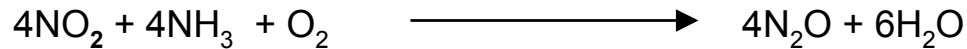


## Possible Chemical Reactions

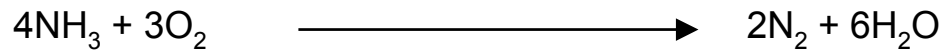
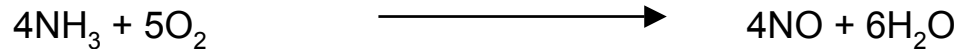
### SCR NO<sub>x</sub>:



### Other NO<sub>x</sub> reactions



### NH<sub>3</sub> Oxidation:



### Preferred Activity Level

High

High

High

Low

Low

High

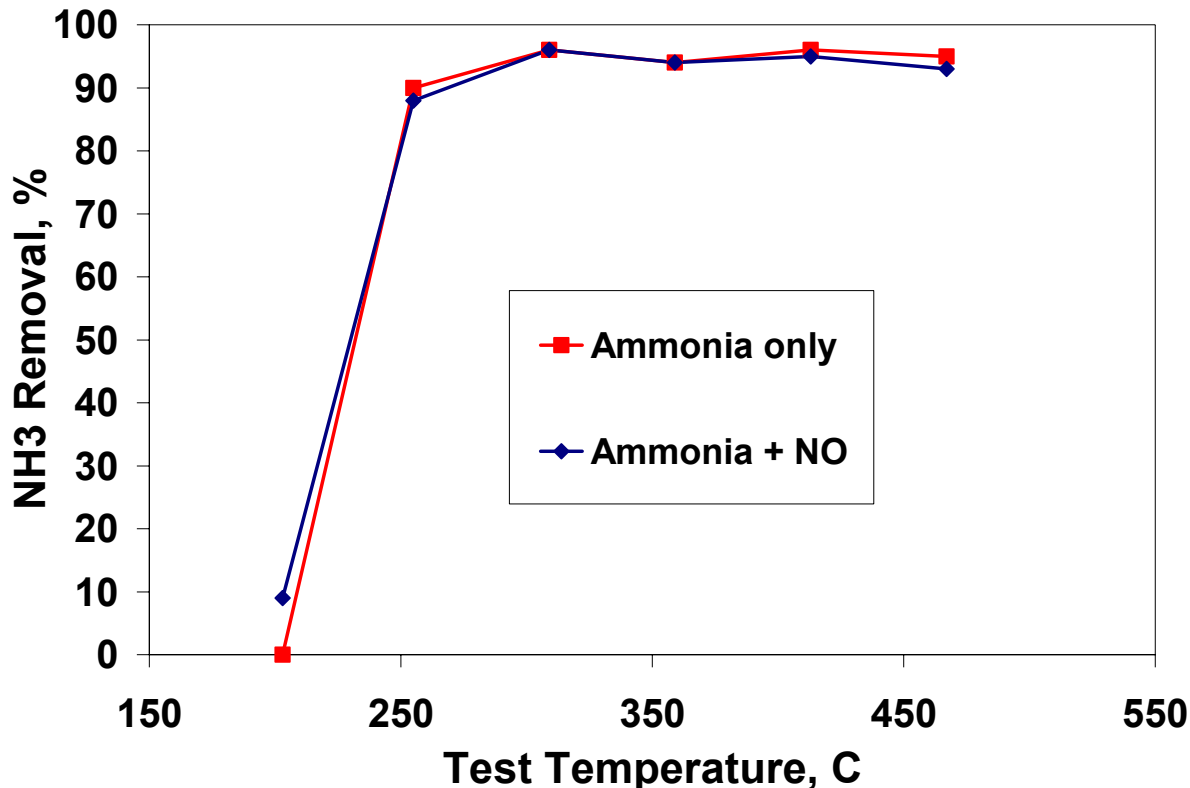


## Evaluation of AMOX catalysts



- Evaluation by the destruction of ammonia is insufficient
  - NO<sub>x</sub> and N<sub>2</sub>O production must also be considered
- For NO<sub>x</sub> make:
  - a)  $\Delta \text{NO}_x / \text{inlet NH}_3$  or b)  $\Delta \text{NO}_x / \Delta \text{NH}_3$
- For N<sub>2</sub>O make;
  - a)  $2 \Delta \text{N}_2\text{O} / \text{inlet NH}_3$  or b)  $2 \Delta \text{N}_2\text{O} / \Delta \text{NH}_3$ 
    - With NO<sub>x</sub> in the feed, NO<sub>x</sub> can contribute to the N<sub>2</sub>O concentration via the SCR reaction
- With a pre DOC / CSF in the system some N<sub>2</sub>O can come from the HC lean NO<sub>x</sub> reaction

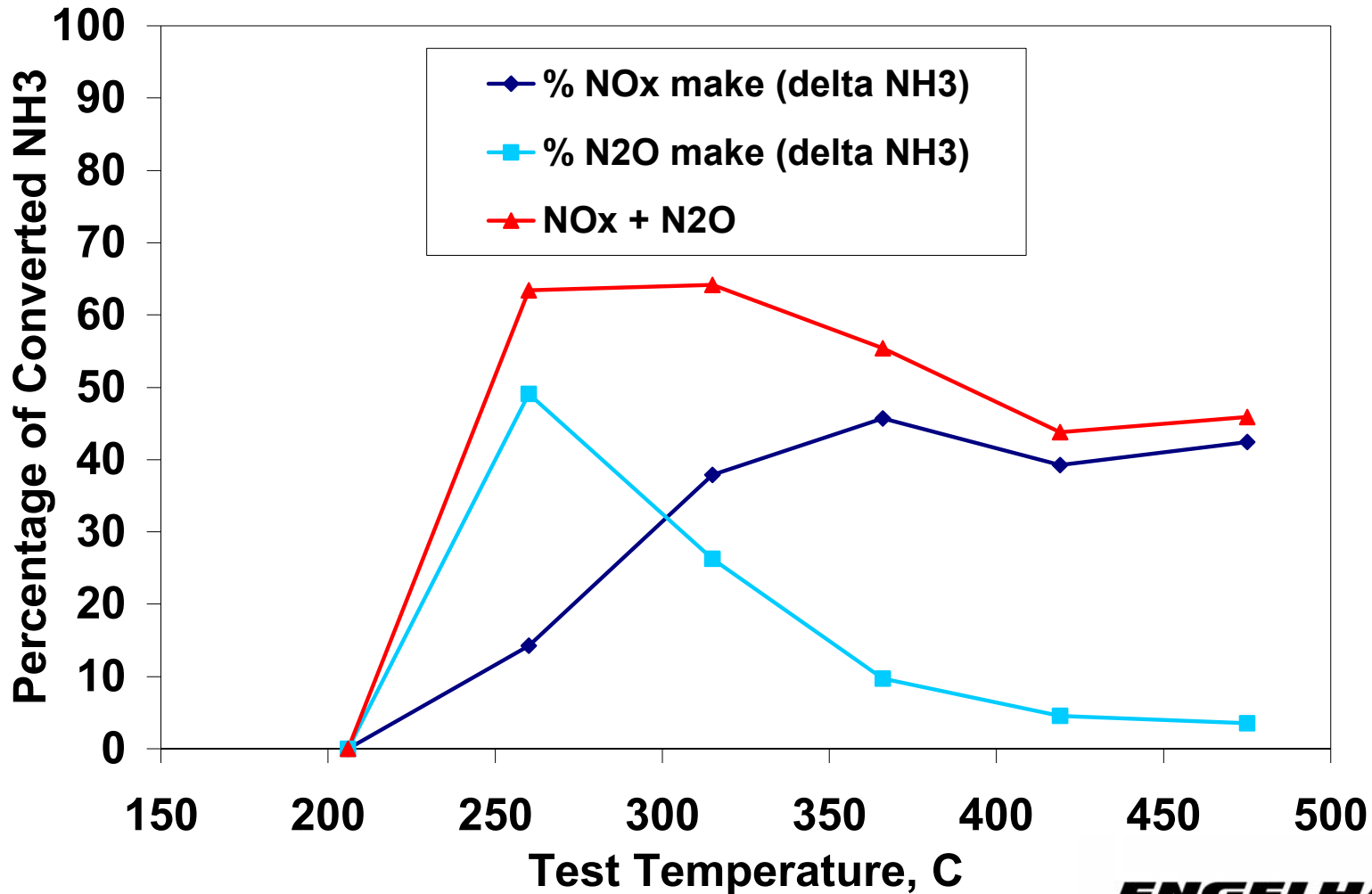
## Typical ammonia removal at 5 g/ft<sup>3</sup> Pt, Lab reactor, 10% O<sub>2</sub> & H<sub>2</sub>O



- With small catalyst lengths entrance effects are important
- Zone coated catalysts must account for the up stream honeycomb channels
- i.e.. 0.5 inch catalyst length is not the same as 0.5 catalyst coated on a 6 inch honeycomb

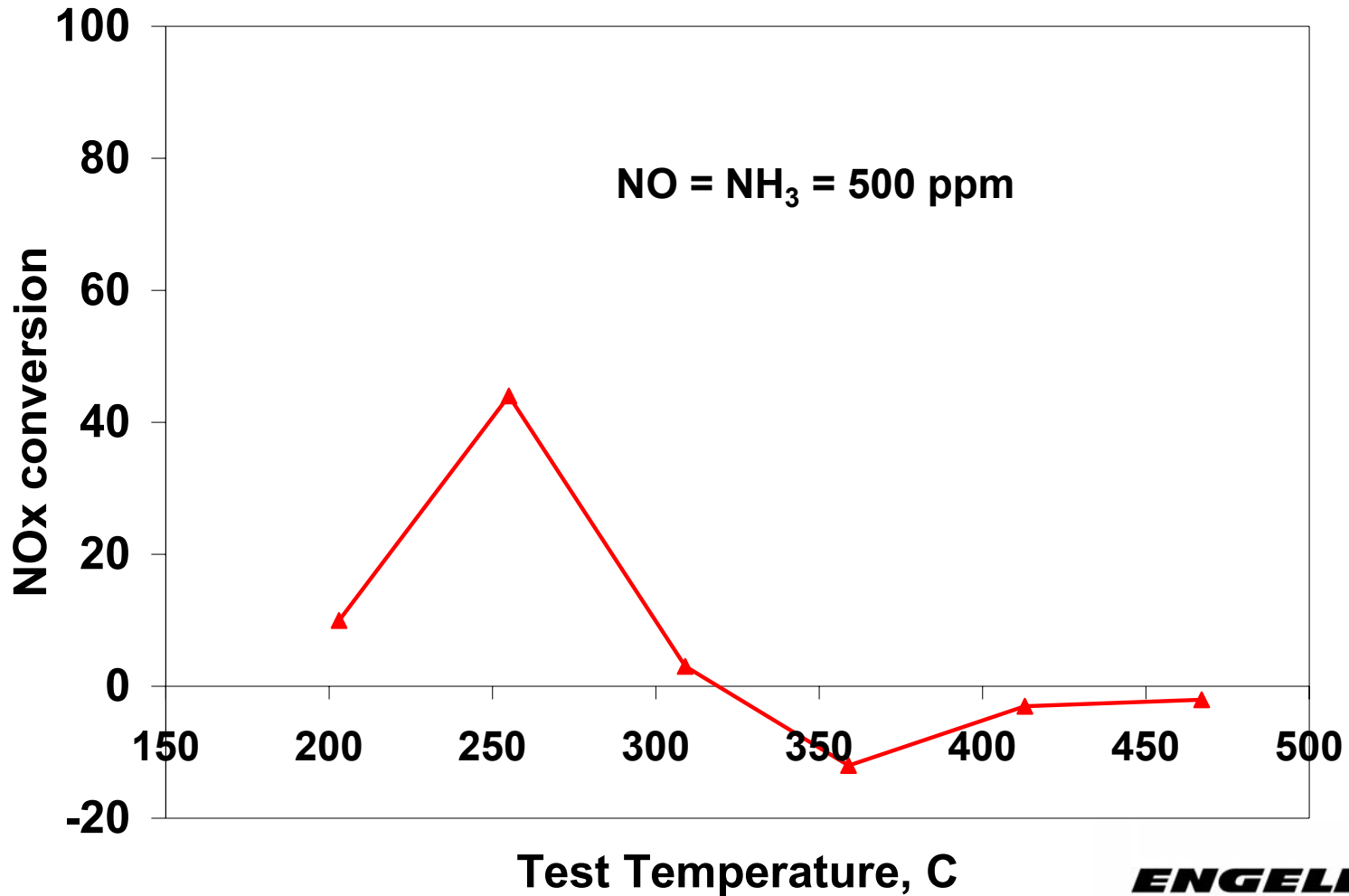
3 inch length, engine aged 800 hrs @ 400 C SV = 80,000 hr<sup>-1</sup>  
NH<sub>3</sub> = 500 ppm, NO<sub>x</sub> as NO = 500 ppm

In the absence of NO the yield to N<sub>2</sub> varies from 35 to 55 %

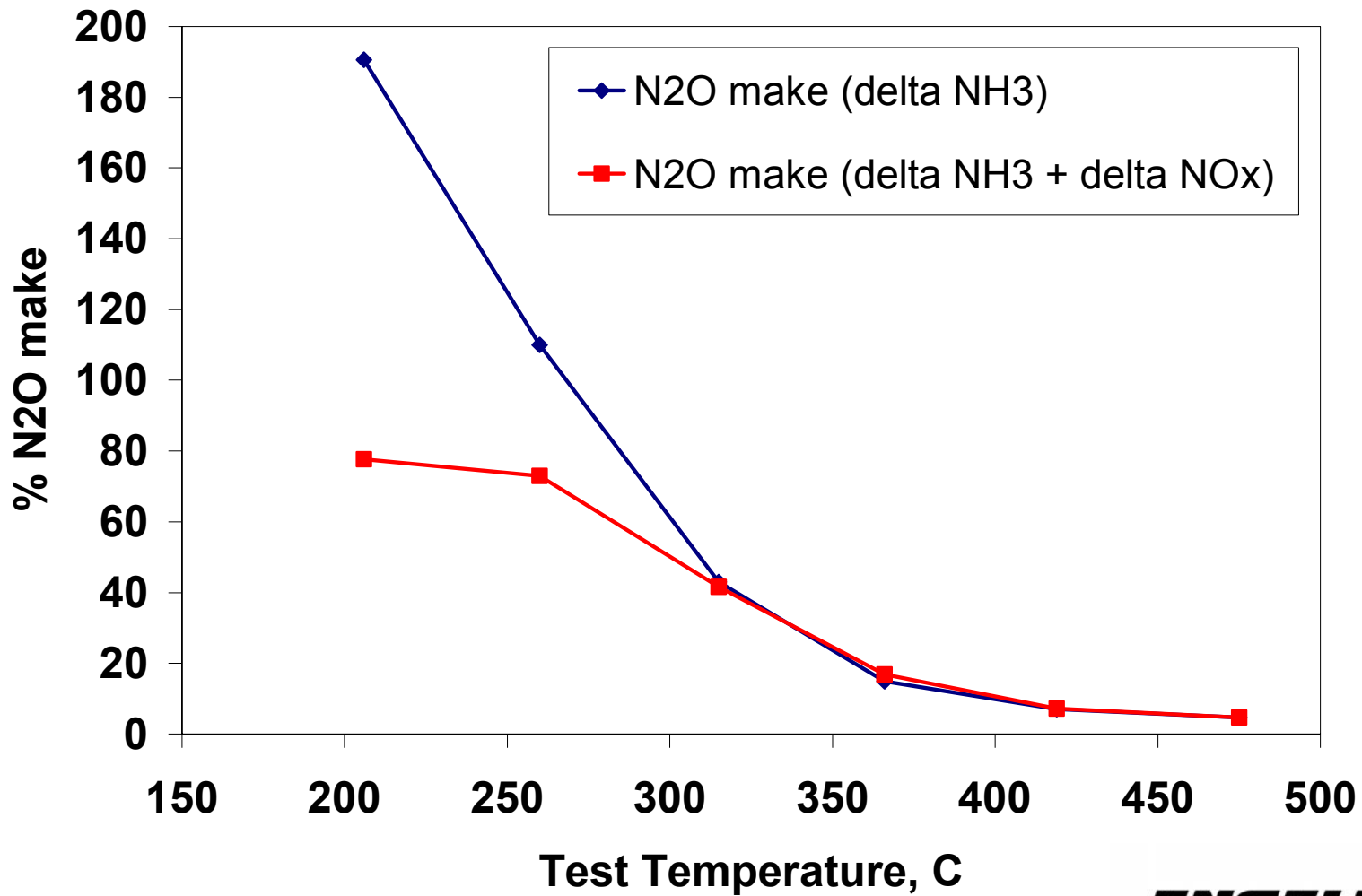




In the presence of NO(x) significant NOx removal can occur at lower temperatures



**N<sub>2</sub>O concentrations are too high to come from just NH<sub>3</sub> oxidation**

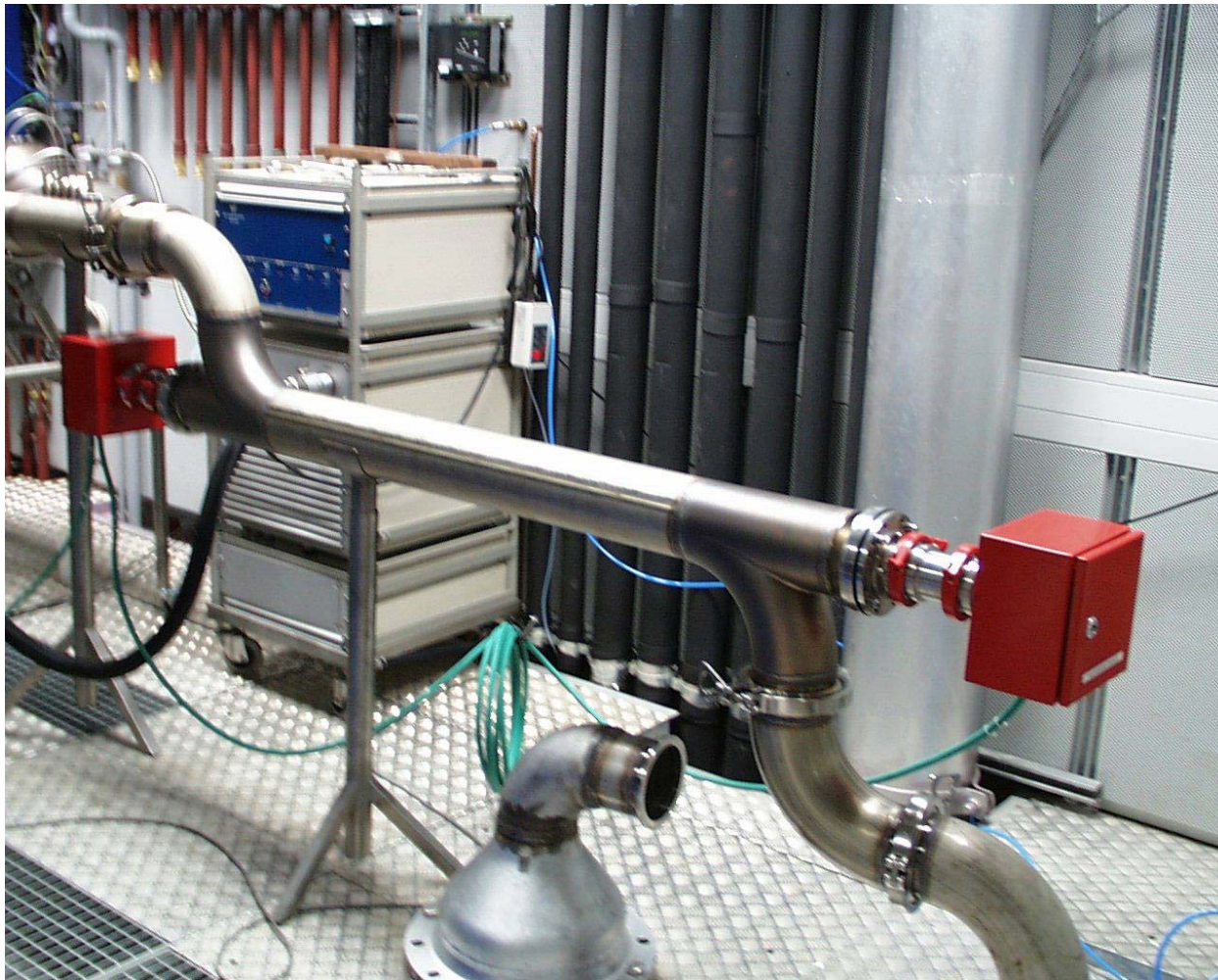




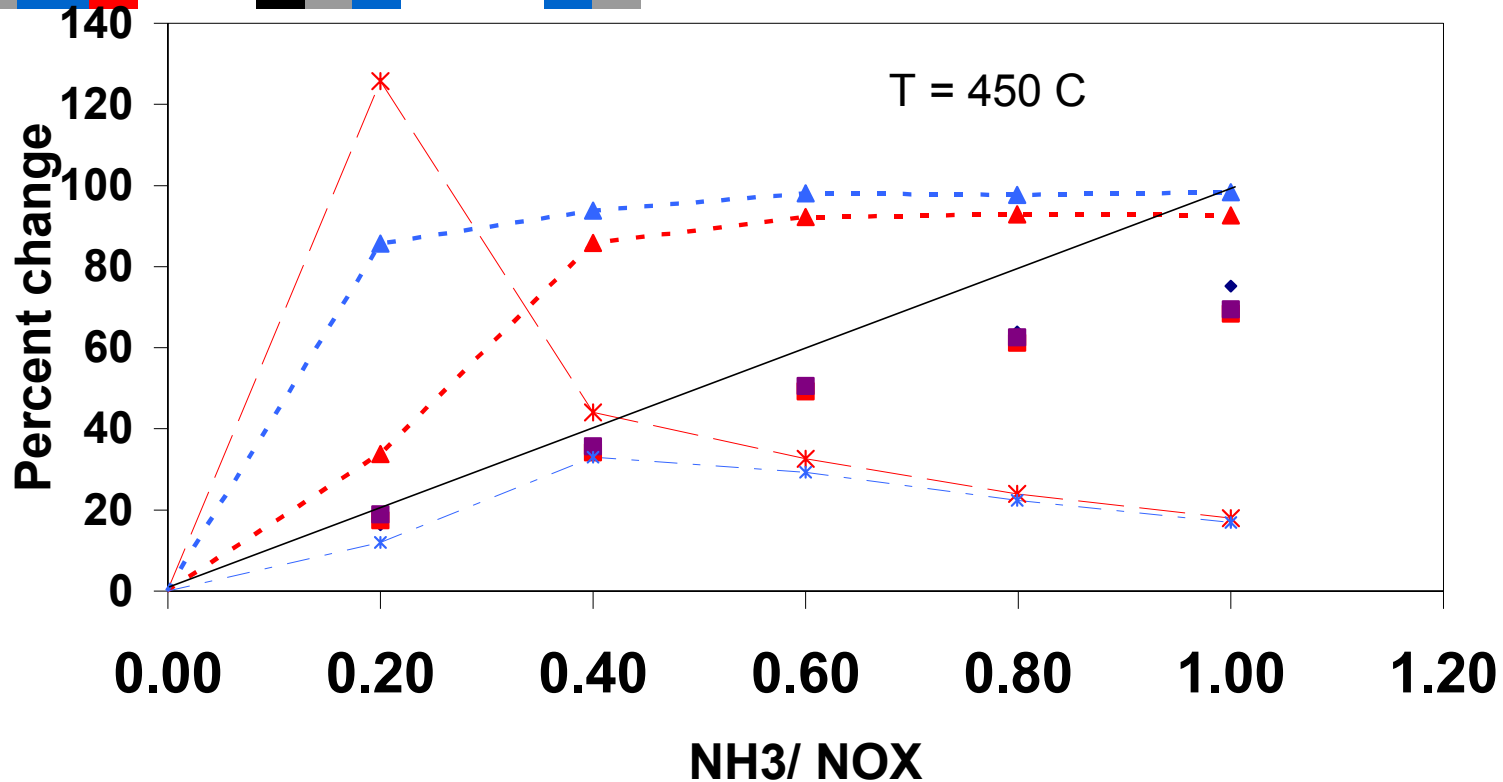
## Catalysts used for engine evaluation

- SCR
  - $\text{TiO}_2 - \text{WO}_3 - \text{V}_2\text{O}_5$
  - Aged and reduced in volume to guarantee unreacted ammonia
- AMOX
  - oxidation catalyst with  $5 \text{ g/ft}^3 \text{ Pt}$
  - two catalyst volumes to study SV effects
- Urea dosing
  - in house system, NOx following based NOx sensor post turbo
  - unless indicated  $\text{NH}_3 / \text{NOx} = 0.8$ , constant
- Engine is 12.6 liter, Euro 3, turbo charged, after cooled, no EGR

# Ammonia measurement in the test cell used LDS 3000 behind SCR/AMOX catalysts

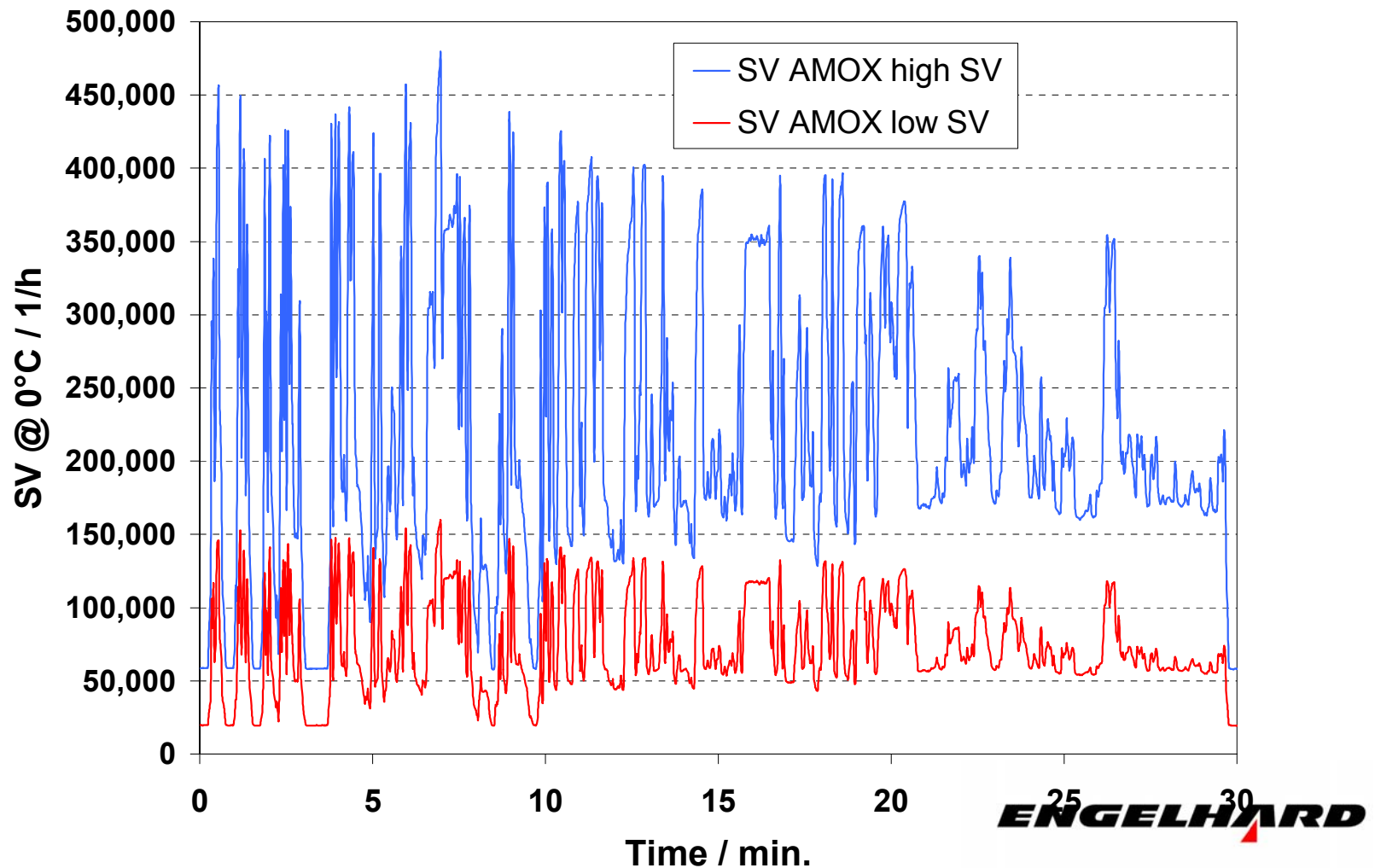


At constant temperature, the  $N_2O$  make decreases as the  $NH_3$  concentration increases, SV AMOX = 90,000 and 270,000  $hr^{-1}$

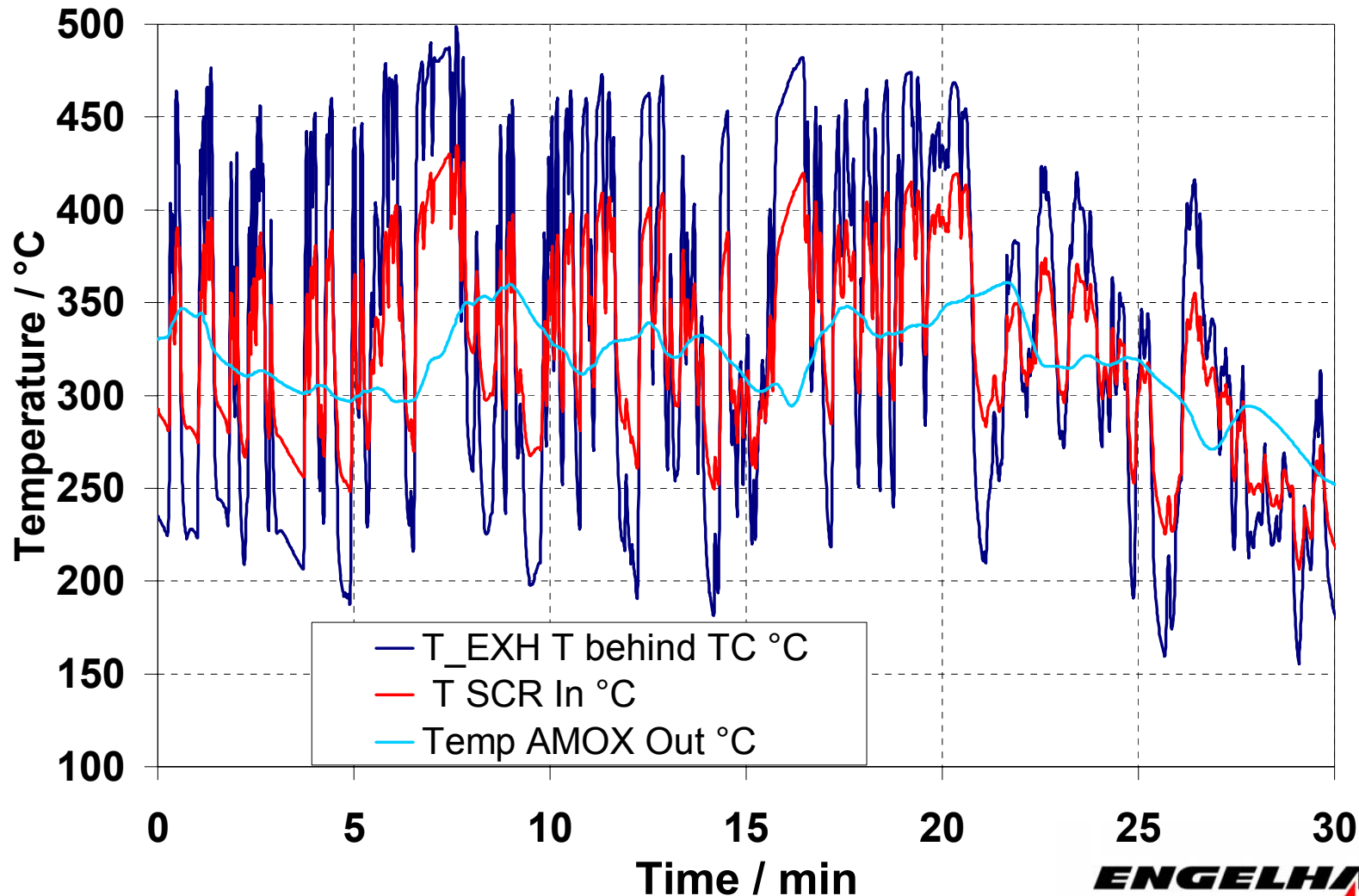


- ◆ DeNOx, No AMOX
- ▲- NH3 Conv, High SV AMOX
- DeNOx, Low SV AMOX
- \* - Delta N2O / Delta NH3, High SV AMOX
- ▲- % NH3 removal, Low SV AMOX
- \* - Delta N2O / Delta NH3, Low SV AMOX

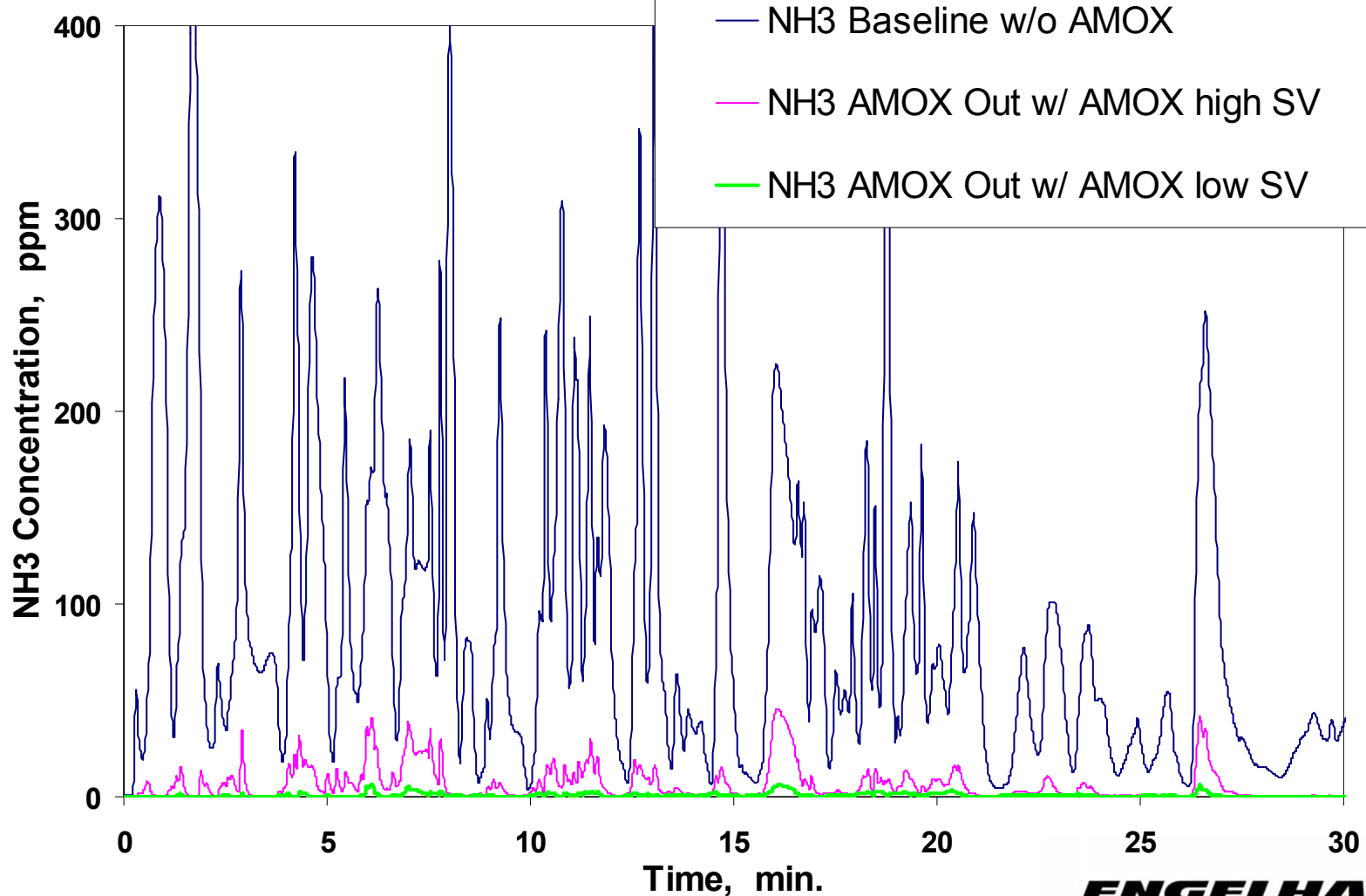
For the two AMOX volumes studied – SV ranges from 50,000 – 150,000 and 150,000 - 450,000 hr<sup>1</sup>, Data from ETC



# The catalyst volume ahead of the AMOX dampens temperature changes and range, ETC

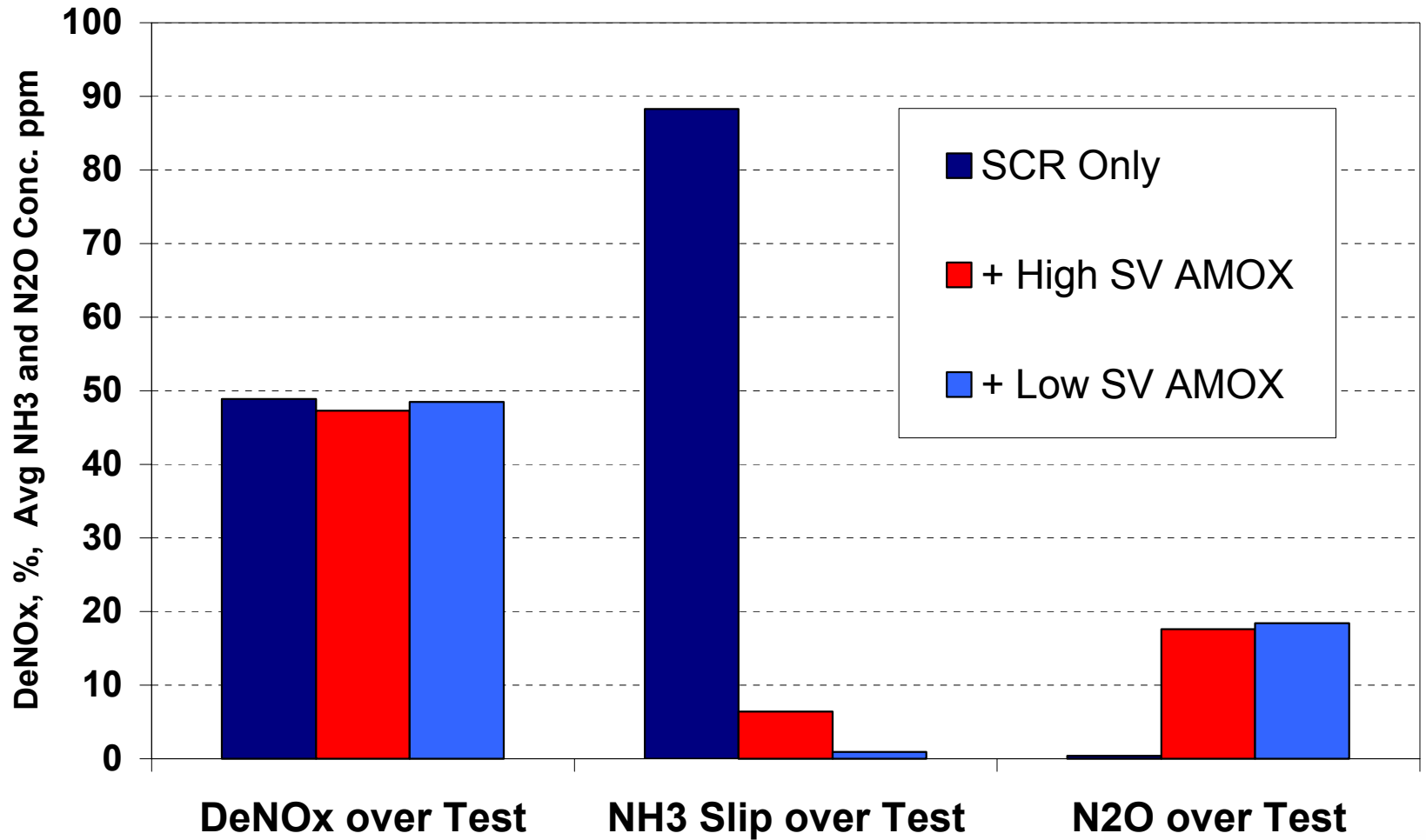


# Even with a small catalyst volume (high SV) effective ammonia control is obtained (ETC modal data)

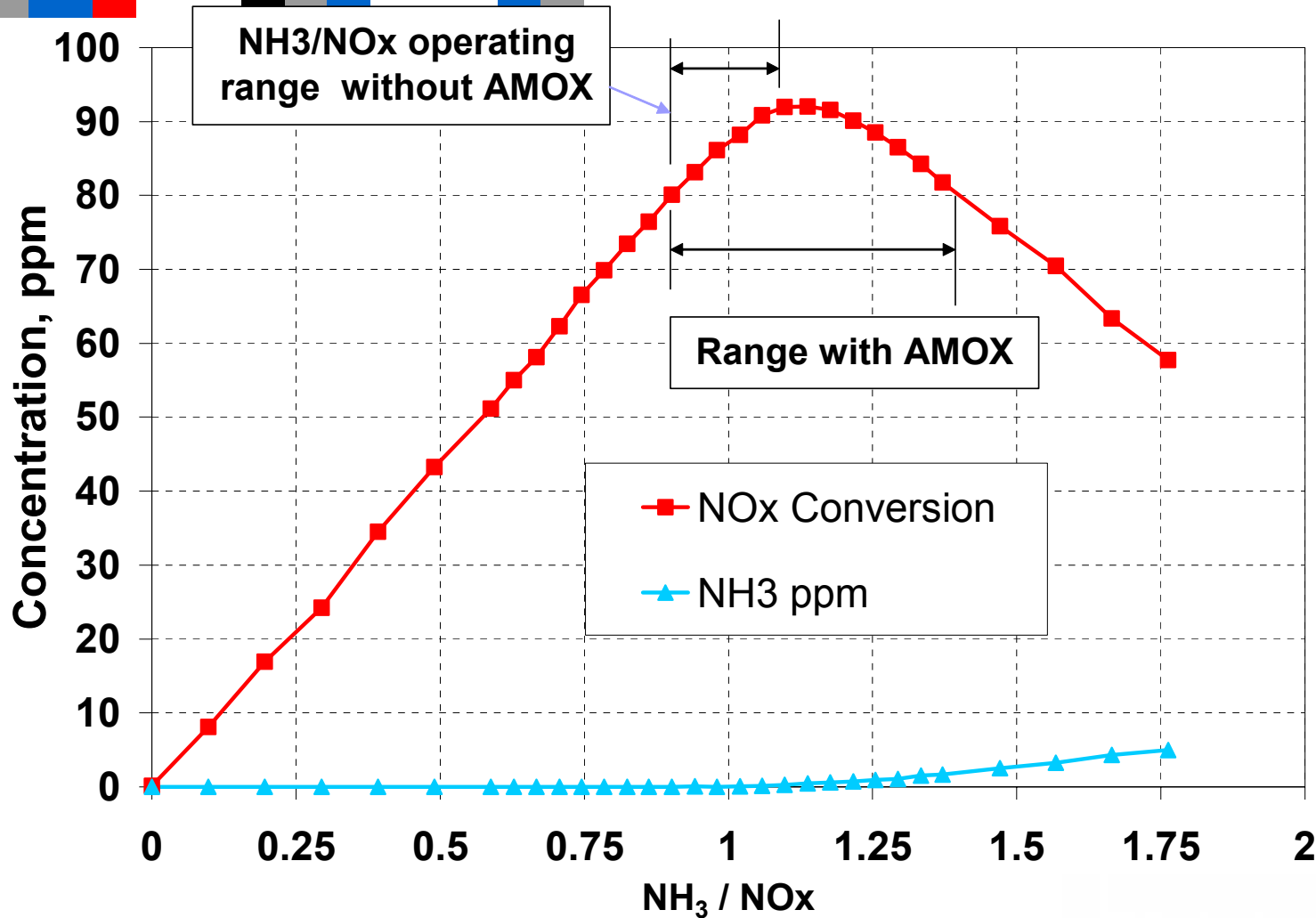




# The oxidation of ammonia is not accompanied by an increase in NOx, Cycle data for the ETC



# Extending the $\text{NH}_3/\text{NO}_x$ to higher ratios shows the dosing flexibility created by the AMOX (different catalyst system, 450 C)





## Conclusions



- Catalysts have been developed that are effective in removing ammonia without excessive NO<sub>x</sub> or N<sub>2</sub>O make
- The selectivity and activity of these catalysts is strongly dependent on the operating conditions
  - transient operation is more beneficial than steady state
  - NH<sub>3</sub> / NO<sub>x</sub> ratio
- The greatest contribution of the AMOX catalyst will be in its ability to expand the range of NH<sub>3</sub>/NO<sub>x</sub> ratios over which high NO<sub>x</sub> conversion can be achieved.